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COMBUSTION RESPONSE MODELING FOR COMPOSITE SOLID PROPELLANTS.(U)

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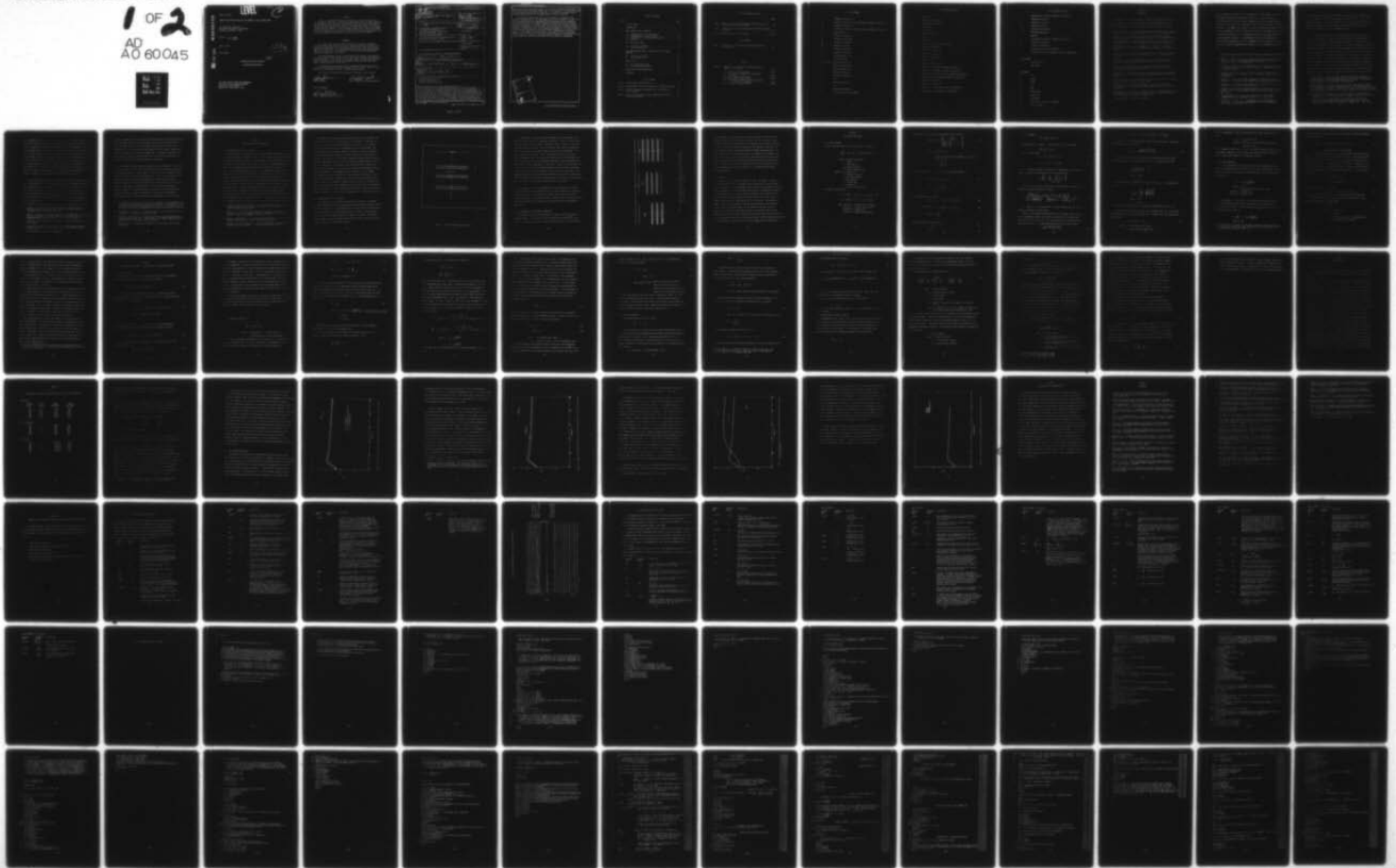
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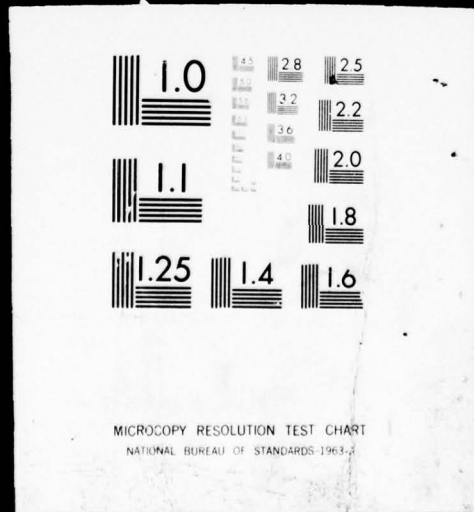
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COMBUSTION RESPONSE MODELING FOR COMPOSITE SOLID PROPELLANTS

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June 1, 1978

Final Report

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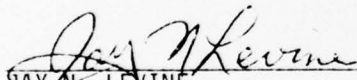
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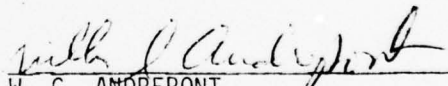
This report was prepared by the Jet Propulsion Laboratory, Pasadena, California 91103, under Air Force Rocket Propulsion Laboratory MIPR No. F04611-76-X-0050 as administered by the National Aeronautics and Space Administration under Contract NAS7-100. This investigation is entitled, "Combustion Response Modeling for Composite Solid Propellants," and was technically monitored by Captain Jack Donn and Mr. Jay Levine.

The Program Manager for this program was Mr. Leon Strand. Contributions to the technical effort were made by Drs. James Bowyer, Norman Cohen, Fred Culick and Kumar Ramohalli. The program was conducted within the Advanced Technology Group of the Solid Propulsion and Environmental Systems Section, under the general supervision of Dr. Giulio Varsi.


This report has been reviewed by the Information Office/XOJ and is releasable to the National Technical Information Service (NTIS). At NTIS it will be available to the general public, including foreign nations.

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approximation of the BDP flame model is utilized to represent the gas phase. By the use of several reasonable assumptions, it is found that a significant portion of the problem can be solved in closed form. A method is presented by which the model can be applied to tetramodal particle size distributions.

A computerized steady-state version of the model was completed, which served to validate the various approximations and lay a foundation for the combustion response modeling. The combustion response modeling was completed in a form which does not require an iterative solution, and some preliminary results were acquired. The model satisfactorily describes the steady state combustion properties, but is deficient in describing the transient combustion response. Although an effect of solid phase heterogeneity on transient combustion response is predicted by the current model, the effect is so small as to allow it to be neglected in future work. It is concluded that some other mechanism associated with the propellant heterogeneity must be incorporated into the theory to account for observed behavior. Potential deficiencies of the current model are identified, and areas for future work are recommended.

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# LIST OF SYMBOLS

a	defined in Equation 15
A	kinetics prefactor; also a solid phase parameter in Equation 51
b	defined in Equation 15
B	defined in Equation 3; also a gas phase parameter in Equation 51
c	heat capacity
C	defined in Equation 4.
$C_F$	defined in Equation 24
$C_M$	defined in Equation 13
$C_1, C_2$	arbitrary constants
d	defined in Equation 16
D	defined in Equation 4
$D_1$	oxidizer particle size
E	activation energy
$f_1(x), f_2(x)$	denotes functions of x
F	defined in Equation 22
g	spatial gradient in $\tau$
H	defined in Equation 3
$H_f$	defined in Equation 43
i	$\sqrt{-1}$
k	thermal conductivity
K	C/D
$K_2$	defined by Equation 49
n	burning rate pressure exponent

# LIST OF SYMBOLS (cont'd)

$p$	pressure
$Q$	heat of decomposition
$Q_f$	heat release in the gas
$r$	burning rate
$R$	gas constant
$R$	response function
$t$	time
$T$	temperature
$u$	gas velocity normal to the surface
$V_3$	defined in Equation 50
$V_5$	defined in Equation 32
$V_{6A}$	defined in Equation 50
$V_{6B}$	defined in Equation 50
$W$	weight fraction
$x$	distance into the solid
$x^*$	effective flame height, defined by Equation 24
$y$	dimensionless distance $x$ , defined in Equation 3
$y_S$	time-dependent surface position, defined in Equation 29
$y^*$	dimensionless flame height, defined in Equation 20
$z$	defined in Equation 16
$Z$	defined in Equation 5b
$\Delta y$	thickness of a particular layer, see Equation 18
$\epsilon$	an extremely small number, see Equation 38b



# LIST OF SYMBOLS (Cont'd)

$\xi$	dimensionless distance $x$ , defined in Equation 19
$\eta$	defined by Equation 7
$\theta$	Defined in Equation 32
$\kappa$	thermal diffusivity
$\lambda_1, \lambda_2$	defined in Equation 36
$\xi$	defined by Equation 6
$\rho$	density
$\tau$	normalized temperature $T$ , defined in Equation 3
$\tau_F$	defined in Equation 41
$x$	defined in Equation 32
$\omega$	angular frequency of oscillations
$\Omega$	dimensionless angular frequency, defined in Equation 26

## Superscripts

'	perturbed value
-	mean value

## Subscripts

$a$	AP
$b$	binder
$f$	flame
$g$	gas
$m$	melt
$N$	Nth AP layer
$o$	deep solid
$s$	propellant
Top	upper side of boundry or interface
$w$	wall or surface

SECTION I  
INTRODUCTION

Experimental data have established that ammonium perchlorate (AP) particle size has a significant effect upon the pressure-coupled response function of composite solid propellants (1-14). Moreover, the effect cannot be attributed

1. Green, L.G., "Effects of Oxidizer Concentration and Particle Size on Resonance Burning of Composite Solid Propellants", Jet Prop. 28, 159-164 (Mar., 1958).
2. Strand, L. D., "Low Pressure L\* Instability and Extinction", 3rd ICRPG Combustion Conference (CPIA Publication 138, Vol. I, Feb., 1967) pp. 195-207.
3. "Experimental Studies on the Oscillatory Combustion of Solid Propellants", Report NWC-TP-4393, U.S. Naval Weapons Center, China Lake, CA (Mar., 1969).
4. Beckstead, M.W., Boggs, T.L. and Madden, O.H., "The effect of Oxidizer Particle Size and Binder Type on Nonacoustic Instability", AIAA Paper 69-175 (1969).
5. Boggs, T.L. and Beckstead, M.W., "Failure of Existing Theories to Correlate Experimental Nonacoustic Combustion Instability Data", J. AIAA 8, 626-631 (Apr. 1970).
6. Crump, J.E., "Combustion Instability in a Series of AP-HTPB Smokeless Propellants", 8th JANNAF Combustion Meeting (CPIA Publication 220, Vol. II, Dec. 1971) pp. 81-90.
7. Crump, J.E., "Combustion Instability Studies on Non-metallized AP-HTPB Propellants", 9th JANNAF Combustion Meeting (CPIA Publication 231, Vol. III, Dec., 1972) pp. 123-134.
8. Wendelken, C.P., "Combustion Stability Characteristics of Solid Propellants", AFRPL-TR-73-63, Air Force Rocket Propulsion Laboratory, Edwards, CA (Oct., 1973).
9. "Aluminum Behaviour in Solid Propellant Combustion", AFRPL-TR-74-13, Lockheed Propulsion Company, Redlands, CA (May, 1974).
10. Micheli, P.L., "Stabilization of Smokeless Propellants with Additives", 11th JANNAF Combustion Meeting (CPIA Publication 261, Vol. III, Dec., 1974) pp. 123-136.
11. Anderson, F.A. and Kumar, R.N., "Feasibility Study of Propellants and Igniters for Shuttle Solid Rocket Booster Separation Motors", Report 900-710, Jet Propulsion Laboratory, Pasadena, CA (June, 1975).

(See next page for remainder of references.)

simply to changes in burning rate or formulation; the effect appears to involve the composite propellant heterogeneity as well (15). Classical theories of combustion driving (16) have assumed a homogeneous propellant and are therefore inadequate to fully explain the combustion instability characteristics of composite propellants. The community has come to rely upon experimental measurement of the combustion response in T-Burners, and work in recent years has been devoted largely to improving the method (17-19). Although experimental measurement serves several important purposes, interest in the theoretical work has revived because the acquisition and interpretation of full complements of data continues to be expensive and does not furnish a phenomenological mechanism for the guidance of propellant R & D.

Viewing the combustion zone as the region between the thermal wave penetration

12. Cohen, N.S., et al., "Design of a Smokeless Solid Rocket Motor Emphasizing Combustion Stability", 12th JANNAF Combustion Meeting (CPIA Publication 273, Vol. II, Dec. 1975) pp 205-220.
13. Horton, M.D. and Rice, D. W., "The effects of Compositional Variables Upon Oscillatory Combustion of Solid Rocket Propellants", Combustion and Flame 8, 21-28 (Mar. 1964).
14. "Control of Solids Distribution in HTPB Propellants", Contract F04611-76-C-0006, Hercules, Inc., Allegheny Ballistics Laboratory, Cumberland, MD. (in progress).
15. Cohen, N. S., "Report of Workshop on Combustion Instability of Smokeless Propellants", Proceedings of 14th JANNAF Combustion Meeting (to be published).
16. Culick, F.E.C., "A Review of Calculations for Unsteady Burning of a Solid Propellant", J. AIAA 6, 2241-2254 (Dec. 1968).
17. "T-Burner Testing of Metallized Solid Propellants", AFRPL-TR-74-28, edited by F.E.C. Culick, Air Force Rocket Propulsion Laboratory, Edwards, Calif. (Oct. 1974).
18. "T-Burner Motor Verification Program Final Report", AFRPL-TR-74-71, Aerojet Solid Propulsion Company, Sacramento, Calif. (Jan. 1975).
19. Lovine, R.L. and Linfor, J.J., "Measurement of Propellant Response at High Frequency", 13th JANNAF Combustion Meeting (CPIA Publication 281, Vol. II, Dec. 1976) pp 95-112.

in the solid and the location of the flames in the gas, there are several ways in which the composite propellant heterogeneity can manifest itself. Two schools of thought have arisen: one which emphasizes the solid phase, treating the gas as a homogeneous source of propellant heating; and one which emphasizes the gas, continuing to treat the solid as a homogeneous medium.

The solid phase proponents may be represented by Lengelle & Williams (20), Kumar (21) and Cohen (12). Lengelle & Williams performed a one-dimensional analysis of a solid having sinusoidal thermal properties. Although the model was too idealized for direct practical application, it made the essential point that the heterogeneity augments the combustion response depending upon the periodicity of the thermal properties (and, therefore, particle size and spacing). Kumar introduced a surface melt layer, purportedly representative of the AP surface, in an otherwise homogeneous solid. The most significant result of this model was a mechanism by which zero-exponent propellants could exhibit a positive combustion response and pressure effects<sup>1</sup>. Since Kumar did not treat in-depth heterogeneity, particle size effects appeared in the solid only through the effect of burn rate on melt layer thickness<sup>2</sup>. Cohen postulated two characteristic parameters for the solid phase,

1. Classical theories produce a response function proportional to pressure exponent, yet it is well known that plateau (zero exponent) and mesa (negative exponent) propellants have exhibited combustion instability. The AP melt may be analogous to the foam zone of such propellants.
2. An effect of burn rate on melt layer thickness would also appear in double-base propellants, so it cannot be the sole basis for the role of AP particle size in composite propellants. Furthermore, AP size effects persist at constant burning rate when catalysts are used or solids loading or distribution are varied.

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20. Williams, F.A., and Lengelle, G., "Simplified Model for Effect of Solid Heterogeneity on Oscillatory Combustion", *Astronautica Acta* 14, 97-118 (1968).

21. Kumar, R.N., "Some Considerations in the Combustion of AP/Composite Propellants", Report under Contract NAS7-100, Guggenheim Jet Propulsion Center, California Institute of Technology, Pasadena, Calif. (Aug. 1972).



each dependent upon particle size. One was a measure of frequency response, the other of thermal response. He assumed that all response function curves could be determined by the pressure exponent plus these two parameters, and used experimental data for a standard propellant as calibration. The essential result is that decreasing particle size increases the peak response and shifts the peak to higher frequency. He further assumed that all multimodal propellants could be treated by linear superposition of the constituent results, and predicted multi-peaked response functions. Although the method is not founded upon a formal analysis, it is being used to guide propellant tailoring (15,22). Extensive applications have revealed some qualitative and quantitative deficiencies, for example, a tendency to over-emphasize the effect of fine sizes (22).

The gas phase proponents may be represented by Hamann (23), Glick and Condon (24), and Beckstead (25). All utilize some form of the "BDP" model of steady-state combustion (26) to represent the gas phase details, and none consider the solid to be heterogeneous. Hamann performed a perturbation analysis upon the entire BDP model, but did not report any results. Beckstead used the BDP model to calculate values for the parameters which are called for by the homogeneous theory of Denison & Baum (27). This approach of combining unrelated models is

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22. Glick, R.L., Private Communications, Thiokol Corp., Huntsville, Ala. (1977).
  23. Hamann, R.J., "Three Solid Propellant Combustion Models, A Comparison and Some Application to Non-Steady Cases", Memo. M-215, Delft University of Technology, Delft, Netherlands (Apr. 1974).
  24. Condon, J. A., Osborn, J.R. and Glick, R.L., "Statistical Analysis of Poly-disperse, Heterogeneous Propellant Combustion: Nonsteady-state", 13th JANNAF Combustion Meeting (CPIA Pub. 281, Vol. II, Dec. 1976) pp 209-223.
  25. Beckstead, M. W., "Combustion Calculations for Composite Solid Propellants", *ibid.*, 299-312.
  26. Beckstead, M.W., Derr, R.L. and Price, C.F., "Model of Solid Propellant Combustion Based on Multiple Flames", J. AIAA 8, 2200-2207 (Dec. 1970).

(See next page for remainder of references.)

open to question (15), and a review of the technique reveals several deficiencies<sup>3</sup>. Glick and Condon employed a similar approach, but used a modified BDP model (28) for polydisperse particle size distributions and the method of Zeldovich and Novozhilov (29) as an alternative to the theory of Denison & Baum. Comparison of results with experimental data was disappointing. Considerable improvement was noted, however, when the Cohen postulates were incorporated into the method to position the peak response and peak response frequency (24).

The following consensus appears to emerge from this background. First, there is a need to account for the melt layer and the in-depth solid phase heterogeneity of composite propellants. Second, there is a need to provide an analytical basis to test, confirm or modify the Cohen postulates. Third, the representation of the gas phase also should address the heterogeneity of composite propellants by embodying some form of the BDP model rather than the homogeneity of the classical theories. Accordingly, it was the objective of this program to develop an analytical model of the combustion response of composite solid propellants with particular attention to these contributions of the propellant heterogeneity. Primary emphasis was placed on the modeling of heterogeneity in the solid phase.

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3 For example, calculation of the "A" and "B" parameters of the homogeneous theory by this method reveals much too small a pressure effect to account for measured changes in the response function curve with pressure. As with Kumar, particle size effects appear only through changes in steady-state burning rate properties.

- 
27. Denison, M. R. and Baum, E., "A Simplified Model of Unstable Burning in Solid Propellants", J. ARS 31, 1112-1122 (Aug. 1961).
28. Glick, R.L. and Condon, J.A., "Statistical Analysis of Polydisperse, Heterogeneous Propellant Combustion: Steady-State", 13th JANNAF Combustion Meeting, (CPIA Pub. 281, Vol. II, Dec. 1976) pp 313-345.
29. Novozhilov, B. V., "Nonstationary Combustion of Solid Rocket Fuels", Nauka, Moscow (1973).

## SECTION 2

### MODEL PREMISES AND ASSUMPTIONS

#### 2.1 REPRESENTATION OF THE SOLID PHASE

The solid phase is represented by a "sideways sandwich", following the concept of Lengelle & Williams, as shown in Figure 1. This picture, really, does nothing more than state that the analysis is one-dimensional, so its dissimilarity to real propellants is of no greater concern than is the use of a one-dimensional treatment. Such a treatment assumes that the lateral processes are negligible in comparison to the normal processes. The solid is considered to be semi-infinite, having alternating layers of AP and binder. The thickness of the AP layers is nominally equal to the particle size, with exceptions to be noted later. The thickness of the binder layers is equal to the interstitial spacing as determined from the statistical geometry (26, 30). The surface AP layer contains a thin melt layer, which is justified experimentally (31-33), and follows the model of Kumar as a region of decomposition reactions in accordance with an Arrhenius law. The melt layer is "thin" in that the melting point of AP approximates the surface temperature during deflagration (32, 33). The analysis is linearized for small harmonic pressure perturbations, and is concerned with pressure-coupling only.

30. Cohen, N.S., Price, C.F. and Strand L.D., "Analytical Model of the Combustion of Multicomponent Solid Propellants", AIAA Paper 77-927, AIAA/SAE 13th Propulsion Conference (July, 1977).
31. Boggs, T.L., "The Decomposition, Pyrolysis and Deflagration of Ammonium Perchlorate", et seq., 7th JANNAF Combustion Conference (CPIA Publication 204, Vol. I, 1971) pp 113-138.
32. Guirao, C. and Williams, F.A., "A Model for Ammonium Perchlorate Deflagration Between 20 and 100 atm", J. AIAA 9, 1345-1356 (July 1971).
33. Beckstead, M.W. and Hightower, J.D., "Surface Temperature of Deflagrating Ammonium Perchlorate Crystals", J. AIAA 5, 1785-1790 (Oct. 1967).

Although the model contains the convective heating term to represent the regression of the material at the mean rate  $\bar{r}$ , the geometry of the layers is taken to be fixed with the AP layer always at the surface. This assumption is similar to the statistically fixed geometry used in the BDP model. One consequence of this assumption is that the "pulsation" mechanism associated with the sequential burn through of individual crystals and binder layers is excluded. The existence of a "pulsation" mechanism, coherent over microscopic regions of propellant surface, is open to question, although Lengelle & Williams (20) offer an argument in its favor. Thus, the present model examines only the effect of heterogeneity in relation to the thermal wave propagation through the solid propellant. A consequence of this assumption is that in-depth heterogeneity will not be important in those cases where the particle size is larger than the thermal wave (generally, coarse particles and high burn rate). Whether or not this consequence is unduly restrictive remains to be seen, but the fact that catalyzed coarse propellants are more stable than fine propellants would seem to permit it. The statistically fixed geometry requires the surface AP layer (including the melt) to have a thickness  $\sqrt[2]{3}$  of the particle size (26).

## 2.2 REPRESENTATION OF THE GAS PHASE

The function of the gas phase in the analytical scheme is to transform the oscillating pressure into an oscillating heat flux boundary condition at the surface of the AP melt. An approximate form of the BDP model has been selected to represent the gas phase, and the gas phase is assumed to be quasi-steady (viz, the gas phase responds instantly to changes in pressure). The approximation assumes a single flame above the propellant surface, where all gas phase reactions occur, as illustrated by Figure 1.



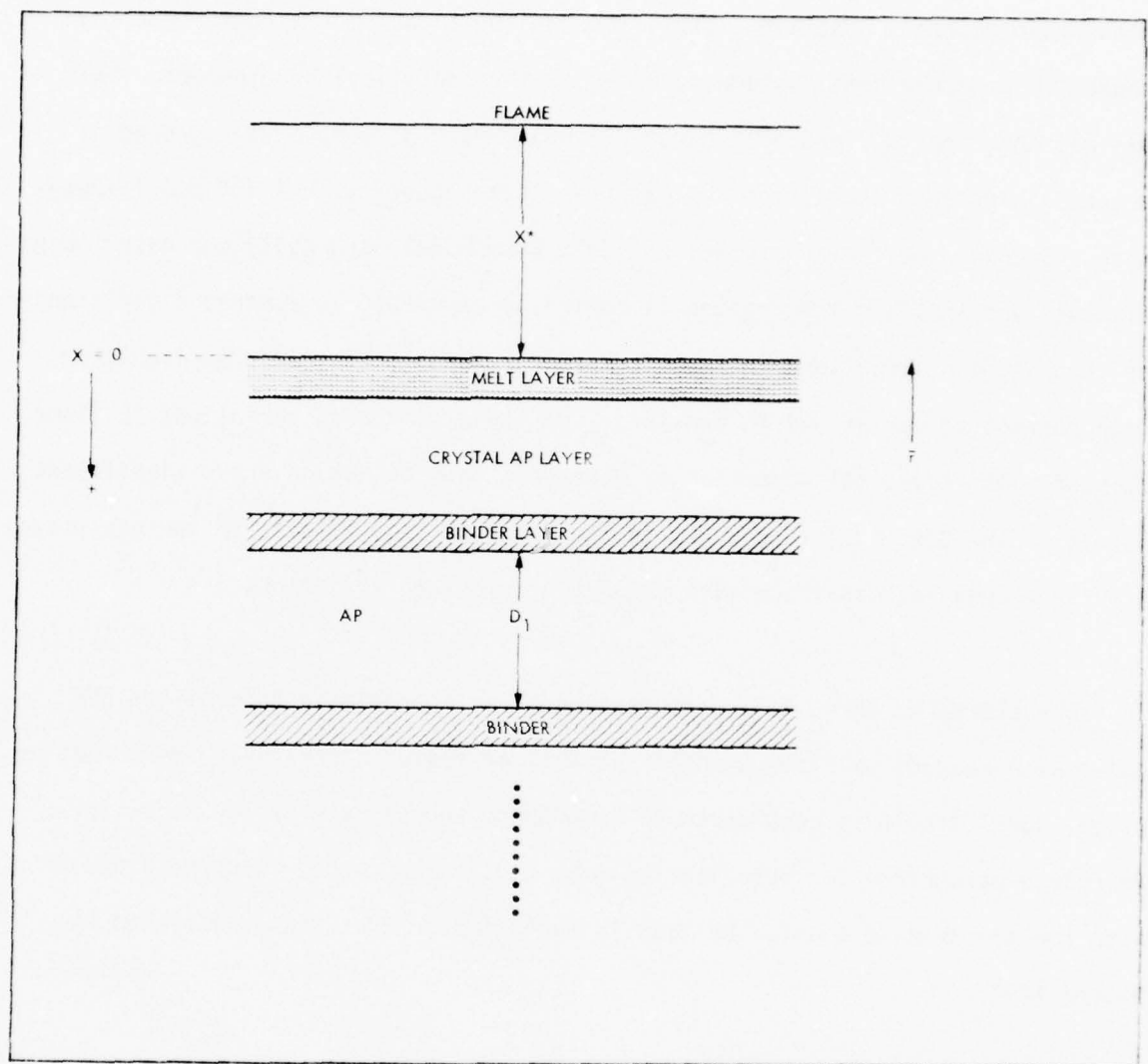


Figure 1. Physical Model Representation

Presuming that the condensed phase heterogeneity has the dominant effect upon the response function of composite propellants, it would not seem to matter what particular model were chosen to represent the gas so long as it provides a reasonable boundary condition. Thus, the Denison & Baum model could have been chosen to preserve some systematic order to the analytical development. This was not done for two reasons: First, it would have presumptuously ignored those developments addressing the gas phase heterogeneity in a BDP model framework. Second, the fact that the Denison & Baum model is heavily dependent upon fluctuations in flame temperature is coming to be viewed as a serious deficiency of that model. Variations in flame temperature are fourth order in magnitude with respect to variations in pressure. On the other hand, variations in flame standoff, which are not addressed by Denison & Baum but which are a significant aspect of the BDP model (and a key to the particle size effects in the gas phase), are first order of magnitude with respect to pressure variations.

The approach, then, is a perturbation of an approximate form of the BDP model with respect to flame standoff as well as flame temperature. Perturbation of the model itself is considered to be proper, whereas use of the model to calculate parameters for substitution into a different model is open to question. With the approximate model, the task is much simpler than that undertaken by Hamann (23).

### 2.3 REPRESENTATION OF MULTIMODAL PROPELLANTS

Multimodal propellants are represented by adjacent columns of layers, as shown by Figure 2. Each particle size, corrected by the factor  $\sqrt[3]{2/3}$ , tops a column. The remaining AP layers consist of the finest size in the distribution.

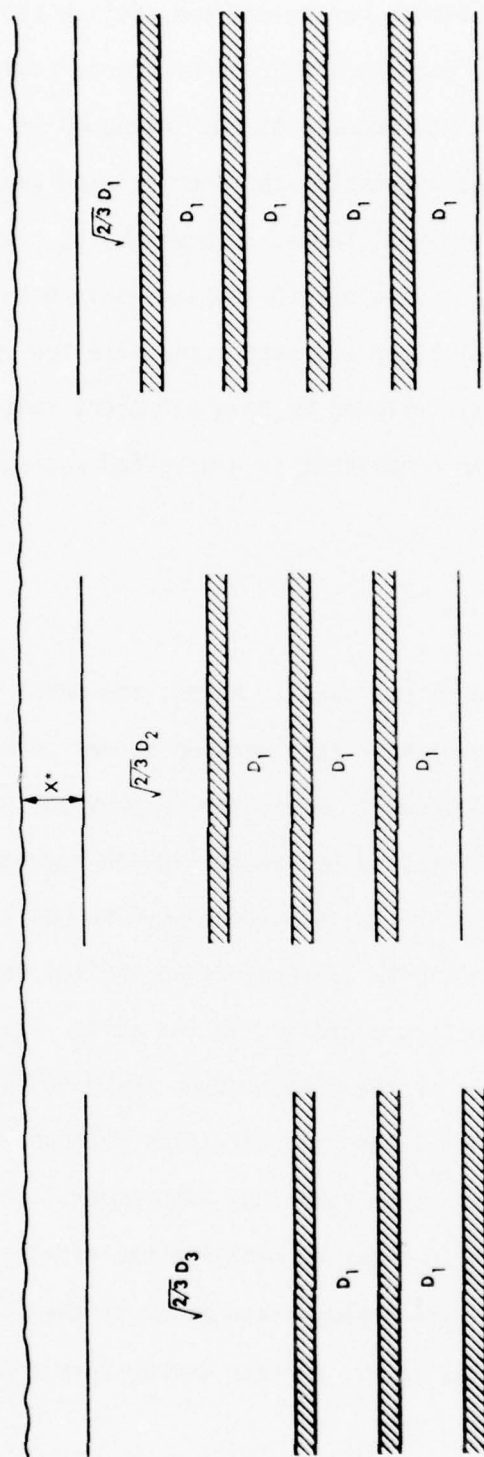


Figure 2. Layered Model of the Solid Phase for a Trimodal Propellant:  
 Sizes  $D_1$ ,  $D_2$ ,  $D_3$ . Shaded Layers are Binder. The Top of the  
 Surface AP Layer is a Thin Melt

This assumption is justified by the fact that the finest size will fill the smallest interstices between coarser particles, and will be valid so long as the thermal wave does not penetrate to a subsequent coarse sublayer. Validity is likely in practical propellants because of the influence of the fine size in raising the burning rate and decreasing the thermal wave penetration. The binder layers are all of the same thickness, as computed by the method of Ref. (30). All of the columns are constrained to the same mean burning rate, which implies one effective flame height or characteristic size for the diffusion flame. However, the columns are allowed to have different response functions and the aggregate value for the propellant is a weighted average from the constituent columns.

#### 2.4 APPROACH

The analysis is performed in two parts. First, the model is derived in its steady-state version. The steady-state version serves to calculate mean values required for the time-dependent model, verify that the boundary conditions will be reasonably accurate as measured by the ability to reproduce experimental (or formal BDP) results, establish the zero-frequency (no oscillation) limit, verify some of the model assumptions, and provide an initial check on the method of solving for the temperature profile in the solid. The steady-state model is one of the subroutines of the computerized response function model. Secondly, the time-dependent model for the combustion response function is derived. In calculating the response function, experimental values of mean burning rate are used as input in order to minimize the effects of uncertainties in the steady-state modeling. The steady-state model is then limited to calculation of other steady-state quantities (e.g., surface temperature and flame height).

### SECTION 3

#### THE STEADY-STATE MODEL

#### 3.1 SOLID PHASE EQUATIONS

The heat conduction equation in the melt layer is written as:

$$k_a \frac{d^2T}{dx^2} + \rho_a c_a r \frac{dT}{dx} = W_a \rho_a Q_a A \exp(-E/RT) \quad (1)$$

where  $k$  = thermal conductivity

$\rho$  = density

$c$  = heat capacity

$W$  = weight fraction

$Q$  = heat of decomposition

subscript  $a$  = denotes AP

$A$  = kinetics prefactor

$E$  = activation energy

$R$  = gas constant

$r$  = burning rate

$T$  = temperature

$x$  = distance into the solid

The boundary conditions are:

$$x = 0, -k_a \frac{dT}{dx} = \rho_s c_s r (T_w - T_o) + W_a \rho_s r (Q_a + Q_m) \quad (2a)$$

$$x = x_m, -k_a \frac{dT}{dx} = \rho_s c_s r (T_m - T_o) + W_a \rho_s r Q_m \quad (2b)$$

where subscript  $w$  = denotes wall or surface

subscript  $s$  = denotes mean propellant

subscript  $m$  = denotes melt

subscript  $o$  = denotes the deep solid

Equation (1) may be written in dimensionless form as follows:

$$\frac{d^2\tau}{dy^2} + \frac{d\tau}{dy} = B \exp \left[ \frac{-E/RT_w}{\left(\frac{T_w - T_0}{T_w}\right)(\tau - 1) + 1} \right] \quad (3)$$

$$\text{where } \tau = (T - T_0)/(T_w - T_0)$$

$$y = \frac{r}{\kappa} x$$

$\kappa$  = thermal diffusivity of the medium,  $\kappa_a$  for Eq. (3)

$$B = A \frac{\kappa_a}{r^2} H_a \frac{c_s}{c_a}$$

$$H = \frac{WQ}{c_s (T_w - T_0)}$$

In the thin melt layer,  $\tau \approx 1$ , so Eq. (3) may be approximated as:

$$\frac{d^2\tau}{dy^2} + \frac{d\tau}{dy} = C \exp [-D(1-\tau)] \quad (4)$$

$$\text{where } C = B \exp(-E/RT_w)$$

$$D = \frac{E}{RT_w^2} (T_w - T_0) \quad \left\{ \right.$$

The boundary conditions become:

$$\text{surface: } y = 0, \quad \frac{d\tau}{dy} = -Z_a (1 + H_a + H_m) \quad (5a)$$

$$\text{melt/crystal: } y = y_m, \quad \frac{d\tau}{dy} = -Z_a (\tau_m + H_m) \quad (5b)$$

$$\text{where } Z_a = \frac{\rho_s c_s}{\rho_a c_a}$$

Making the following transformation:

$$\xi = \tau + \frac{d\tau}{dy} \quad (6)$$

$$\eta = D(1-\tau) \quad (7)$$



Eq. (4) becomes:

$$(\xi - 1 + \eta/D) \frac{d\xi}{d\eta} = \frac{-C}{D} \exp(-\eta) \quad (8)$$

Recognizing  $\eta/D \ll 1$  where  $\tau \approx 1$ , and letting  $K = \frac{C}{D}$ , Eq. (8) becomes:

$$-\xi \frac{d\xi}{d\eta} + \frac{d\xi}{d\eta} = K \exp(-\eta) \quad (9)$$

Eqs. (5a & b) become:

$$\eta=0, \quad \xi = \xi_w = 1 - Z_a(1 + H_a + H_m) \quad (10a)$$

$$\eta=\eta_m, \quad \xi = \xi_m = \tau_m - Z_a(\tau_m + H_m) \quad (10b)$$

Eq. (9) may be integrated in closed form. Applying Eqs.(10) and some algebra yields an expression for burning rate in the following form:

$$K = \frac{\xi_w \left( \frac{\xi_w}{2} - 1 \right) - \xi_m \left( \frac{\xi_m}{2} - 1 \right)}{1 - \exp(-\eta_m)} \quad (11)$$

Making all substitutions, burning rate is expressed as a function of wall temperature and other constants as follows:

$$r^2 = \frac{2 \kappa_a A W_a Q_a R T_w^2}{C_a (T_w - T_0) E (T_w - T_0)} \exp\left(-\frac{E}{RT_w}\right) \frac{\left[ 1 - \exp\left(-\frac{E}{RT_w} \frac{T_w - T_m}{T_w}\right) \right]}{\left\{ Z_a \left[ 1 + \frac{W_a (Q_a + Q_m)}{c_s (T_w - T_0)} \right] \right\}^2 - \left\{ \left( \frac{T_m - T_0}{T_w - T_0} \right) (1 - Z_a) - Z_a \frac{W_a Q_m}{c_s (T_w - T_0)} - 1 \right\}^2} \quad (12)$$

This relation is to be matched with a relation between burn rate and wall temperature from the gas phase model.

Analysis of the steady-state problem and, as will appear later, solution of the time-dependent problem, also require a description of the steady-state temperature profile in the solid. The temperature profile in the melt layer is determined from Eq. (9). Integration and application of Eq.(10a) yields:

$$\xi = 1 \pm \sqrt{1 + 2[K \exp(-\eta) - C_M]} \quad (13)$$

$$\text{where } C_M = K - \frac{1}{2} [1 - Z_a(1 + H_a + H_m)]^2 + 1 - Z(1 + H_a + H_m)$$

The physics of the temperature decay requires the negative root. Substituting the definitions for  $\xi$  and  $\tau$  yields:

$$\frac{d\eta}{dy} = -\eta + D \sqrt{1 + 2[K \exp(-\eta) - C_M]} \quad (14)$$

An order of magnitude analysis shows that the square root term will always be much larger than  $\eta$  in the melt layer. Thus, Eq. (14) reduces to the form:

$$\frac{d\eta}{\sqrt{a + b \exp(-\eta)}} = D dy \quad (15)$$

$$\text{where } a = 1 - 2C_M$$

$$b = 2K$$

This equation can be integrated in closed form for  $y(\eta)$ ; it is transcendental as  $\eta = \eta(y)$ .

$$y = \frac{-1}{D\sqrt{a}} \ln \left[ \frac{1+z - \sqrt{z^2 + 2z}}{1+d - \sqrt{d^2 + 2d}} \right] \quad (16)$$

$$\text{where } d = 2a/b$$

$$z = d \exp(\eta)$$

The melt layer thickness may be calculated by evaluating Eq. (16) at  $\eta = \eta_m$ .

For all layers beneath the melt layer, the right-hand-side of Eq. (3) vanishes. The gradient condition at the top of each layer is similar to Eq. (5b), without the heat of fusion.

$$y = y_{\text{Top}}, \quad \frac{d\tau}{dy} = -Z \tau_{\text{Top}} \quad (17)$$

where  $Z = Z_a$  when entering an AP layer

$Z = Z_b$  when entering a binder layer



Thus the temperatures in each layer beneath the melt layer follow the recurring form:

$$\tau = \tau_{\text{Top}} - Z \tau_{\text{Top}} [1 - \exp(-\Delta y)] \quad (18)$$

where  $\Delta y$  = thickness of the particular layer, and uses the appropriate  $\kappa$ .

For a homogeneous propellant,  $Z=1$ , so Eq. (18) properly reduces to the result for a homogeneous propellant. Note also that the temperature and the gradient will properly tend to zero together, as  $y$  approaches infinity.

### 3.2 GAS PHASE EQUATIONS

If it is assumed that all reactions occur at the flame height, the heat conduction equation has the form of Eq. (1) with a zero right-hand-side. Taking the flame to be at  $x=0$  and the wall at the flame height ( $x=x^*$ ), the temperature distribution is:

$$T = T_f - (T_f - T_w) \frac{1 - \exp(-\zeta)}{1 - \exp(-\zeta^*)} \quad (19)$$

where  $\zeta = ux/\kappa_g$

$u$  = gas velocity normal to the surface

subscript  $g$  = denotes gas

subscript  $f$  = denotes flame

For convenience,  $\zeta$  is set equal to  $y$  by employing the continuity relation,  $\rho_g u = \rho_s r$ , and assuming that the ratio of heat capacity to thermal conductivity is equal for gas and solid<sup>4</sup>. Then the gradient at the wall may be written, from differentiation of Eq. (16), as:

$$y=y^*, \frac{dT}{dy} = - (T_f - T_w) \frac{\exp(-y^*)}{1 - \exp(-y^*)} \quad (20)$$

where  $y^* = \frac{rx^*}{\kappa_s}$

<sup>4</sup> This assumption is comparable to the general assumption that these properties are temperature-insensitive. The conductivities of propellant gases may be calculated, but are not well-known.

At the same time, the gradient at the wall must satisfy the energy requirements of the condensed phase:

$$-k_g \frac{dT}{dx} = \rho_s c_s r (T_w - T_o) + W_a \rho_s r (Q_a + Q_m) + W_b \rho_s r Q_b \quad (21)$$

where subscript b = denotes binder.

Eq. (21), when compared to Eq. (2a), states that the binder heat of decomposition is being positioned on the gas side of the wall. The binder does not appear at the surface in the model of Fig. 1, but does in reality exist over portions of the surface. The model surface is the AP melt. Therefore, in the framework of this model, the decomposing binder is external to the melt layer so may be represented by a heat absorption on the gas side. Eq. (21) may be re-written as:

$$y = y^*, -\frac{dT}{dy} = (T_w - T_o) + F \quad (22)$$

$$\text{where } F = (H_a + H_m + H_b)(T_w - T_o)$$

Equating Eq. (20) and Eq. (22) yields:

$$T_w = (T_f + F - T_o) \exp(-y^*) - (F - T_o) \quad (23)$$

which is the required matching relation in burn rate and wall temperature.

The remaining unknown,  $x^*$ , is determined by an approximate fit of the effective flame height from the BDP model:

$$x^* = C_F \frac{r D_1}{p} \quad (24)$$

where  $D_1$  = particle size

$p$  = pressure

$C_F = 24.6$  for  $r$  in cm/sec,  $p$  in atmospheres,  $D_1$  in microns and  $x^*$  in microns.

This form does not take into consideration the relative importance of the components of the BDP multiple flame structure and their differing dependencies upon the parameters of Eq. (21). However, it is a reasonable representation selected for mathematical convenience and with the perturbation analysis in mind.

After substitution of Eq. (21) into Eq. (18), Eqs. (12) and (20) are two equations for the unknowns  $r$  and  $T_w$ . These equations are solved by iteration. Once  $r$  and  $T_w$  are known, it is possible to calculate the melt layer thickness and the thermal profile in the solid.

The steady-state model is not intended to be used to calculate burning rates for multimodal propellants. That would require some definition of an effective particle size or flame height for use of Eq. (4). Rather, experimental values of burning rate are used to determine the wall temperature from the solid phase model, whence the effective flame height and particle size may be determined from the gas phase model. This is the general method for determining the mean values for use in the response function model. An option is provided to predict these values for unimodal propellants, but is used in this work only to validate aspects of the modeling. Those results are discussed in Section 5.

Note that the effects of particle size appear only as gas phase effects in the steady-state model. This conforms with a generally-accepted view of steady-state combustion (34). Although Eq. (12) (from the solid phase) may influence the magnitude of the particle size effect, particle size does not appear in that equation. The thermal profile in the solid does not enter into the calculation for mean burning rate. However, this does not preclude the importance of solid phase effects in determining the role of particle size in the time-dependent model for the response function.

34. Derr, R.L., "Review of Workshop on Steady State Combustion Modeling of Composite Solid Propellants", 7th JANNAF Combustion Meeting (CPIA Publication 204, Vol. 1, 1971) pp 1-8.

## SECTION 4

### THE TIME-DEPENDENT MODEL: CALCULATION OF THE RESPONSE FUNCTION

#### 4.1 SOLID PHASE EQUATIONS

Using dimensionless quantities as previously defined, the time-dependent heat conduction equation in the thin melt layer is written as:

$$\frac{\partial^2 \tau}{\partial y^2} + \frac{\partial \tau}{\partial y} - \frac{\kappa a}{r^2} \frac{\partial \tau}{\partial t} = C \exp[-D(1-\tau)] \quad (25)$$

Eq. (25) is the time-dependent form of Eq. (4). Denoting mean values as barred and perturbed values as primed, and employing Eq. (4) to describe the mean portion, Eq. (25) may be written as:

$$\frac{\partial^2 \tau'}{\partial y^2} + \frac{\partial \tau'}{\partial y} - \Omega \frac{\partial \tau'}{\partial (\omega t)} = C \exp(\bar{\eta}) [\exp(D\tau') - 1] \quad (26)$$

where  $\omega$  = frequency of oscillations

$$\Omega = \frac{\kappa}{r^2} \omega$$

For harmonic perturbations,  $\tau' = \exp(i\omega t)$ , the time-dependent term of Eq. (26) may be re-written to provide an ordinary differential equation:

$$\frac{d^2 \tau'}{dy^2} + \frac{d\tau'}{dy} - i\Omega \tau' = C \exp(-\bar{\eta}) [\exp(D\tau') - 1] \quad (27)$$

If  $\tau'$  is of second order of magnitude and  $\Omega$  sufficiently small, Eq. (27) may be approximated as:

$$\frac{d^2 \tau'}{dy^2} + \frac{d\tau'}{dy} = CD\tau' \exp(-\bar{\eta}) \quad (28)$$

The problem is linearized to small perturbations, and is therefore restricted to linear instability. Variations in burning rate are of the order of variations in pressure, but variations in surface temperature are second or third order with respect to variations in burning rate. Thus, for second-order pressure perturbations,  $\tau'$  is at most of third order. The exponential in  $\bar{\eta}$  is approximately unity in the melt layer, and the product  $CD$  is of the order  $10^2$ . This would permit frequencies as high as 10KHz to satisfy the approximation for cases of interest. Since the quasi-steady assumption for the gas-phase model will also restrict the frequencies to values less than 10KHz, use of Eq. (28) is consistent with that assumption.

In applying the boundary conditions at the surface, one must recognize that the surface is fluctuating relative to the mean surface ( $y=0$ ) position. Since the fluctuating burning rate will also be of the form,  $\exp(i\omega t)$ , in the linearized problem, it follows that the surface position is given by:

$$y_S = -\frac{i}{\Omega} \frac{r'}{\bar{r}} \quad (29)$$

The boundary conditions are:

$$y = y_S, \quad \tau' = \tau'_w \quad (30a)$$

$$\frac{d\tau'}{dy} = Z_a \left( g'_w + \frac{r'}{\bar{r}} H_b \right) \quad (30b)$$

where  $g'_w$  = the gradient in  $\tau'$  at the surface, on the negative (gas) side of the boundary.

Eq. (30b) is derived by substituting Eq. (2a) into Eq. (21), and perturbing in the non-dimensional form. For small perturbations, the quantities at the actual surface may be related to the quantities at the mean surface as:



$$y = y_S, \quad \tau' = \tau'|_{y=0} - \frac{i}{\Omega} \frac{r'}{\bar{r}} \bar{g}|_{y=0} \quad (31a)$$

$$\frac{d\tau'}{dy} = g'|_{y=0} - \frac{i}{\Omega} \frac{r'}{\bar{r}} \frac{d\bar{g}}{dy}|_{y=0} \quad (31b)$$

where  $\bar{g}$  = the gradient in  $\bar{\tau}$

Eq. (28) is integrated numerically. The functions  $\exp(-\bar{\eta})$  and  $\bar{g}$  are available in terms of  $y$  from Eq. (16). The integration provides the mean surface values, which are then converted to the actual surface values by means of Eqs. (31). The actual surface values must satisfy Eqs. (30);  $g'_w$  is determined from the gas phase model, and  $\tau'_w$  is related to  $r'$  by perturbing Eq. (12). The perturbation of Eq. (12) yields:

$$\frac{r'}{\bar{r}} = V_5 \tau'_w \quad (32)$$

$$\text{where } V_5 = (1 + \frac{\theta}{2})\chi + \frac{D}{2} \frac{1 - 2\chi(1 - \tau_m)}{\exp[D(1 - \tau_m)] - 1} - \frac{1}{Z_a(1 + H_a + H_m) - \tau_m(1 - Z_a) + Z_a H_m + 1}$$

$$\theta = E/(RT_w)$$

$$\chi = (\bar{T}_w - T_0)/\bar{T}_w$$

Although the solution appears to require iteration, it will be shown subsequently that it does not (cf. Subsection 4.3).

For all layers beneath the melt layer, the right-hand-side of Eq. (27) vanishes so the time-derivative term cannot be neglected. Thus:

$$\frac{d^2\tau'}{dy^2} + \frac{d\tau'}{dy} - i\Omega\tau' = 0 \quad (33)$$

The boundary conditions at each interface are generally:

$$y=y_{\text{Top}}, \quad \tau'=\tau'_{\text{Top}} \quad (34a)$$

$$\frac{d\tau'}{dy} = \frac{Z_{a,b}}{Z_{b,a}} g'_{\text{Top}} \quad (34b)$$

where the first Z subscript is used when entering an AP layer and the second is used when entering a binder layer. Assuming that the product  $\rho c$  for the melt is equal to that for the solid AP, the ratio of Z does not appear for that first layer of solid AP which joins the melt. The  $g'_{\text{Top}}$  refers to that value of the perturbed gradient on the negative (upper) side of the boundary, which drives the behavior below. The  $\tau'_{\text{Top}}$ , however, is preserved on the positive side. Eq. (34b) is similar in form to Eq. (30b), but there is no phase change heat beneath the melt layer and the sublayers do not oscillate relative to the mean surface. Eq. (33) may be integrated to produce the following recurring formulas:

$$\tau'=\tau'_{\text{Top}} \exp(\lambda_1 \Delta y) - \frac{\lambda_1 \tau'_{\text{Top}} - \frac{Z_{a,b}}{Z_{b,a}} g'_{\text{Top}}}{\lambda_2 - \lambda_1} [\exp(\lambda_2 \Delta y) - \exp(\lambda_1 \Delta y)] \quad (35)$$

$$\frac{d\tau'}{dy} = \lambda_1 \tau'_{\text{Top}} \exp(\lambda_1 \Delta y) - \frac{\lambda_1 \tau'_{\text{Top}} - \frac{Z_{a,b}}{Z_{b,a}} g'_{\text{Top}}}{\lambda_2 - \lambda_1} [\lambda_2 \exp(\lambda_2 \Delta y) - \lambda_1 \exp(\lambda_1 \Delta y)] \quad (36)$$

$$\text{where } \lambda_1 = -\frac{1}{2} - \frac{1}{2} \sqrt{1+4i\Omega}$$

$$\lambda_2 = -\frac{1}{2} + \frac{1}{2} \sqrt{1+4i\Omega}$$

Each layer uses the appropriate ratio of Z, and the appropriate  $\kappa$  for  $\Delta y$ ,  $\lambda_1$  and  $\lambda_2$ .

Eqs. (35) and (36) properly reduce to the results for a homogeneous solid ( $Z=1$ , and the difference between  $g'$  and  $\lambda_1 \tau'$  vanishes throughout, leaving only the first term on the right-hand-side). However, these equations retain the growing exponential term (in  $\lambda_2$ , of positive real part) for the layered solid because the formulation of the problem does not explicitly impose the boundary condition at infinity upon each layer. This condition is the requirement that  $\tau'$  and  $d\tau'/dy$  vanish together. For the homogeneous solid, this condition would immediately set the exponential in  $\lambda_2$  equal to zero. For the layered solid, it can only be said that a layer will eventually be reached where this condition may be approximated for all practical purposes. Since the effect of the heterogeneity on the perturbations also disappears when the perturbations disappear, this approximate condition may be expressed in the form of the homogeneous solid:

$$\tau' \rightarrow 0, \frac{d\tau'}{dy} \rightarrow \lambda_1 \tau' \quad (37)$$

In other words, there is a depth below which the propellant can be treated as homogeneous for purposes of the perturbation problem. Consider that this occurs below the  $N^{\text{th}}$  AP layer. Then Eq. (37) may be expressed as:

$$y=y_N, \tau' = \epsilon \quad (38a)$$

$$\frac{d\tau'}{dy} = \lambda_{1s} \epsilon \quad (38b)$$

where  $\epsilon$  = an extremely small number

$\lambda_{1s}$  = value of  $\lambda_1$  using  $\kappa_s$  for the homogeneous region.

Eq. (38b) represents the perturbed gradient at the top of the homogeneous region, on the positive (homogeneous) side of the boundary with the  $N^{\text{th}}$  AP layer. This may be converted to the perturbed gradient on the negative (AP) side of the



boundary through use of Eq. (34b), recognizing that  $Z=1$  in the homogeneous region. Thus, Eqs. (38) become:

$$y = y_N, \quad \tau_{\text{TopN}}' = \epsilon \quad (39a)$$

$$g_{\text{TopN}}' = Z_a \lambda_{1s} \epsilon \quad (39b)$$

where subscript TopN = denotes the bottom of the  $N^{\text{th}}$  AP layer, which would be the "top" condition for the succeeding homogeneous region were the calculation to continue.

Thus, the problem of the solid phase is now properly closed. Eqs. (30) define the conditions at the "top", and Eqs. (39) define the conditions at the "bottom". The conditions at the bottom are now known, but the conditions at the top depend upon the gas phase. Additional discussion with respect to the solution for the solid phase is deferred to Subsection 4.3.

#### 4.2 GAS PHASE EQUATIONS

The perturbed form of Eq. (24) is simply:

$$\frac{x^{\star'}}{x^{\star}} = \frac{r'}{\bar{r}} - \frac{p'}{\bar{p}} \quad (40)$$

Since the analysis will take into account flame temperature perturbations, a relation between the flame temperature perturbations and the wall temperature perturbations is required. This is obtained by perturbation of Eq. (23). Using dimensionless quantities as previously defined, Eq. (40) for the flame standoff perturbations, and linearizing the exponential in perturbed quantities, there results:

$$\tau_f' = \tau_w' \exp(\bar{y}^{\star}) - (1 + \tau_f) \bar{y}^{\star} \exp(\bar{y}^{\star}) \left[ \frac{p'}{\bar{p}} - 2 \frac{r'}{\bar{r}} \right] \quad (41)$$

$$\text{where } \tau_F = \frac{F}{\bar{T}_w - T_0}$$

The perturbed gradient on the gas side of the wall is derived from an energy balance. The energy being transmitted into the solid is the difference between the heat release in the gas and the energy required to raise the gas from the wall temperature to the flame temperature:

$$-k_g \frac{dT}{dx} = -\rho_s r Q_f - c_g (T_f - T_w) \quad (42)$$

where  $Q_f$  = heat release in the gas (negative for an exotherm).

Using the same relation between gas and solid thermal properties as led to Eq. (20), Eq. (42) may be written in dimensionless form as follows:

$$\bar{q}_w = H_f + (\bar{\tau}_f - 1) \quad (43)$$

where  $\bar{q}_w$  = gradient in  $\bar{\tau}$  at the wall on the negative (gas) side

$$H_f = \frac{Q_f}{c_g (\bar{T}_w - T_0)}$$

The perturbed dimensionless form of Eq. (42) is:

$$q'_w = \frac{r'}{\bar{r}} [H_f + (\bar{\tau}_f - 1)] + (\tau'_f - \tau'_w) \quad (44)$$

$H_f$  may be eliminated by combining the relations in Eqs. (43), (5a) and (21)<sup>5</sup>.

5 For this purpose, Eq. (21) may be written as:  $d\bar{\tau}/dy = Z(\bar{q}_w + H_f)$ . This is the steady-state analog of Eq. (30b), and comes from substituting Eq. (2a) into Eq. (21) in dimensionless form.

$$H_F = -(\bar{\tau}_F - 1) - (1 + \tau_F) \quad (45)$$

Substitution into Eq. (44) yields:

$$g_W' = -\frac{r'}{\bar{r}} (1 + \tau_F) + (\tau_F' - \tau_W') \quad (46)$$

Substitution of Eq. (41) into Eq. (46) yields, after combining terms:

$$g_W' = \frac{r'}{\bar{r}} (1 + \tau_F) (2\bar{y}^* \exp(\bar{y}^*) - 1) + \tau_W' (\exp(\bar{y}^*) - 1) - \frac{p'}{\bar{p}} (1 + \tau_F) \bar{y}^* \exp(\bar{y}^*) \quad (47)$$

Eq. (47) is the necessary matching relation for Eq. (30b). Thus, the formulation of the time-dependent problem is complete.

Eq. (45) also may be substituted into Eq. (43) to yield:

$$\bar{g}_W = -(1 + \tau_F) \quad (48)$$

Eq. (48) is the dimensionless form of Eq. (22), so consistency is verified in this respect.

#### 4.3 SOLUTION FOR THE RESPONSE FUNCTION

By combination of Eqs. (30b), (31a), (31b), (32) and (47), it is possible to derive an explicit expression for the response function in terms of solid phase constants, gas phase constants and one key parameter characteristic of the solution for the solid phase. This key parameter is the ratio of the perturbed gradient to the perturbed temperature at the mean surface:

$$\left. \frac{g'}{\tau'} \right|_{y=0} \equiv K_2 \quad (49)$$

The components of this ratio appear individually in Eqs. (31), and the ratio is defined here as  $K_2$ . In the classical homogeneous theory, this ratio is always  $\lambda_1$ . In this work, the ratio will depend upon the modeled heterogeneity and  $\lambda_2$  as well as on  $\lambda_1$ .

The expression for the response function is:

$$R = \frac{\Omega_a V_{6B}}{\Omega_a \left[ \frac{V_{6A}}{V_5} + 2V_{6B} - \frac{V_3}{Z_a} \right] + i \frac{C}{Z_a} - \frac{K_2}{Z_a} \left[ \frac{\Omega_a}{V_5} - i V_3 \right]} \quad (50)$$

Where  $R$  = response function

$$V_3 = Z_a (1 + H_a + H_m) \text{ (see Eq. [5a])}$$

$$V_5 = \text{(see Eq. [32])}$$

$$C = \text{(see Eq. [4])}$$

$$V_{6A} = (\exp(\bar{y}^*) - 1) \text{ (see Eq. [47], appears as coefficient of } \tau_w')$$

$$V_{6B} = (1 + \tau_F) \bar{y}^* \exp(\bar{y}^*) \text{ (see Eq. [47], appears as coefficient of } p'/\bar{p} \text{ and as part of the coefficient of } r'/\bar{r}).$$

If the ratio  $K_2$  depended upon  $g_w'$  and  $\tau_w'$  separately, the problem would require an iterative solution. However, it turns out that  $K_2$  is an intrinsic property of the solid phase, independent of the surface boundary condition, just as is  $\lambda_1$  for the homogeneous solid. The reason is that the solid phase is described by linear homogeneous differential equations. All solutions of such equations of second order are of the form:

$$f = C_1 f_1(x) + C_2 f_2(x)$$

where  $f$  = denotes functions

$$C_1 = \text{first arbitrary constant}$$

$$C_2 = \text{second arbitrary constant}$$

The gradient is:

$$g = C_1 f_1'(x) + C_2 f_2'(x)$$

It is required that  $g/f$  go to  $\lambda_1$  in the deep solid. This constitutes one of the two boundary conditions that can be imposed. Therefore,  $C_1$  and  $C_2$  cannot be independent. Solving for  $C_2$  in terms of  $C_1$ :

$$C_2 = C_1 \frac{f_1'(\infty) - \lambda_1 f_1(\infty)}{\lambda_1 f_2(\infty) - f_2'(\infty)}$$

Substitution of this expression for  $C_2$  into the ratio,  $g/f$ , followed by algebraic simplification, leads to the result that  $g/f$  depends upon the ratio  $C_2/C_1$  and not upon  $C_1$  and  $C_2$  independently. Of course,  $g/f$  will vary from case to case and will vary with  $x$  for a given case; the important point is that it depends only on the ratio  $C_2/C_1$  and  $x$ . This property was first observed numerically in the course of a prototypal computer program which was based upon an iterative scheme. Accordingly, it suffices to go through Eqs. (35) and (36) in the layers, beginning with Eqs. (39)<sup>6</sup>, and then solve numerically through the melt layer, just one time for  $K_2$ <sup>7</sup>. Knowing  $K_2$ , Eq. (50) for  $R$  is solved by complex arithmetic<sup>8</sup>.

It is of interest to examine the form of Eq. (50) in comparison to the form obtained from the homogeneous theory (Ref. 16). The latter can be written as:

$$R = \frac{\Omega n A B}{\Omega [A B - (1 + A)] + i A - \lambda_1 [\Omega - i A]} \quad (51)$$

where  $n$  = pressure exponent

$A$  = a solid phase parameter, not to be confused with  $A$  as defined in Eq. (1)

$B$  = a gas phase parameter, not to be confused with  $B$  as defined in Eq. (3)

$\lambda_1$  = as defined in Eqs. (35, 36); it is of opposite sign in Ref. (16).

6 Subroutine LAYRSP of the computer program.

7 Subroutine MLTLRP of the computer program.

8 Subroutine GLTFP of the computer program.



It is noted that Eqs. (50) and (51) are identical in form and, to some extent, they are similar in substance. The parameter  $V_{6B}$  combines condensed phase and gas phase terms, as does  $(nAB)$  of Eq. (51). The parameters  $C$  and  $V_3$ , although different, are condensed phase terms as is  $A$  of Eq. (51). The parameter  $V_{6A}$  is a gas phase term, as is  $B$  of Eq. (51). The parameter  $V_5$  is related to  $C$ , and, therefore, a part of the analogy to  $A$ ; but important differences from  $A$  derive from the finite melt layer. The parameter  $K_2$  is the heterogeneous analog of  $\lambda_1$ . The parameter  $Z_a$  is purely a consequence of the heterogeneity, so there would be no analog for it in Eq. (51). The identity in form, and the similarity in substance, suggests that the heterogeneity as described by this model will not produce radical changes in the qualitative behavior of the response function.

The zero-frequency limit of Eq. (51) is the pressure-exponent,  $n$ . Pressure exponent does not appear explicitly as such in the steady-state model described herein. Nevertheless, it is of interest to examine the zero-frequency limit of Eq. (50). It is readily apparent that a non-zero response function at zero frequency requires that the following relationship be satisfied:

$$\lim_{\Omega_a \rightarrow 0} K_2 = -\frac{C}{V_3} \quad (52)$$

The satisfaction of Eq. (52) is verified by combining Eqs. (31), (32), (5a), the derivative of Eq. (15) applied at  $y=0$ , and a perturbation of Eq. (2a). In general,  $K_2$  must be solved numerically, but at zero frequency it is possible to derive an expression which reduces to  $-C/V_3$ . Since Eq. (52) is satisfied, the indeterminate form of Eq. (50) that results may be evaluated to yield the non-zero response function:

$$\lim_{\Omega_a \rightarrow 0} R = \frac{V_{6B}}{2V_{6B} + \frac{1}{V_5} (1+V_{6A})} \quad (53)$$

Eq. (53) may be thought of as an "effective" pressure exponent, extracting an implicit property of the model. Note that it depends upon condensed phase terms as well as gas phase terms. Numerically, it is found to be consistent with pressure-dependence as calculated from results of the steady-state model.

## SECTION 5

### MODEL RESULTS

#### 5.1 THE STEADY-STATE MODEL

Results of the steady-state model have been obtained in order to evaluate some of the important model premises. The essential results are tabulated in Table I.

Table I presents various results, compared with data and with BDP model results, for A-13 propellant used as a standard case. The first set of results compares burning rate as a function of pressure. The model results compare very well with the data. It should be emphasized, however, that these results should not be construed to imply that this model is "better than" the BDP model. The second set of results compares surface temperature. Experimental values of surface temperature are reportedly in the neighborhood of 850°K (26). It is observed that this model produces higher surface temperatures and a somewhat greater sensitivity to pressure than does the BDP model. However, the results are reasonable. The results also confirm the assumption that variations in surface temperature are second order (or smaller) with respect to variations in burning rate. The third set of results compares flame standoff distance. This model uses one flame. The BDP results are for the primary flame (sum of diffusion and reaction heights), and the values to the right of the slash are for the AP monopropellant flame when that flame moves closer to the surface than the primary flame. When that happens, the BDP model employs an energy partitioning which may be thought of as some single flame having an effective height between the two shown. On that basis, the flame heights from this model are roughly a factor of 3 greater than from the BDP model, but the qualitative behavior with pressure is the same. The value of  $C_F$  in Eq. (24) was adjusted to achieve good agreement with the burning rate data; values of other constants

TABLE I

COMPARISONS OF BURNING RATE AND OTHER QUANTITIES FOR A-13 PROPELLANT

BURNING RATE

<u>PRESSURE</u> <u>(PSIA)</u>	<u>DATA</u> <u>(cm/sec)</u>	<u>FROM</u> <u>BDP MODEL</u>	<u>FROM</u> <u>THIS MODEL</u>
100	0.27	0.29	0.28
300	0.41	0.39	0.47
500	0.52	0.47	0.55
700	0.62	0.53	0.65
900	0.73	0.60	0.74
1100	0.85	0.65	0.83

WALL TEMPERATURE

100	---	824 <sup>0</sup> K	864
300	---	836	900
500	---	844	937
700	---	851	973
900	---	855	982
1100	---	859	986

FLAME HEIGHT

100	---	25.6 $\mu$ m	82.9
300	---	20.7	50.8
500	---	19.9/18.3	35.7
700	---	19.5/5.7	30.2
900	---	19.4/3.1	25.8
1100	---	19.3/3.1	23.6

are the same as used in the BDP model. It is concluded that, for purposes of the time-dependent analysis, the model conforms reasonably well with steady-state reality.

The ability to reproduce measured effects of AP particle size on burning rate was tested with a series of propellants analogous to A-13. These propellants were the subject of a low pressure  $L^*$  instability study performed by Ramohalli (35). The comparison of burning rates at 100 psia is as follows:

<u>PARTICLE SIZE (<math>\mu\text{m}</math>)</u>	<u>DATA (cm/sec)</u>	<u>MODEL (cm/sec)</u>
40	0.41	0.38
90	0.27	0.28
200	0.23	0.19
360	0.19	0.13

Again, the agreement is reasonable.

There are two other aspects of the steady-state model results which merit discussion: The melt layer and the heterogeneity in relation to the thermal wave.

The melt layer thickness is computed to be of the order of microns or less, which is consistent with experimental observation and the thin melt layer assumption. Its dependence upon heating rate involves a tradeoff between surface temperature and the steepness of the thermal gradient. Theoretically, it will disappear at such low burning rate that the surface temperature does not reach the AP melting point, and also will approach zero at very high burning rate where the gradient is very steep. Although the layer is thin, it was considered improper to neglect it for mathematical convenience because the characteristic time of its dimension corresponds to the high frequencies of interest.

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35. Kumar, R. N. and McNamara, R. P., "Some Experiments Related to L-Star Instability in Rocket Motors", AIAA Paper 73-1300 (Nov., 1973).



For particle sizes in excess of  $40\mu\text{m}$ , the thermal wave will not penetrate the first AP layer under conditions of interest. The implication is that, except for the melt layer, the solid can be considered homogeneous in determining its role. However, this is not true for the fine sizes which are generally utilized in practical propellants. An estimate for a  $2\mu\text{m}$  AP propellant reveals that, at 1000 psi, the temperature does not fall to within 10 percent of the bulk temperature until about 5 pairs of AP-binder layers are traversed. Further, if the  $2\mu\text{m}$  AP is a component of a multimodal propellant, the burn rate will be lower such that the thermal wave will penetrate more layers of the column consisting of the  $2\mu\text{m}$  AP. As a result, it appears that the role of solid phase heterogeneity will be limited to melt layer heterogeneity in the intermediate-coarse size regime, but that in-depth heterogeneity can be important in the fine size regime. This distinction is one consequence of the present fixed-geometry model; were the layers permitted to move to evoke the pulsation mechanism, then the in-depth heterogeneity could be important for all sizes. The distinction was considered significant in view of the experimental importance of fine AP (15).

## 5.2 THE TIME-DEPENDENT MODEL

The effects of the solid phase heterogeneities are most likely to appear at combinations of fine AP and low burning rate. Therefore, a test case consisting of a  $2\mu\text{m}$  AP propellant at a burning rate of 0.47 cm/sec was selected for evaluation. Except for the particle size, this test case would correspond to A-13 propellant at 300 psi. Results are shown in Figure 3. The solid line is for the heterogeneous propellant. The long-dash line is for AP and binder thermal properties equal to mean propellant thermal properties; therefore, it is for melt layer

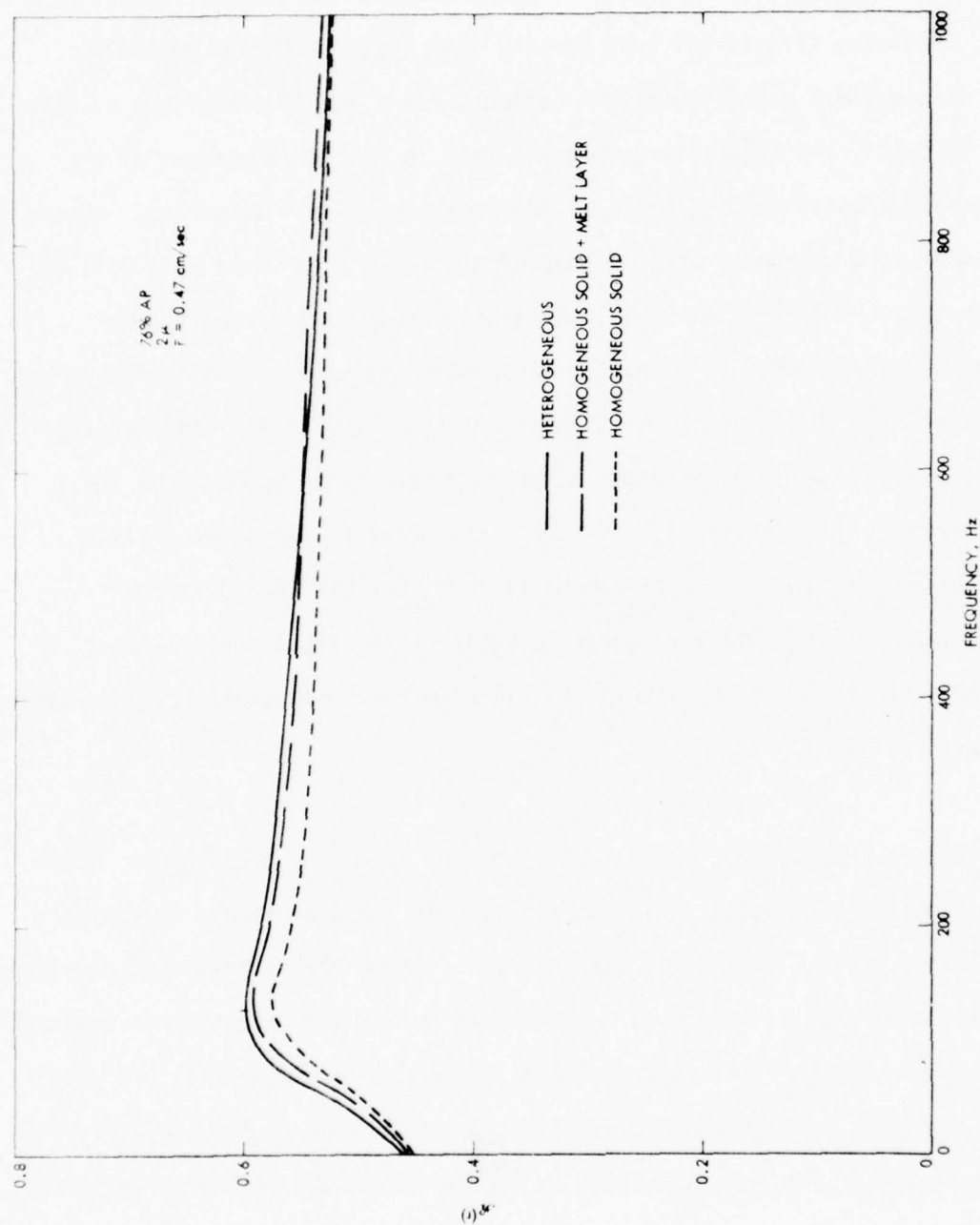


Figure 3. Response Function Calculations for a  $2 \mu$  AP Analog of A-13 Propellant

heterogeneity only, the propellant below the melt layer being homogeneous<sup>9</sup>. The short-dash line is for a completely homogeneous solid; i.e., the distributed heat release in the finite melt layer is now concentrated at the surface only and the entire region beneath the surface is homogeneous<sup>10</sup>. It is observed that the effects of the heterogeneities are small.

Figure 4 compares results for a 90 $\mu$ m AP propellant, which is A-13 propellant, with the Figure 3 results. Thus, the effect of particle size at a constant burning rate is shown. In the framework of this model, a constant burning rate implies a constant wall temperature and constant dimensionless flame properties; thus, any difference is due to solid phase heterogeneities. An effect of the heterogeneity does appear, but again, it is small. It is noted that the results for A-13 are virtually identical to the homogeneous solution displayed in Figure 3. In the case of A-13, the thermal wave does not penetrate the surface AP layer and the melt layer thickness is about 1 percent of the particle size; thus, the solid is homogeneous for all practical purposes. In the case of the 2 $\mu$ m propellant the thermal wave penetrates 15 AP layers and the melt layer thickness is about one-third (1/3) of the particle size; thus, the solid is heterogeneous, but the effect of the heterogeneity appears to be small. Significantly, the effect is small with respect to peak response

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9  $k_a = k_b = k_s$ ;  $\rho_a = \rho_b = \rho_s$ ;  $c_a = c_b = c_s$ ;  $Z=1$ .

10  $V_3 = C = Z = 1$ ;  $K_2 = \lambda_1$ ;  $V_5 = \theta \cdot x$ . This would correspond to the Denison and Baum model except for differences in the modeling of the gas phase, and differences in the values of combustion constants due to the use of this model (including the finite melt layer) to reproduce steady-state burning rates.

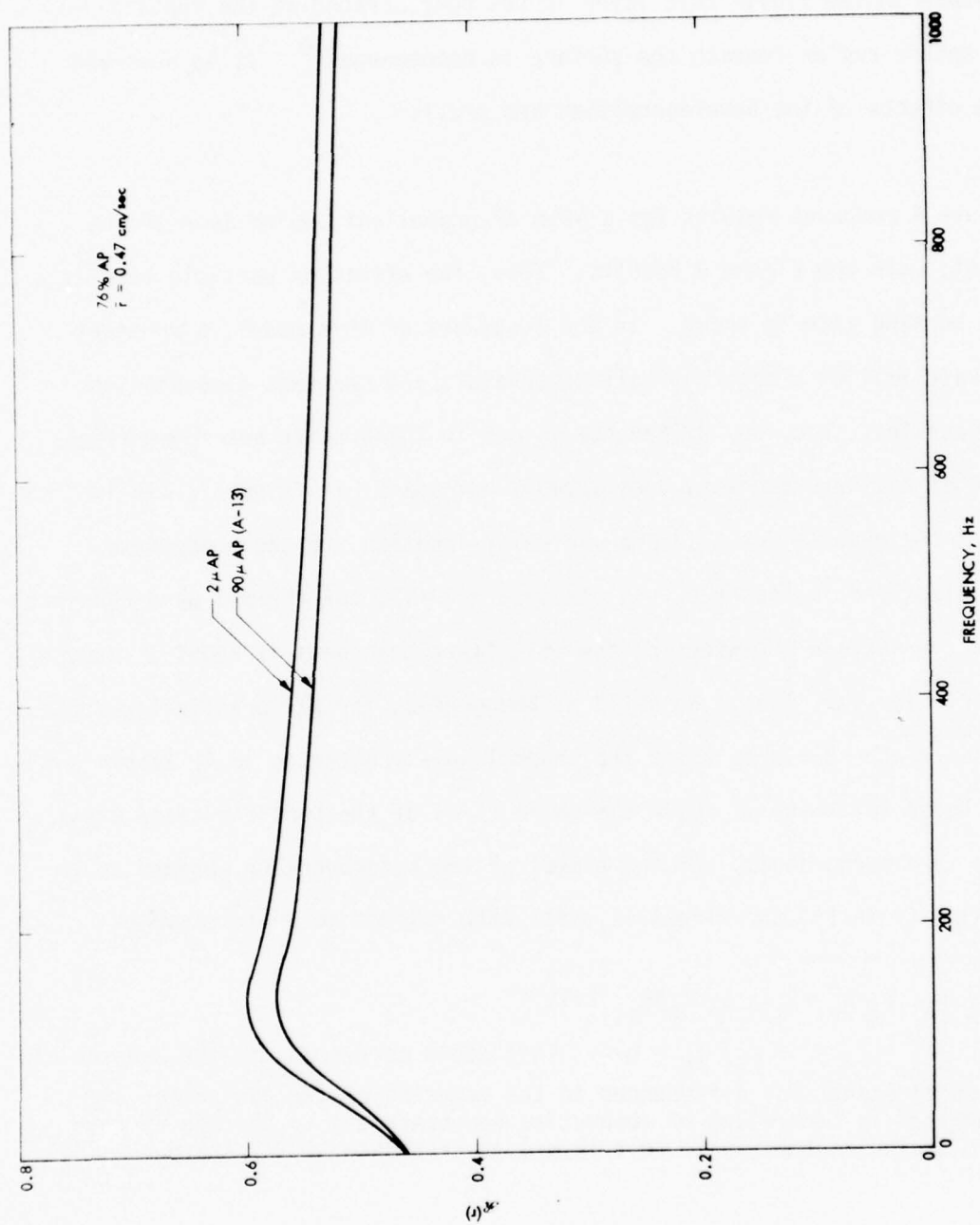


Figure 4. Effect of AP Particle Size at Constant Burning Rate for A-13 Type Propellant

frequency as well as magnitude. Thus, it can be concluded that the expected effects of the heterogeneity are not being represented by this model.

The theoretical results for the A-13 propellant, moreover, do not agree with experimental data. The A-13 is a JANNAF standard propellant, and has been well-characterized in T-burner testing (Ref. 36). The experimental peak response is about 4 and occurs at roughly 300 Hz. Thereafter, the response declines to a value of approximately 1.5 at 1000 Hz. The theoretical results presented in Figure 4 show a peak response of 0.58 at 125 Hz, and a value of 0.51 at 1000 Hz. Therefore, the theory shows a relatively slight peak and at too low a frequency. Such theoretical results are a consequence of the combustion parameters, analogous to the "A" and "B" (or " $\alpha$ ") parameters of the Denison & Baum model. Presumably, the agreement with data could be improved by selection of a different set of parameters. However, a ground rule of this study was that the parameters would be predetermined by considerations of a credible steady-state model. Given that model, it is inappropriate to change the constants arbitrarily. According to Ref. (27), a relatively large value of the "B" (or " $\alpha$ ") parameter will constrain the time-dependent model to the prediction of small peaks, and a relatively small value of the "A" parameter will produce low peak response frequencies. By analogy, that is the situation here. Since it would be inappropriate to juggle parameters, it must be concluded that there is a mechanistic deficiency in the time-dependent model that has been postulated here.

Figure 5 presents theoretical results showing the effect of burning rate for a constant particle size. The 2 $\mu$ m AP propellant was selected for this illustration.

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36. "T-Burner Manual", CPIA Publication 191 (Nov., 1969).



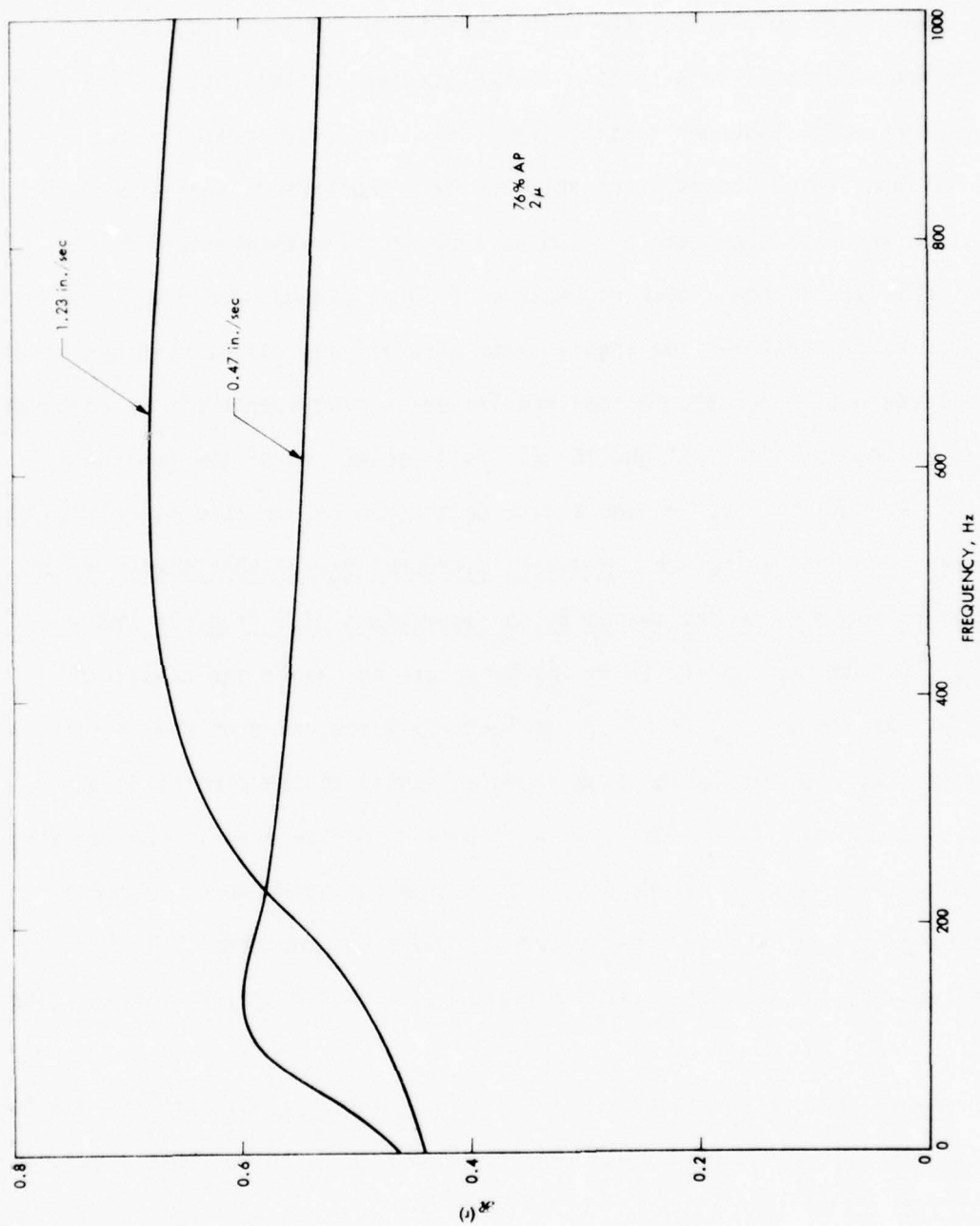


Figure 5. Effect of Burning Rate at Constant AP Particle Size for the 2  $\mu$  Analog of A-13 Propellant

The higher burning rate is representative of this propellant; the lower burning rate may be thought of as a suppression for purposes of Figures 3 and 4. The effect on peak response frequency demonstrates further that the modeled heterogeneities are of little consequence. It is observed that the peak response frequency varies nearly with the square of the burning rate, which is the result for homogeneous propellants. On the other hand, the Figure 3 and 4 results show that the effect of the heterogeneity on peak response frequency is about 10 percent. According to the Cohen postulates for the effect of heterogeneity, the peak response frequency in Figure 5 should vary with the first power of burning rate, and in Figure 4 it should vary inversely with particle size. These effects are not being produced by this model.

Figure 6 compares theoretical results with experimental data for a bimodal propellant. Although the shape of the theoretical curve is reasonable, the peak response magnitude and frequency are again underpredicted. Also, the zero frequency limit is overpredicted, reflecting a deviation from the measured steady-state pressure exponent. It appears that further work is necessary in order to implement a proper mechanism for the combustion response.

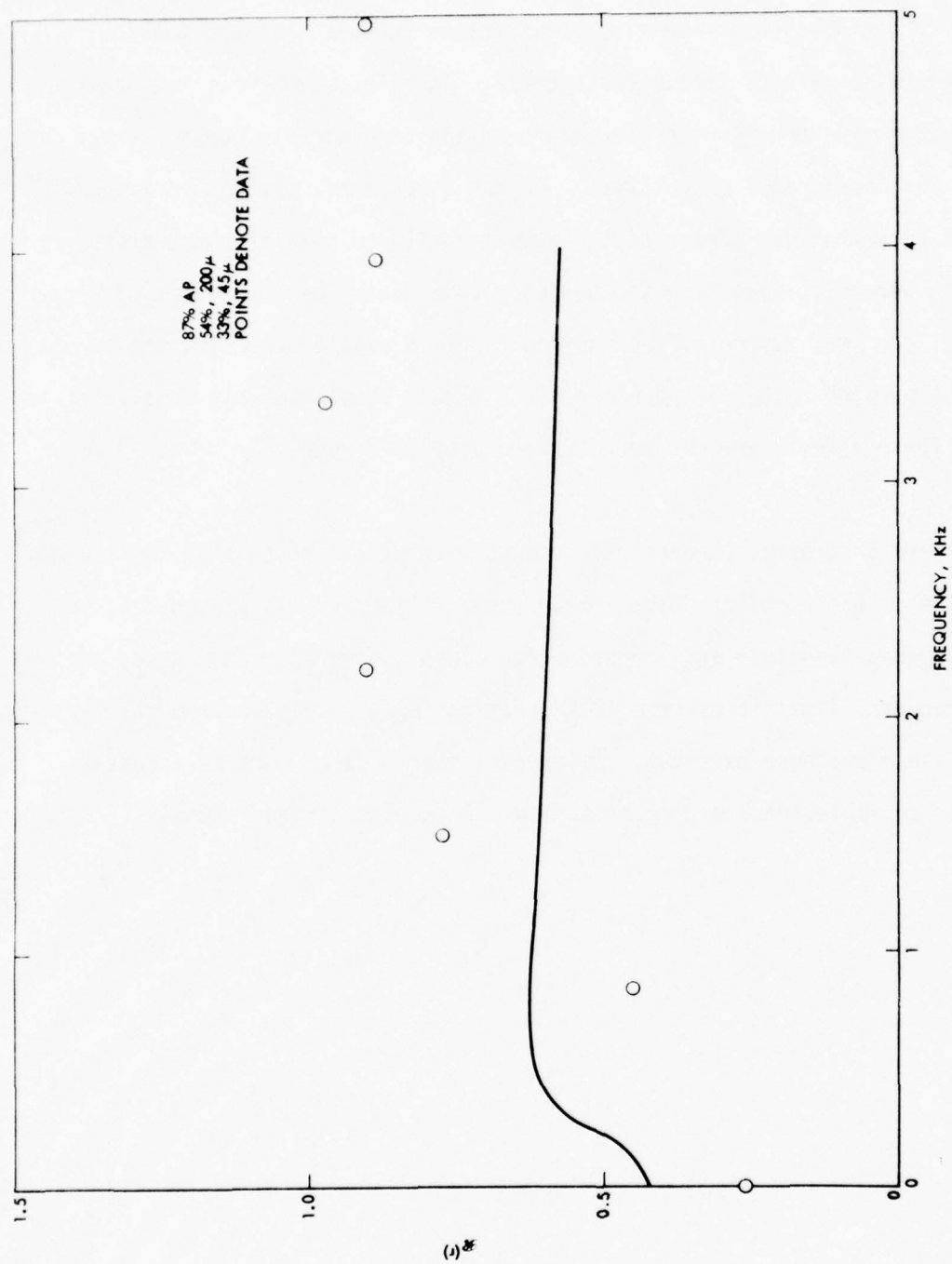


Figure 6. Comparison of Theory and Experiment for SP-540 Propellant at 500 psi

## SECTION 6

### CONCLUSIONS AND RECOMMENDATIONS

An analytical model has been developed which incorporates mechanisms of solid phase and gas phase heterogeneities into the calculation of steady-state and linear time-dependent combustion properties of composite solid propellants. Although the model satisfactorily describes the steady-state combustion properties, it is deficient in describing the time-dependent combustion response characteristics in several respects. Use of a consistent set of combustion constants produces peak response magnitudes and frequencies which are too low in comparison to experimental data and which are not significantly affected by the AP particle size per se. Although an effect of the solid phase heterogeneities is predicted by this model, the effect is quantitatively so small as to allow it to be neglected in future work. Therefore, the role of AP cannot be attributed to the solid phase alone unless some other mechanism is incorporated into the theory. It is recommended that the concept of moving layers be re-examined, including justification for the coherence of such a mechanism. It is further recommended that the perturbed BDP model be examined as a potentially useful way in which to represent the heterogeneity of the gas phase. It is desired not only to achieve the effects of the heterogeneity, but also to justify a set of values of the combustion constants that will properly position the response function curve. It appears necessary to modify both the solid phase and gas phase models in order to achieve those purposes in a consistent manner.

## SECTION 7

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## APPENDIX A

### COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL COMPUTER PROGRAM

This appendix presents information essential to the utilization of the composite Solid Propellant Combustion Response Model (CSP CRM) computer program. This information is presented under the following headings and in the order listed:

1. Definitions of Input Data
2. Input Deck Corresponding to the Example Problem.
3. Definitions of Output Data
4. Card Image Listing of Program.
5. Description of Program Logic, Subroutines and Use of Text Equations
6. Solutions to Example Problem

# A-1. DEFINITIONS OF INPUT DATA

All input to the Composite Solid Propellant Combustion Response Model Computer Program is made by means of a NAMELIST/INPUT statement and an associated read statement, both of which appear in the DATAIN subroutine. The FORTRAN names of the input variables and parameters, together with their corresponding algebraic symbols and brief definitions are presented below in the exact order that they appear in the INPUT list:

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
CA	$C_a$	specific heat at constant pressure for the oxidizer ( $\text{cal g}^{-1} \text{ } ^\circ\text{K}^{-1}$ , real)
CB	$C_b$	specific heat at constant pressure for the binder ( $\text{cal g}^{-1} \text{ } ^\circ\text{K}^{-1}$ , real)
CG	$C_g$	specific heat at constant pressure for the combustion gas mixture that exists between the gas-condensed phase interface and the flame front ( $\text{cal g}^{-1} \text{ } ^\circ\text{K}^{-1}$ , real)
KA	$k_a$	thermal conductivity of the oxidizer ( $\text{cal sec}^{-1} \text{ cm}^{-1} \text{ } ^\circ\text{K}^{-1}$ , real)
KB	$k_b$	thermal conductivity of the binder ( $\text{cal sec}^{-1} \text{ cm}^{-1} \text{ } ^\circ\text{K}^{-1}$ , real)
RØA	$\rho_a$	density of the oxidizer ( $\text{g cm}^{-3}$ , real)
RØB	$\rho_b$	density of the binder ( $\text{g cm}^{-3}$ , real)
WAC(J)	$W_a(j)$	fraction of composite solid propellant mass attributable to the jth size component of the oxidizer ( $j \leq 4$ ) (dimensionless, real)
SMLA(J)	$a_j$ or $D_j$	diameter of jth size component oxidizer particles ( $j \leq 4$ ) (cm, real) Note: Must be listed in order of increasing particle size.
E	E	activation energy for decomposition of the oxidizer ( $\text{cal. g-mole}^{-1}$ , real)
R	R	universal gas constant ( $\text{cal. g-mole}^{-1} \text{ } ^\circ\text{K}^{-1}$ , real)

FORTTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
PRXFAC	A	prefactor in the Arrhenius expression for oxidizer decomposition ( $\text{sec}^{-1}$ , real)
QS	$Q_a$	gross heat of decomposition of the oxidizer (equals net heat of decomposition of the oxidizer minus latent heat of melting of the oxidizer) ( $\text{cal g}^{-1}$ , real)
QB	$Q_b$	heat of decomposition of the binder ( $\text{cal g}^{-1}$ , real)
QLM	$Q_m$	latent heat of melting of the oxidizer ( $\text{cal g}^{-1}$ , real)
KFLMHT	CF	$CF = \bar{p}x^*/(\bar{r}D_l)$ constant of proportionality in the rational algebraic approximation to BDP effective flame height ( $\text{atmos sec } \mu\text{m}^{-1}$ , real)
TFLM	$T_f$	adiabatic temperature of the gas-phase combustion flame sheet ( $^{\circ}\text{K}$ , real)
TM	$T_m$	melting temperature of the oxidizer ( $^{\circ}\text{K}$ , real)
TZRØ	$T_o$	temperature in the composite solid propellant far from the gas-condensed phase interface ( $^{\circ}\text{K}$ , real)
PBAR	$\bar{p}$	temporal mean pressure in the gas phase---assumed to be uniform ( $\text{atmos}$ , real)
RBR	$\bar{r}$	temporal mean rate of regression of the composite solid propellant; no input if ITERA=1 ( $\text{cm sec}^{-1}$ , real)
TØL	-	arbitrary tolerance employed in the steady-state part of the computer program to evaluate convergence of the steady-state solution (dimensionless, real, usually $10^{-3} \leq TØL \leq 10^{-5}$ )
ITERA	-	specifies the mode of operation of the computer program: If ITERA=0, the program determines the combustion response parameters for a CSP whose temporal mean regression rate is specified; if ITERA=1, the program determines the temporal mean regression rate for a propellant whose basic physical and chemical characteristics have been specified (dimensionless, integer).



FØRTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
N5MAX	-	if ITERA=1 and if a satisfactory value for RBR has not been achieved after N5MAX-1 one-percent increments or decrements of RBR, the solution will be terminated and an appropriate comment will be printed in the computer output (dimensionless, integer, $5 \leq N5MAX \leq 20$ ) Note: This mode of program termination indicates an injudicious initial choice for RBR.
NPP	$p'/\bar{p}$	normalized pressure perturbation (dimensionless, polar complex) Note: This is the exciter of the perturbation; as such, its phase is arbitrarily set equal to zero
TAPIN	$\tau'_{y>0}$	normalized temperature perturbation applied in the solid phase at a distance from the gas-condensed phase interface that is several times the characteristic transient thermal depth within the solid. (dimensionless polar complex) Note: Since the ratio, $(g'/\tau')_{y=0}$ , obtained from the solid phase solution is independent of the argument assumed for $\tau'$ , the argument is ordinarily arbitrarily set equal to zero.
YTD		factor which, when multiplied by SQRT (KAPS/ØMEGA), provides a value of $x>0$ , viz., XTD (dimensionless, usually assumed to be an integer $\geq 3$ ) Note: SQRT (KAPS/ØMEGA) is a measure of the depth of penetration of the perturbation into the CSP
ØMEGA	$\omega$	assumed angular frequency of the perturbation (radians sec <sup>-1</sup> , real)
NEQ	-	number of differential equations solved in subroutine SVDQ---always equal to one in this computer program (dimensionless integer)
KD	-	order of the differential equations solved in subroutine SVDQ--- always equal to two in this computer program (dimensionless, integer)
MXSTEP	-	maximum number of steps allowed between output points in subroutine SVDQ---usually set equal to one hundred in this computer program (dimensionless, integer)
EP	-	parameter used to control local error in subroutine SVDQ---refer to description of subroutine for guidance in setting the value of this parameter (dimensionless, real)

FØRTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
IHØMØ	-	When IHØMØ=0, certain pertinent physical and thermal properties of the propellant binder, oxidizer, and gaseous products specified in namelist/input/are generally distinct; however, when IHØMØ=1, these properties are set equal to corresponding properties of the oxidizer. Thus, specifying IHØMØ=1 implies a homogeneous propellant (dimensionless, integer)



### A-3. DEFINITIONS OF OUTPUT DATA

All permanent output of the Composite Solid Propellant Combustion Response Model (CSP CRM) Computer Program is made by means of NAMELIST/OUTPUT statements and corresponding associated write statements. All of the NAMELIST/OUTPUT statements and associated write statements appear in the DTAOUT.

Although some temporary NAMELIST/TPOUT statements and associated write statements are located in various intermediate subprograms of the CSP CRM Computer Program, the FORTRAN names therein are, with rare and inconsequential exception, reprinted in one or the other of the write statements associated with NAMELIST/OUTPUT statements. For this reason, only FORTRAN names associated with permanent output are presented here.

Each NAMELIST/OUTPT and, within each list, each FORTRAN name appearing in DTAOUT are presented below in the exact order of appearance in the resulting print-out.

#### NAMELIST/OUTPT 1

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
JMAX	$j_{\max}$	maximum number of size components of the oxidizer ( $j_{\max} \leq 4$ ) (dimensionless, integer)
WA	$W_a$	$W_a = \sum W_a(j)$ fraction of solid propellant mass attributable to all size components of the oxidizer (dimensionless, real)
DNM	-	denominator in formula for SMLB in subroutine DATAIN $\sum [W_a(j)/a_j]$ ( $\text{cm}^{-1}$ , real)
WB	$W_b$	$W_b = 1 - W_a$ fraction of solid propellant mass attributable to the binder (dimensionless, real)
VFA	$v$	volume of the oxidizer expressed as a fraction of solid propellant volume (dimensionless, real)
SMLATP	$a_{\text{top}}$	$a_{\text{top}} = \sqrt{\frac{2}{3}} A_{j_m}$ Hermance equivalent mean size of the oxidizer size component assumed to exist in the topmost lamina of the solid propellant ( $j_m$ ) (cm, real)

FØRTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
DLTYTP	$\Delta \bar{y}_{top}$	$\Delta \bar{y}_{top} = a_{top} \bar{r} / \kappa_a$ thickness of any oxidizer lamina other than the topmost (dimensionless, real)
SMLB	b	$b = W_a \{ [\pi/6v] \}^{1/3} - \sqrt{2/3} \} / \Sigma [W_a(j)/a_j]$ idealized thickness of a binder lamina calculated on the basis of oxidizer packing factor (cm, real)
DLTYBB	$\Delta \bar{y}_b$	$\Delta \bar{y}_b = b \bar{r} / \kappa_b$ thickness of any binder lamina (dimensionless, real)
KS	$k_s$	bulk equivalent thermal conductivity of the CSP (cal sec <sup>-1</sup> cm <sup>-1</sup> °K <sup>-1</sup> , real)
RØS	$\rho_s$	bulk mean density of the CSP (g cm <sup>-3</sup> , real)
CS	$C_s$	bulk equivalent specific heat at constant pressure of the CSP (cal g <sup>-1</sup> °K <sup>-1</sup> , real)
KAPA	$\kappa_a$	$\kappa_a = k_a / (\rho_a C_a)$ thermal diffusivity of the oxidizer (cm <sup>2</sup> sec <sup>-1</sup> , real)
KAPB	$\kappa_b$	$\kappa_b = k_s / (\rho_s C_s)$ bulk equivalent thermal diffusivity of the CSP (cm <sup>2</sup> sec <sup>-1</sup> , real)
KAPS	$\kappa_s$	$\kappa_s = k_s / (\rho_s C_s)$ bulk equivalent thermal diffusivity of the CSP (cm <sup>2</sup> sec <sup>-1</sup> , real)
Z	Z	$Z = \rho_s C_s / (\rho_a C_a)$ ratio of thermal capacity per unit volume of the bulk CSP to that of the oxidizer (dimensionless, real)
Z'	Z'	$Z' = \rho_s C_s / (\rho_b C_b)$ ratio of thermal capacity per unit volume of the bulk CSP to that of the binder (dimensionless, real)



## NAMELIST/OUTPT 2

FORTTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
THETAA	$\theta_a$	$\theta_a = E / (R \bar{T}_w)$ (dimensionless, real)
CHI	$\chi$	$\chi = \frac{\bar{T}_w - T_o}{\bar{T}_w}$ (dimensionless, real)
D	D	$D = \theta_a \cdot \chi$ (dimensionless, real)
QSDMLS	$H_a$	$H_a = W_a Q_a / [C_a (\bar{T}_w - T_o)]$ (dimensionless, real)
QMDMLS	$H_m$	$H_m = W_a Q_m / [C_a (\bar{T}_w - T_o)]$ (dimensionless, real)
FDMLS	$\tau_f$	$\tau_f = \bar{r} / (\bar{T}_w - T_o)$ (dimensionless, real)
B	B	$B = \kappa_a A W_a Q_a / [C_a (\bar{T}_w - T_o) \bar{r}^2]$ (dimensionless, real)
KMLTLR	K	$K = B \exp(-\theta_a) / D$ (dimensionless, real)

## NAMELIST/OUTPT 3

FØRTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
TWBAR	$\bar{T}_w$	mean temperature of the gas-liquid interface at the mean position of this interface, i.e., at $\bar{y}=0$ (°K, real)
YSSTBR	$\bar{y}_s^* = \frac{\bar{x}^* \bar{r}}{\kappa_s}$	dimensionless flame mean stand-off distance (dimensionless, real)
XSTBAR	$\bar{x}^*$	flame mean stand-off distance (cm, real)
AMM	$a_m$	equivalent mean particle diameter (cm, real)
TAUMLT(M-1)	$\bar{\tau}_{m-1}$	dimensionless mean temperature within the melt layer Note: $\bar{T}_0=1.0$ , and $\bar{T}_{100}=T_{\text{melt}}$ , the dimensionless melting temperature of the oxidizer. (dimensionless, real)
XMLT(M-1)	$x_{m-1}$	distance from the mean position of the gas-liquid interface to the location at which $\bar{T}=\bar{T}_{m-1}$ (cm, real)
M	m	index of the increments in $\bar{T}$ and x that are calculated and tabulated through the melt layer $2 \leq M \leq 101$ (dimensionless, integer)
N	n	index of laminae from the gas-liquid interface ( $n=0$ ), through the liquid-solid interface ( $n=1$ ), through the first oxidizer-to-binder interface ( $n=2$ ) through the first binder-to-oxidizer interface ( $n=3$ ), and so on to as far into the CSP as $n=101$ , if necessary (dimensionless, integer)
RBR	$\bar{r}$	temporal mean rate of regression of the composite solid propellant (cm sec <sup>-1</sup> , real)
ITERA	-	specifies the mode of operation of the computer program: If ITERA=0, the program determines the combustion response parameters for a CSP whose temporal mean regression rate is specified; if ITERA=1, the program determines the temporal mean regression rate for a propellant whose basic physical and chemical characteristics have been specified (dimensionless, integer)
N5	-	when ITERA=1, N5 is the number of the iteration in the iterative attempt to determine RBR ( $1 \leq N5 \leq N5\text{MAX}$ ) (dimensionless, integer)
N5MAX	-	if ITERA=1 and if a satisfactory value for RBR has not been achieved after N5MAX-1 one-percent increments or decrements of RBR, the solution will be terminated and an appropriate comment will be printed in the computer output (dimensionless, integer) Note: This mode of program termination indicates an injudicious initial choice for RBR.

NAMelist/OUTPT 3 (continued)

FØRTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
LFLAG	-	LFLAG is set to zero each time SUBROUTINE SLDFAZ is entered in a normal manner. If ITERA=0, LFLAG is then immediately reset to 1 and control of the program is returned to SUBROUTINE CØNTRL, the main program, as soon as explicit values of certain required variables are determined in SUBROUTINES SLDFAZ, GASFAZ, and AMULTI. If ITERA=1, LFLAG is only reset to 1 and program control is only returned to the main program when a suitable value has been found for RBR or when N5=N5MAX (dimensionless, integer)
GWBRs	$\bar{g}_{ws}$	$\bar{g}_{ws} = \left(\frac{d\bar{\tau}}{dy_s}\right)_{y_s=0}$ (dimensionless, real)
DGWBRs	$\left(\frac{d\bar{g}}{dy_s}\right)_{y_s=0}$	$\left(\frac{d\bar{g}}{dy_s}\right)_{y_s=0} = \left(\frac{d^2\bar{\tau}}{dy_s^2}\right)_{y_s=0}$ (dimensionless, real)
QLDMLS	$H_l$	sometimes set equal to $H_s$ ; at other times, calculated as non-dimensionalized sum of $H_m$ and the actual heat absorbed as a result of oxidizer degradation as it is transported through the melt layer. Note: The two methods of determining $H_l$ ordinarily lead to virtually identical results. (dimensionless, real)

NAMelist/OUTPT 4

FØRTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
TAULR(N)	$\bar{\tau}_n$	dimensionless mean temperature at distance SLR(N) from the mean gas-liquid interface (dimensionless, real)
DTAULR(N)	$[\frac{d\bar{\tau}}{dy}(a)_b]_{n-}$	dimensionless mean temperature gradient at distance, XLR(N), from the mean gas-liquid interface and on the side of the N,N+1 interface nearest the mean gas-liquid interface. Note: For n even, $y=y_a$ ; for n odd, $y=y_b$ (dimensionless, real)
XLR (N)	$x_n$	distance from the mean position of the gas-liquid interface to the N,N+1 interface (cm, real)
DSCRIM(N)	$\bar{\tau}_n + (\frac{d\bar{\tau}}{dy})_{n-}$	because, deep in the CSP, the exponentially decaying nature of the solution requires that DSCRIM(N) approach zero, DSCRIM(N) furnishes an indication as to whether the solution in this region has proceeded to a depth sufficient to provide a satisfactory steady-state solution (dimensionless, real)
N	n	index of laminae from the gas-liquid interface (n=0), through the liquid-solid interface (n=1), through the first oxidizer-to-binder interface (n=2) through the first binder-to-oxidizer interface (n=3), and so on to as far into the CSP as n=101, if necessary (dimensionless, integer)
XTD	-	SQRT (KAPS/ØMEGA)*YTD (cm, real)
CAPØA	$\Omega_a$	$\Omega_a = \frac{\omega K_a}{\bar{r}^2}$ (dimensionless, real)
CAPØB	$\Omega_b$	$\Omega_b = \frac{\omega K_b}{\bar{r}^2}$ (dimensionless, real)
CAPØS	$\Omega_s$	$\Omega_s = \frac{\omega K_s}{\bar{r}^2}$ (dimensionless, real)

NAMelist/OUTPT 5

FØRTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
N2	n2	index of the laminae from the deep-solid side of the first oxidizer laminae for which $XLR(N2=N2MXP1) > XTD$ , through the adjacent overlying binder lamina for which $XLR(N2=N2MXP1-1) > XTD$ , through successive laminae of oxidizer and binder and, finally, of melt layer to $N2=0$ . Note: $XLR(N2=N) \equiv XLR(N)$ The index N2 is used in the step-by-step calculation of the perturbed solution, whereas N is used in the step-by-step calculation of the steady-state solution. (dimensionless, integer)
N2MXP1	$n2_{max}+1$	maximum value of N2 determined as indicated in the definition of N2 (dimensionless, integer)
TAPIN	$\tau'_{n2_{max}+1}$	normalized temperature perturbation applied in the solid phase at a distance from the gas-condensed phase interface that is several times the characteristic transient thermal depth within the solid. (dimensionless, complex)
DTAPIN	$g'_{n2_{max}+1}$	$g'_{n2_{max}+1} = \left(\frac{d\tau'}{dy_a}\right)_{n2_{max}+1}$ (dimensionless, complex)
XLR(N2)	$x_{n2}$	distance from the mean position of the gas-liquid interface to the N2, N2+1 interface (cm, real)
TAPLR(N2)	$\tau'_{n2}$	dimensionless perturbed temperature at the N2, N2+1 interface (dimensionless, complex)
DTAPLR(N2)	$g'_{n2}$	first derivative of dimensionless perturbed temperature with respect to $y_a$ when N2 is even, or with respect to $y_b$ when N2 is odd, at the N2, N2+1 interface (dimensionless, complex)
TAUOPS	$\tau'_{y=0}$	dimensionless perturbed temperature at the mean position of the gas-liquid interface, i.e., at $y=0$ (dimensionless, complex)
GOPPS	$g'_{y=0}$	first derivative of dimensionless perturbed temperature with respect to $y_a$ at $y=0+$ (dimensionless, complex)
DGOPPS	$g'_{y=0}$	second derivative of dimensionless perturbed temperature with respect to $y_a$ at $y=0+$ (dimensionless, complex)
RF	R	$R = \left(\frac{r'}{p'/\bar{p}}\right)$ , the response function (dimensionless, complex)



## NAMELIST/OUTPT 5 (continued)

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
NRP	$\frac{p'}{\bar{p}}$	normalized perturbed pressure in the gas phase (quasi-static gas-phase behavior assumed) (dimensionless, complex)
YSWP	$y'_{S_w}$	dimensionless displacement of the instantaneous gas-liquid interface with respect to the mean gas-liquid interface, i.e., with respect to $y=0$ ; displacement non-dimensionalized on the basis of bulk CSP properties (dimensionless, complex)
XWP	$x'_w$	$x'_w = \frac{\kappa_S y'_{S_w}}{\bar{r}}$ (cm, complex)
NXSTP	$\frac{x^{*'}}{\bar{x}^*}$	perturbed displacement of the flame front with respect to the mean position of the flame front; normalized with respect to the mean position of the flame front (dimensionless, complex)
XSTP	$x^{*'}_w$	$x^{*'}_w = \bar{x}^* \cdot \frac{x^{*'}}{\bar{x}^*}$ (cm, complex)
NYSSTP	$\frac{y^{*'}_S}{\bar{y}^{*}_S}$	$\frac{y^{*'}_S}{\bar{y}^{*}_S} = \frac{x^{*'}}{\bar{x}^*}$ (dimensionless, complex)
YSSTP	$y^{*'}_S$	$y^{*'}_S = \bar{y}^{*}_S \cdot \frac{x^{*'}}{\bar{x}^*}$ (dimensionless, complex)
RFNMLT	$R_{NML}$	response function under the assumption that no melt layer (NML) exists in the oxidizer lamina, that is contiguous with the gas phase (dimensionless, complex)
NRPNM	$(\frac{p'}{\bar{p}})_{NML}$	normalized perturbed pressure in the gas phase under the assumption that no melt layer exists (dimensionless, complex)
YSWPNM	$y'_{S_{wNML}}$	$y'_{S_w}$ under the assumption that no melt layer exists (dimensionless, complex)
XWPNM	$x'_{wNML}$	$x'_w$ in the absence of a melt layer (cm, complex)

NAMelist/OUTPT 5 (continued)

FØRTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
NXSTPN	$\left(\frac{x^{*'}}{\bar{x}^{*'}}\right)_{NML}$	$\frac{x^{*'}}{\bar{x}^{*}}$ in the absence of a melt layer (dimensionless, complex)
XSTPNM	$x^{*'}_{NML}$	$x^{*'}$ in the absence of a melt layer (cm, complex)
YSSTPN	$y^{*'}_{S_{NML}}$	$y^{*'}_S$ in the absence of a melt layer (dimensionless, complex)

A-4. CARD IMAGE LISTING OF PROGRAM

A-66

C  
C  
CSTEAD PROC

C  
C  
C  
C  
C  
C

THIS RUN HAS BEEN MADE WITH PROGRAM DECK NO. 9A

IMPLICIT REAL (K)  
COMMON/STEADY/ AMM,B,C,CA,CB,CG,CHI,CM,CS,D,DLTYAB,DLTYBB,DLTYTP,  
1DELTA,DELTAU,DNM,DNOM,DTAULR,DSCRIM,E,ETA,FDMLS,JMAX,KA,KAPA,  
2KAPB,KAPS,KB,KFLMHT,KMLTLR,KS,PBAR,PRXFAC,QB,QBDMLS,QLM,QMDMLS,  
3QS,QSDMLS,R,RBR,ROA,ROB,ROS,SMLA,SMLATP,SMLB,TAULR,BUFFER1,TAUMLT,  
4TFLM,THETAA,TM,TOL,TWBAR,TZRO,VFA,WA,WAC,WB,XLR,BUFFER2,XMLT,  
5XSTBAR,YSSTBR,BUFFER3,YABRML,Z,ZI,ZPR,RBROLD,DLTRBR,ITERA,N5,N5MAX,  
6LFLAG,CAPOA,CAPOB,CAPOS,GWBR5,DGWBR5,QLDMLS,IHOMO

C  
C  
C  
C  
C  
C  
C

BUFFER1, BUFFER2, AND BUFFER3 ARE REQUIRED TO BUFFER THE STORAGE  
LOCATIONS JUST PRECEDING TAUMLT(1), XMLT(1), AND YABRML(1),  
RESPECTIVELY. THIS PROCEDURE IS MADE NECESSARY BY MAKING TAUT(2)  
EQUIVALENT TAUMLT(1), XMLTT(2), TO XMLT(1), AND YABRT(2), TO  
YABRML(1).

DIMENSION DSCRIM(110),DTAULR(110),SMLA(4),TAULR(110),TAUMLT(110),  
1TAUT(110),WAC(4),XLR(110),XMLT(110),XMLTT(110),YABRML(110),  
2YABRT(110)  
EQUIVALENCE (TAUT(2),TAUMLT(1)),(XMLTT(2),XMLT(1)),  
1(YABRT(2),YABRML(1))  
EQUIVALENCE (GWBR5,GOBR5),(DGWBR5,DGOBR5)

END

```

C
C
CUNSTD PROC
C
C
COMMON/UNSTDY/NPP,TAPIN,XTD,YTD,OMEGA,NEQ,KD,MXSTEP,KQ,EP,
1DTAPIN,TAPLR,DTAPLR,N2MXP1,RF,NRP,YSWP,XWP,NXSTP,XSTP,NYSSTP,
2YSSTP,D2TAPR,D2TAPI,TAUOPS,GOPPS,DGOPPS,
3RFNMLT,NRPNM,YSWPNM,XWPNM,NXSTPN,XSTPNM,YSSTPN
C
COMPLEX NPP,TAPIN,DTAPIN,TAPLR,DTAPLR,RF,NRP,YSWP,XWP,NXSTP,XSTP,
1NYSSTP,YSSTP,TAUOPS,GOPPS,DGOPPS,
2RFNMLT,NRPNM,YSWPNM,XWPNM,NXSTPN,XSTPNM,YSSTPN
C
DIMENSION TAPLR(110),DTAPLR(110)
END

```



CONTROL PROVIDES THE SEQUENCE OF CALLS TO  
SUBROUTINES THAT IS REQUIRED TO OBTAIN THE DESIRED SOLUTION  
OF THE COMBUSTION RESPONSE PROBLEM.

```
INCLUDE CSTEAD, LIST
INCLUDE CUNSTD, LIST
```

```

10 CONTINUE
   CALL OVRFLW(3)
   CALL DATIN
   IF (ITERA .EQ. 0 .AND. OMEGA .EQ. 0.) GO TO 70
   CALL SLDFAZ
   CALL MELTLR
   CALL LAYERS
   IF (ITERA .NE. 0) GO TO 60
   CALL LAYRSP
   CALL MLTLRP
   CALL GLIFP
60  CALL DTAOUT
   IF (ITERA .EQ. 0 .AND. OMEGA .NE. 0.) GO TO 10
70  CONTINUE
   STOP
   END

```

SUBROUTINE DAIN LOADS THE INPUT DATA AND DERIVES CERTAIN WIDELY USED PARAMETERS FROM THESE DATA.

```

INCLUDE CSTEAD, LIST
INCLUDE CUNSTD, LIST
INTEGER KD,KQ
DIMENSION TNPP(2),TTAPIN(2)
EQUIVALENCE (TNPP,NPP),(TTAPIN,NRP)

```

CAUTION\*\*\*NAMESLIST/INPUT/ REQUIRES THE ENTRY OF NPP AND TAPIN IN  
TERMS OF THE NUMBER PAIR, MODULUS (AS A DECIMAL FRACTION) AND  
ARGUMENT (AS A PHASE ANGLE IN DEGREES). NPP AND TAPIN ARE THEN  
REDEFINED BY THEIR CARTESIAN REAL AND IMAGINARY COMPONENTS IN  
SUBROUTINE DATAIN.

```

NAMELIST/INPUT/CA,CB,CG,KA,KB,ROA,ROB,WAC,SMLA,E,R,PRXFAC,QS,QB,
1QLM,KFLMHT,TFLM,TM,TZRO,PBAR,RBR,TOL,ITERA,N5MAX,NPP,TAPIN,YTD,
2OMEGA,NEQ,KD,MXSTEP,EP,IHOMO
  READ(5,INPUT)
  IF(OMEGA .EQ. 0.) RETURN
  DO 10 I=1,101
    TAPLR(I)=0.0
    DTAPLR(I)=0.0
10 CONTINUE
  IF(IDATA .EQ. 1) GO TO 106
  IDATA=1
  WRITE(6,INPUT)
  WA=0.
  DNM=0.
  JMAX=0
  IF(WAC(1) .GT. 0.) JMAX=1
  IF(WAC(2) .GT. 0.) JMAX=2
  IF(WAC(3) .GT. 0.) JMAX=3
  IF(WAC(4) .GT. 0.) JMAX=4
  IF(JMAX .EQ. 0) WRITE(6,150)
150 FORMAT(/'/T6,-NO AP PARTICLES OF ANY FINITE DIAMETER HAVE BEEN INCL
  1UDED IN THE INPUT DATA-'/)
  IF(JMAX .EQ. 0) STOP
  DO 105 J=1,JMAX
    WA=WA+WAC(J)
    DNM=DNM+WAC(J)/SMLA(J)
105 CONTINUE
106 IF(IHOMO .EQ. 0) GO TO 107

```

WHEN IHOMO=0, CERTAIN PERTINENT PHYSICAL AND THERMAL PROPERTIES OF THE PROPELLANT BINDER, OXIDIZER, AND GASEOUS PRODUCTS SPECIFIED IN NAMELIST/INPUT/ ARE GENERALLY DISTINCT. HOWEVER, WHEN IHOMO=1, THESE PROPERTIES OF THE OXIDIZER AND GASEOUS PRODUCTS ARE SET EQUAL TO CORRESPONDING PROPERTIES OF THE OXIDIZER. THUS, SPECIFYING IHOMO=1 IMPLIES A HOMOGENEOUS PROPELLANT.

$$\begin{aligned} CB &= CA \\ CG &= CA \end{aligned}$$

```

KB=KA
ROB=ROA
107 CONTINUE
WB=1.-WA
VFA=WA/ROA/(WA/ROA+WB/ROB)
SMLATP=SQRT(2./3.)*SMLA(JMAX)
SMLB=WA*VFA/DNM
KS=KA
ROS=ROA*ROB/(ROA*WB+ROB*WA)
CS=CA*WA+CB*WB
KAPA=KA/ROA/CA
KAPB=KB/ROB/CB
KAPS=KS/ROS/CS
DLTYTP=SMLATP*RBR/KAPA
DLTYAB=RBR*SMLA(1)/KAPA
DLTYBB=RBR*SMLB/KAPB
Z=ROS/ROA*CS/CA
ZPR=ROS/ROB*CS/CB
TNPP(1)=REAL(NPP)*COS(AIMAG(NPP)/57.29578)
TNPP(2)=REAL(NPP)*SIN(AIMAG(NPP)/57.29578)
TTAPIN(1)=REAL(TAPIN)*COS(AIMAG(TAPIN)/57.29578)
TTAPIN(2)=REAL(TAPIN)*SIN(AIMAG(TAPIN)/57.29578)
110 CONTINUE
CAPOA=OMEGA*KAPA/RBR**2
CAPOB=OMEGA*KAPB/RBR**2
CAPOS=OMEGA*KAPS/RBR**2
XID=YTD*SQRT(KAPS/OMEGA)
RETURN
END

```

C  
C  
FUNCTION TAU(TW,TZRO,T)

C  
C  
FUNCTION TAU DETERMINES A DIMENSIONLESS TEMPERATURE THAT IS WIDELY  
C  
C  
USED THROUGHOUT THIS PROGRAM.

C  
TAU=(T-TZRO)/(TW-TZRO)  
RETURN  
END

```

C
C
SUBROUTINE SLDFAZ
C
C FOR A GIVEN VALUE OF MEAN BURNING RATE, RBR, SUBROUTINE SLDFAZ
C CALCULATES MEAN WALL TEMPERATURE, TWBAR.
C
INCLUDE CSTEAD, LIST
INCLUDE CUNSTD, LIST
C
NAMELIST/TPOUT1/TWBAR,QSDMLS,QMDMLS,QBDMLS,THETAA,CHI,D,B,KMLTLR,
IQLDMLS,FDMLS,GWBRS,DGWBR5
C
C
LFLAG=0
N5=1
DAM=0.
202 IF (LFLAG .EQ. 1) RETURN
IF (ITERA .EQ. 0 .OR. N5 .EQ. N5MAX) LFLAG=1
RBROLD=RBR
TWBAR=TM
TRLRBR=0.
DO 205 I=1,100
OLDTWB=TWBAR
OLDRBR=TRLRBR
DELTAT=.01*(TFLM-TM)
TWBAR=OLDTWB+DELTAT
QSDMLS=WA*QS/CA/(TWBAR-TZRO)
QMDMLS=WA*QLM/CA/(TWBAR-TZRO)
QLDMLS=QSDMLS
THETAA=E/R/TWBAR
CHI=(TWBAR-TZRO)/TWBAR
TRLRBR=SQRT(2.*KAPA*PRXFAC*QSDMLS*EXP(-THETAA)*
1(1.-EXP(-THETAA*CHI*(1.-TAU(TWBAR,TZRO,TM))))
2/(THETAA*CHI*((Z*(1.+(QLDMLS+QMDMLS)*CA/CS))**2
3-((TAU(TWBAR,TZRO,TM)*(1.-Z)-Z*QMDMLS*CA/CS)-1.))**2)))
IF (TRLRBR .GT. RBR) GO TO 210
205 CONTINUE
WRITE(6,208)
208 FORMAT(///T6,-NUMBER OF ITERATIONS FOR RBR HAS REACHED 100 IN SUBR
ROUTINE SLDFAZ-///)
STOP
210 TWBAR=OLDTWB+(TWBAR-OLDTWB)*(RBR-OLDRBR)/(TRLRBR-OLDRBR)
QSDMLS=WA*QS/CA/(TWBAR-TZRO)
QMDMLS=WA*QLM/CA/(TWBAR-TZRO)
QLDMLS=QSDMLS
QBDMLS=WB*QB/CB/(TWBAR-TZRO)
THETAA=E/R/TWBAR
CHI=(TWBAR-TZRO)/TWBAR
D=THETAA*CHI
B=KAPA*PRXFAC*QSDMLS/RBR/RBR
KMLTLR=B*EXP(-THETAA)/D
FDMLS=(QLDMLS+QMDMLS)*CA/CS+QBDMLS*CB/CS
GWBRS=-Z*(1.+(QLDMLS+QMDMLS)*CA/CS)
DGWBRS=-GWBRS+B*EXP(-THETAA)
WRITE(5,TPOUT1)
CALL GASFAZ($202)
RETURN
END

```



```

C
C
SUBROUTINE GASFAZ($)
C
C   GIVEN RBR AND TWBAR, SUBROUTINE GASFAZ CALCULATES FLAME STAND-OFF
C   DISTANCES, YSSTBR AND XSTBAR.
C
  INCLUDE CSTEAD, LIST
  INCLUDE CUNSTD, LIST
300 YSSTBR=ALOG((TAU(TWBAR,TZRO,TFLM)+FDMLS)/(1.+FDMLS))
  XSTBAR=YSSTBR*KAPS/RBR
  CALL AMULTI ($310)
310 RETURN
  END

```

```

C
C
SUBROUTINE AMULTI(I)
C
C SUBROUTINE AMULTI CALCULATES A VIRTUAL UNIMODAL AP PARTICLE
C   DIAMETER CORRESPONDING TO RBR AND YSSTBR.
C
  INCLUDE CSTEAD, LIST
500 AMM=KAPS*PBAR*YSSTBR/(KFLMHT*RBR*RBR)
  IF(LFLAG .EQ. 1) RETURN
  DAMOLD=DAM
  DAM=AMM-SMLA(JMAX)
  IF(ABS(DAM-DAMOLD) .GT. ABS(ABS(DAM)-ABS(DAMOLD))) GO TO 550
  DLTRBR=.01*RBR
  IF(DAM)510,520,530
510 RBR=RBR-DLTRBR
  GO TO 540
520 GO TO 540
530 RBR=RBR+DLTRBR
  GO TO 540
540 N5=N5+1
  RETURN1
550 RBR=RBROLD-(RBR-RBROLD)*DAMOLD/(DAM-DAMOLD)
  LFLAG=1
  RETURN
END

```

SUBROUTINE MELTLR

SUBROUTINE MELTLR DETERMINES TEMPORAL MEAN TEMPERATURE AND THE  
DERIVATIVE OF THIS TEMPERATURE WITH RESPECT TO DIMENSIONLESS  
DISTANCE AS FUNCTIONS OF DIMENSIONAL DISTANCE INTO THE LIQUID  
PROPELLANT (MEASURED FROM THE TEMPORAL MEAN POSITION OF THE  
MELTING SURFACE OF THE PROPELLANT).

INCLUDE CSTEAD, LIST  
INCLUDE CUNSTD, LIST  
COMMON/M/ M  
COMMON/N/ N  
COMMON/MLTINT/ P,NDEG

DELTAU=.01\*(1.-TAU(TWBAR,TZRO,TM))  
TAUT(1)=1.  
YABRT(1)=0.  
DO 505 I=2,101  
TAUT(I)=TAUT(I-1)-DELTAU  
ETA=D\*(1.-TAUT(I))  
CM=0.5+KMLTLR-0.5\*(Z\*(1.+(QLDMLS+QMDMLS)\*CA/CS))\*\*2  
C=(1.-2.\*CM)/KMLTLR  
ZI=C\*EXP(ETA)  
DNOM=1.+C-SQRT(C\*\*2+2.\*C)  
YABRT(I)=ALOG((1.+ZI-SQRT(ZI\*\*2+2.\*ZI))/DNOM)/(D\*SQRT(1.-2.\*CM))  
XMLTT(I)=KAPA\*YABRT(I)/RBR  
M=I  
505 CONTINUE  
DIMENSION P(10),W(200)  
CALL PFIT(M,YABRT,TAUT,-1.,6.,.TRUE...TRUE...TRUE.,P,NDEG,  
1 SIGFAC,W)  
NP3=NDEG+3  
WRITE(6,510) NDEG,SIGFAC,(P(I),I=1,NP3)  
510 FORMAT(/T5,-NDEG=-,I2,T17,-SIGFAC=-,F6.4/T5,-P(1),...,P(NDEG+3)=-  
1,T24,3F15.8/(T24,3F15.8))  
DO 530 I=1,M  
TAUFIT=SCPVAL(P,NDEG,YABRT(I))  
TAUERR=TAUT(I)-TAUFIT  
530 CONTINUE  
TAULR(1)=TAUMLT(100)  
DTAULR(1)=-Z\*(TAUMLT(100)+QMDMLS\*CA/CS)  
XLR(1)=YABRML(100)\*KAPA/RBR  
DSCRIM(1)=TAULR(1)+DTAULR(1)  
N=2  
RETURN  
END

C  
C  
C  
C  
C  
C  
C  
C  
C

# SUBROUTINE LAYERS

SUBROUTINE LAYERS DETERMINES TEMPORAL MEAN TEMPERATURE AND THE DERIVATIVE OF THIS TEMPERATURE WITH RESPECT TO DIMENSIONLESS DISTANCE AS FUNCTIONS OF DIMENSIONAL DISTANCE INTO THE SOLID PROPELLANT (MEASURED FROM THE TEMPORAL MEAN POSITION OF THE MELTING SURFACE OF THE PROPELLANT).

```
INCLUDE CSTEAD, LIST
INCLUDE CUNSTD, LIST
COMMON/N/ N
601 IF(N .EQ. 2) GO TO 610
602 IF(MOD(N,2) .EQ. 0) GO TO 615
605 DELTAY=DLTYBB
    DELTAX=SMLB
    C1=(1.-ZPR)*TAULR(N-1)
    GO TO 630
610 DELTAY=DLTYTP
    DELTAX=SMLATP
    C1=(1.-Z)*TAULR(1)
    GO TO 630
615 DELTAY=DLTYAB
    DELTAX=SMLA(1)
    C1=(1.-Z)*TAULR(N-1)
630 TAULR(N)=C1-(C1-TAULR(N-1))*EXP(-(DELTAY))
    DTAULR(N)=C1-TAULR(N)
    XLR(N)=XLR(N-1)+DELTAX
    DSCRIM(N)=TAULR(N)+DTAULR(N)
    IF(MOD(N,2) .EQ. 0) GO TO 6540
    ITOL=0
    IN=0
    IXTD=0
6400 IF(ABS(ABS(DSCRIM(N))-ABS(DSCRIM(N-2)))) .EQ. ABS(DSCRIM(N)-
    1DSCRIM(N-2)) .AND. ABS(DSCRIM(N)) .LT. TOL .AND. ABS(TAULR(N))
    2.LT. TOL) GO TO 6410
    GO TO 6420
6410 ITOL=1
    WRITE(6,6415)
6415 FORMAT(//6X,-TOLERANCE TESTS FOR A SATISFACTORY STEADY-STATE SOLUT
    1ION HAVE BEEN MET.--//)
6420 IF(N .LE. 100) GO TO 6430
    WRITE(6,6425)
6425 FORMAT(//6X,-MORE THAN FIFTY PAIR OF OXIDIZER AND BINDER LAYERS HA
    1VE BEEN TRAVERSED.--//)
    GO TO 6440
6430 IN=1
6440 IF(XLR(N-1) .GT. XTD) GO TO 6450
    WRITE(6,6445)
6445 FORMAT(//6X,-NUMBER OF LAYERS TRAVERSED IS INSUFFICIENT TO INSURE
    1SATISFACTORY ACCURACY OF THE PERTURBED SOLUTION.--//)
    GO TO 6460
6450 IXTD=1
6460 CONTINUE
6500 IF(ITOL .EQ. 1) GO TO 6510
    IF(IN .EQ. 1) GO TO 6530
    IF(IXTD .EQ. 1) GO TO 6550
6510 IF(IN .EQ. 1) GO TO 6520
```

```

      GO TO 6550
6520 IF(IXTD .EQ. 1) GO TO 6560
6530 GO TO 6540
6540 N=N+1
      GO TO 602
6550 IF(ABS(ABS(DSCIM(N))-ABS(DSCIM(N-2)))) .EQ. ABS(DSCIM(N)-
      IDSCIM(N-2))) WRITE(6,660)
660  FORMAT(/6X,-DISCRIMINANTS N AND N-2 HAVE THE SAME ALGEBRAIC SIGN.-)
      IF(ABS(DSCIM(N)) .LT. TOL) WRITE(6,665)
665  FORMAT(/6X,-ABS(DSCIM(N)) MEETS REQUIREMENTS FOR A SATISFACTORY S
      OLUTION.-)
      IF(ABS(TAULR(N)) .LT. TOL) WRITE(6,670)
670  FORMAT(/6X,-ABS(TAULR(N)) MEETS REQUIREMENTS FOR A SATISFACTORY SO
      LUTION.-)
      WRITE(6,6555)
6555 FORMAT(/6X,-THE ACCURACY OF THIS STEADY-STATE SOLUTION MAY BE SAT
      ISFACTORY$-/6X,-HOWEVER, IT HAS NOT MET ALL CONVERGENCE CRITERIA.-
      2/6X,-REFER TO THE PRECEDING DIAGNOSTIC REMARKS TO DETERMINE WHICH
      3CRITERIA-/6X,-HAVE BEEN MET AND WHICH HAVE NOT.-//)
      RETURN
6560 WRITE(6,6565)
6565 FORMAT(/6X,-A SATISFACTORY STEADY-STATE SOLUTION HAS BEEN OBTAIN
      ED.-//)
      RETURN
      END

```



SUBROUTINE LAYRSP

IN SUBROUTINE LAYRSP, AN INITIAL DEPTH WITHIN THE SOLID, ADEQUATE TO EXCEED SOME CHOSEN MULTIPLE OF THERMAL DEPTH AND TERMINATING ON THAT SURFACE OF A BINDER LAYER WHICH IS FARTHEST FROM THE BURNING SURFACE, IS DETERMINED. INITIAL VALUES OF DIMENSIONLESS TEMPERATURE AND ITS DERIVATIVE WITH RESPECT TO DIMENSIONLESS DISTANCE ARE THEN SPECIFIED ON THE FAR SIDE OF THE NEXT UNDERLYING OXIDIZER LAYER. DIMENSIONLESS TEMPERATURE IS ARBITRARILY ASSUMED. ITS DERIVATIVE IS APPROXIMATED FROM A REQUIREMENT THAT IS STRICTLY VALID ONLY FOR A HOMOGENEOUS SEMI-INFINITE SLAB.

INCLUDE CSTEAD, LIST  
INCLUDE CUNSTD, LIST

COMMON/N2/N2

COMPLEX LAM1, LAM2, C1, C2, TAP, GPM

```

N2=3
1601 IF(XLR(N2) .GT. XTD) GO TO 1605
N2=N2+2
GO TO 1601
1605 N2MXP1=N2+1
CAPO=CAPOA
A1=SQRT((SQRT(1.+16.*CAPO**2)+1.)/2)
B1=SQRT((SQRT(1.+16.*CAPO**2)-1.)/2)
LAM1=CMPLX(-0.5*(1.+A1),-0.5*B1)
DTAPIN=LAM1*TAPIN
N2=N2MXP1
DELTAY=-DLTYAB
TAPLR(N2)=TAPIN
TAP=TAPIN
DTAPLR(N2)=DTAPIN
GPM=DTAPIN
GO TO 1655
1607 IF(N2 .EQ. 2) GO TO 1630
1609 IF(MOD(N2,2) .EQ. 0) GO TO 1620
1610 DELTAY=-DLTYBB
CAPO=CAPOB
TAP=TAPLR(N2)
GPM=ZPR/Z*DTAPLR(N2)
GO TO 1655
1620 DELTAY=-DLTYAB
CAPO=CAPOA
TAP=TAPLR(N2)
GPM=Z/ZPR*DTAPLR(N2)
GO TO 1655
1630 DELTAY=-DLTYTP
CAPO=CAPOA
TAP=TAPLR(2)
GPM=Z/ZPR*DTAPLR(2)
1655 A1=SQRT((SQRT(1.+16.*CAPO**2)+1.)/2)
B1=SQRT((SQRT(1.+16.*CAPO**2)-1.)/2)

```

```

LAM1=CMPLX(-0.5*(1.+A1),-0.5*B1)
LAM2=CMPLX(-0.5*(1.-A1),+0.5*B1)
C1=(LAM2*TAP-GPM)/(LAM2-LAM1)
C2=-(LAM1*TAP-GPM)/(LAM2-LAM1)
TAPLR(N2-1)=C1*EXP(LAM1*DELTAY)+C2*EXP(LAM2*DELTAY)
DTAPLR(N2-1)=C1*LAM1*EXP(LAM1*DELTAY)+C2*LAM2*EXP(LAM2*DELTAY)
1665 N2=N2-1
IF(N2 .EQ. 1) RETURN
GO TO 1607
END

```

```

C
C
SUBROUTINE MLTLRP
C
C   GIVEN TAULR(1) AND DTAULR(1), SUBROUTINE MLTLRP INTEGRATES
C   STEP-BY-STEP FROM THE LIQUID-SOLID INTERFACE IN THE TOPMOST
C   OXIDIZER LAYER TO THE GAS-LIQUID INTERFACE THAT IS THE BURNING
C   SURFACE.  TAUOPS AND GOPPS ARE THUS DETERMINED FOR THE LIQUID
C   SIDE OF THE BURNING SURFACE.
C
C   INCLUDE CSTEAD, LIST
C   INCLUDE CUNSTD, LIST
C
COMMON/M/ M
COMMON/MLTINT/ P,NDEG
COMMON/N2/N2
C
C   DIMENSION P(10)
C
C
1500 INTEGER NEQ,KD,IFLAG,MXSTEP,KSTEP,KEMAX,KQ
      REAL EP,HMINA,HMAXA,EMAX
      REAL D2TAP,DT(10,1)
      REAL YABRV,DEPVAR(2)
      H=-.01*YABRT(M)
      HMINA=.1*H
      HMAXA=10.*H
      YABRVF=0.
      DELT=10.*H
1501 L=1
      YABRV=YABRT(M)
      DEPVAR(1)=REAL(TAPLR(1))
      DEPVAR(2)=REAL(DTAPLR(1))
      WRITE(6,1504)
1504 FORMAT(/T11,-YABRV-,T26,-TAPR-,T41,-DTAPR-,T55,-D2TAPR-/)
      GO TO 1507
1502 L=2
      YABRV=YABRT(M)
      DEPVAR(1)=AIMAG(TAPLR(1))
      DEPVAR(2)=AIMAG(DTAPLR(1))
      WRITE(6,1506)
1506 FORMAT(/T11,-YABRV-,T26,-TAPI-,T41,-DTAPI-,T55,-D2TAPI-/)
1507 CALL SVDQ(NEQ,YABRV,DEPVAR,D2TAP,KD,EP,IFLAG,H,HMINA,HMAXA,DELT,
1YABRVF,MXSTEP,KSTEP,KEMAX,EMAX,KQ,YN,DT)
      GO TO 20
10 CALL SVDQ1
20 GO TO (30,30,40,40,50,60,70,70), IFLAG
30 TAUFIT=SCPVAL(P,NDEG,YABRV)
      T3=KMLTLR*D*D*EXP(-D*(1.-TAUFIT))*DEPVAR(1)
      D2TAP=-DEPVAR(2)+T3
      GO TO 10
40 WRITE(6,1540) IFLAG, H
1540 FORMAT(/T6,-IFLAG=,I2,T21,-H=,E15.6)
45 WRITE(6,1545) YABRV,DEPVAR(1),DEPVAR(2),D2TAP
1545 FORMAT(/T6,4E15.6)
      IF(IFLAG.EQ. 3) GO TO 10
      IF(L.EQ. 1) GO TO 1552
      IF(L.EQ. 2) GO TO 1554
50 WRITE(6,1540) IFLAG, H

```

```

      GO TO 10
60  EP=32.*EMAX*EP
      WRITE(6,1560) YABRV,EP
1560 FORMAT(/T6,-OLD EP WAS TOO SMALL. NEW EP HAS BEEN ESTABLISHED AT Y
      1ABRV-/T8,-YABRV=-,E15.6,T36,-EP=-,E15.6)
      GO TO 10
70  WRITE(6,1540) IFLAG, H
      GO TO 10
1552 TAPR=DEPVAR(1)
      DTAPR=DEPVAR(2)
      D2TAPR=D2TAP
      GO TO 1502
1554 TAPI=DEPVAR(1)
      DTAPI=DEPVAR(2)
      D2TAPI=D2TAP
      TAUCPS=CMPLX(TAPR,TAPI)
      GOPPS=CMPLX(DTAPR,DTAPI)
      DGOPPS=CMPLX(D2TAPR,D2TAPI)
      N2=0
      RETURN
      END

```

SUBROUTINE GLIFP

SUBROUTINE GLIFP DETERMINES THE RESPONSE FUNCTION AND OTHER  
DEPENDENT VARIABLES ASSOCIATED WITH THE PERTURBED SOLUTION.  
THE EFFECT OF THE CONDENSED-PHASE ON THESE RESULTS IS DETERMINED  
SOLELY BY THE RATIO, GOPPS/TAUOPS, WHICH APPEARS IN THE FORMULA  
FOR RESPONSE FUNCTION, RF.

INCLUDE CSTEAD,LIST  
INCLUDE CUNSTD,LIST

COMPLEX K2

NAMelist/TPOUT3/K2,V3,V5,V6A,V6B,V7,RF0,K2NM,V5NM

K2=GOPPS/TAUOPS  
V3=Z\*(1.+(QMDMLS+QLDMLS)\*CA/CS)  
V5=(1.+THETAA/2.)\*CHI  
1+(D/2.)\*(1.-2.\*(1.-TAU(TWBAR,TZRO,TM))\*CHI)  
2/(EXP(D\*(1.-TAU(TWBAR,TZRO,TM)))-1.)  
3-1./(V3-(TAU(TWBAR,TZRO,TM)\*(1.-Z)-Z\*QMDMLS\*CA/CS-1.))  
V6A=EXP(YSSTBR)-1.  
V6B=(1.+FDMLS)\*YSSTBR\*EXP(YSSTBR)  
V7=Z\*QBDMLS\*CB/CS  
RF0=V6B/(2.\*V6B+V6A/V5+1./V5)  
RF=CAPOA\*V6B/(CAPOA\*(2.\*V6B+V6A/V5-V3/Z)+(0.,1.)\*KMLTLR\*D/Z  
1-(CAPOA/V5-(0.,1.)\*V3)\*K2/Z)  
NRP=RF\*NPP  
YSWP=(0.,-1.)\*NRP/CAPOS  
XWP=KAPS\*YSWP/RBR  
NXSTP=(1.-CMPLX(0.,-1./((CAPOS\*YSSTBR)))\*NRP-NPP  
XSTP=NXSTP\*XSTBAR  
NYSSTP=NXSTP  
YSSTP=NYSSTP\*YSSTBR  
IF(IHOMO.EQ.0) GO TO 1650  
K2NM=DTAPIN/TAPIN  
CAPCNM=1.  
V3NM=1.  
V5NM=THETAA\*CHI  
RFNMLT=CAPOA\*V6B/(CAPOA\*(2.\*V6B+V6A/V5NM-V3NM/Z)+(0.,1.)\*CAPCNM/Z  
1-(CAPOA/V5NM-(0.,1.)\*V3NM)\*K2NM/Z)  
NRPNM=RFNMLT\*NPP  
YSWPNM=(0.,1.)\*NRPNM/CAPOS  
XWPNM=KAPS\*YSWPNM/RBP  
NXSTPN=(1.-CMPLX(0.,-1./((CAPOS\*YSSTBR)))\*NRPNM-NPP  
XSTPNM=NXSTPN\*XSTBAR  
YSSTPN=NXSTPN\*YSSTBR  
1650 CONTINUE  
WRITE(6,TPOUT3)  
RETURN  
END



SUBROUTINE DTAOUT

SUBROUTINE DTAOUT PROVIDES A PRINTED RECORD OF THE RESULTS THAT  
HAVE ACCUMULATED DURING THE COURSE OF THE RUN.

INCLUDE CSTEAD, LIST  
INCLUDE CUNSTD, LIST

INTEGER KD,KQ

COMMON/M/ M  
COMMON/N/ N  
COMMON/N2/N2

NAMelist/INPUT/CA,CB,CG,KA,KB,ROA,ROB,WAC,SMLA,E,R,PRXFAC,QS,QB,  
IOLM,KFLMHT,TFLM,TM,TZRO,PBAR,RBR,TOL,ITERA,N5MAX,NPP,TAPIN,YTD,  
ZOMEGA,NEQ,KD,MXSTEP,EP,IHOMO  
NAMelist/OUTPT1/ JMAX,WA,DNM,WB,VFA,SMLATP,DLTYTP,DLTYAB,SMLB,  
IDLTYBB,KS,ROS,CS,KAPA,KAPB,KAPS,Z,ZPR  
NAMelist/OUTPT2/ THETAA,CHI,D,QSDMLS,QBDMLS,QMDMLS,FDMLS,B,KMLTLR  
NAMelist/OUTPT3/TWBAR,YSSTBR,XSTBAR,AMM,TAUMLT,XMLT,M,N,RBR,ITERA,  
IN5,N5MAX,LFLAG,GWBRS,DGWBRS,QLDMLS  
NAMelist/OUTPT4/ TAU LR,DTAU LR,XLR,DSCRIM,N,XTD,CAPOA,CAPOB,CAPOS  
NAMelist/OUTPT5/N2,N2MXP1,TAPIN,DTAPIN,XLR,TAPLR,DTAPLR,TAUOPS,  
1GOPPS,DGUPPS,RF,NRP,YSWP,XWP,NXSTP,XSTP,NYSSTP,YSSTP,  
2RFNMLT,NRPNM,YSWPNM,XWPNM,NXSTPN,XSTPNM,YSSTPN  
WRITE(6,INPUT)  
WRITE(6,OUTPT1)  
WRITE(6,OUTPT2)  
WRITE(6,OUTPT3)  
WRITE(6,OUTPT4)  
IF(ITERA.NE.0) RETURN  
WRITE(6,OUTPT5)  
RETURN  
END

```

SUBROUTINE PFIT (M,X,Y,SIG,NMAX,SEKN,COMTRN,CHBBAS,P,NFIT,SIGFAC,PFT00100
1W)
C      C.L.LAWSON, JPL, 1969 DEC 10
C      C.L.LAWSON, JPL, 1970 JAN 12      CALLING SEQUENCE CHANGED
C      LEAST SQUARES POLYNOMIAL FIT TO DISCRETE DATA.
C      M      NO. OF DATA POINTS
C      (X(I),I=1,M)  ABCISSAS OF DATA
C      (Y(I),I=1,M)  ORDINATES OF DATA
C      (SIG(I),I=1,M) STANDARD DEVIATIONS OF DATA Y(I)
C                      IF SIG(1) .LT. 0., THE SUBR WILL FUNCTION AS
C                      THOUGH ALL SIG(I) ARE EQUAL TO ABS(SIG(1))
C      NMAX      NMAX      SPECIFIES HIGHEST DEGREE POLYNOMIAL TO
C                      BE CONSIDERED.
C      SEKN      IF .TRUE.      THE SUBR WILL DETERMINE OPTIMUM
C                      NFIT NOT EXCEEDING NMAX.
C                      IF .FALSE. THE SUBR WILL SET NFIT = NMAX
C                      UNLESS THIS PRODUCES A NEAR-SINGULAR PROBLEM, IN
C                      WHICH CASE NFIT WILL BE REDUCED.
C      COMTRN = .TRUE.  SUBR WILL COMPUTE TRANSFORMATION PARAMETERS,
C                      P(1) AND P(2) SO THAT THE TRANSFORMED VARIABLE
C                      RANGES FROM -1. TO +1.
C                      = .FALSE. SUBR WILL USE P(1) AND P(2) AS SET BY USER.
C      CHBBAS = .TRUE.  MEANS USE CHEBYSHEV BASIS
C                      = .FALSE. MEANS USE MONOMIAL BASIS
C      (P(J),J=1,NMAX+3) P(1) AND P(2) DEFINE A TRANSFORMATION OF THE
C                      INDEPENDENT VARIABLE AS FOLLOWS..
C
C                      
$$S = (X - P(1)) / P(2)$$

C
C                      (P(I+3),I=0,...,NMAX) ARE POLY COEFFS COMPUTED
C                      BY THE SUBR. P(I+3) IS THE COEFF OF S**I
C                      IF MONOMIAL BASIS IS USED AND OF THE I-TH
C                      DEGREE CHEBY POLY IF THE CHEBY BASIS IS USED.
C
C                      IF NFIT .LT. NMAX THE COEFFS P(I+3) FOR
C                      I .GT. NFIT WILL BE SET TO ZERO.
C
C      NFIT      DEGREE OF POLY AS DETERMINED BY SUBROUTINE.
C      SIGFAC      FACTOR BY WHICH THE GIVEN SIG(I) VALUES SHOULD
C                      BE MULTIPLIED TO IMPROVE CONSISTENCY WITH THE
C                      FIT. SIGFAC IS THE SQUARE ROOT OF THE
C                      RATIO OF (THE SUM OF SQUARES OF RESIDUALS)
C                      TO (M-NFIT-1).
C      W(I)      WORKING SPACE. MUST BE DIMENSIONED AT LEAST
C                      ( MAX(2*NMAX,20) )*(NMAX+2)
C
C      LOGICAL    SEKN, COMTRN, CHBBAS
C      REAL       X(M),Y(M),SIG(M),P(1),W(1)

```

C		EPS = 2**(-27)	PFT06000
	DATA	EPS/ .745E-8/	PFT06100
	DATA	TOL/1.E-7/	PFT06200
	DATA	ONE,TWO,HALF/1.E0,2.E0,.5E0/, ZERO/0.E0/	PFT06300
C			PFT06400
C		DEFINE A(,) TO BE A FUNCTION	PFT06500
C		A(I,J)=W(I+(J-1)*IDIM)	PFT06600
C		A(I,J)=W(-IDIM+I+J*IDIM)	PFT06700
			PFT06800
		N=NMAX	PFT06900
		NP1=N+1	PFT07000
		NP2=NP1+1	PFT07100
		IF (N.LI.0.OR.M.LE.0) GO TO 320	PFT07200
		IDIM=MAX0(2*NMAX,20)	PFT07300
		SIGMA=ABS(SIG(1))	PFT07400
C		ZERO FIRST N+2 LOCATIONS OF COLUMN N+2	PFT07500
C		THIS IS DONE TO CLEAN UP OUTPUT IN CASES IN	PFT07600
C		WHICH M IS LESS THAN N+2. IT IS NOT	PFT07700
C		NECESSARY FOR THE COMPUTATION.	PFT07800
		DO 10 I=1,NP2	PFT07900
	10	A(I,NP2)=ZERO	PFT08000
			PFT08100
C		COMPUTE P(1),P(2) IF REQUESTED	PFT08200
C			PFT08300
C		CHANGE OF INDEPENDENT VARIABLE IS GIVEN BY S=(X-P(1))/P(2)	PFT08400
C		OR X=P(1) + P(2)*S	PFT08500
			PFT08600
		IF (COMTRN) GO TO 20	PFT08700
		IF (P(2)) 60,320,60	PFT08800
	20	CONTINUE	PFT08900
		XMIN=X(1)	PFT09000
		XMAX=XMIN	PFT09100
		IF (M.EQ.1) GO TO 40	PFT09200
		DO 30 I=2,M	PFT09300
		XMIN=AMIN1(XMIN,X(I))	PFT09400
	30	XMAX=AMAX1(XMAX,X(I))	PFT09500
	40	CONTINUE	PFT09600
		P(1)=(XMAX+XMIN)*HALF	PFT09700
		P(2)=(XMAX-XMIN)*HALF	PFT09800
		IF (P(2)) 60,50,60	PFT09900
	50	P(2)=ONE	PFT10000
C			PFT10100
C			PFT10200
	60	CONTINUE	PFT10300
C		INITIALIZE FOR ACCUMULATION	PFT10400
		CALL BHSLR1 (W,IDIM,NP1,A(1,NP2),IDIM,1,IR)	PFT10500
		I=1	PFT10600
C			PFT10700
C		ACCUMULATION LOOP BEGINS HERE	PFT10800
	70	MEQ=MIN0(IDIM-IR,M-I)+1	PFT10900
		IF (MEQ.LE.0) GO TO 150	PFT11000
		KMAX=IR+MEQ-1	PFT11100
		DO 140 K=IR,KMAX	PFT11200
		S=(X(I)-P(1))/P(2)	PFT11300
		IF (SIG(1)) 90,320,80	PFT11400
	80	SIGMA=SIG(I)	PFT11500
		IF (SIGMA) 320,320,90	PFT11600
	90	CONTINUE	PFT11700
		A(K,1)=ONE/SIGMA	PFT11800
		A(K,NP2)=Y(I)/SIGMA	

IF (N.LE.0) GO TO 130	PFT11900
IF (CHBBAS) GO TO 110	PFT12000
C	PFT12100
DO 100 J=2,NP1	PFT12200
100 A(K,J)=S*A(K,J-1)	PFT12300
GO TO 130	PFT12400
C	PFT12500
110 CONTINUE	PFT12600
A(K,2)=S/SIGMA	PFT12700
IF (N.EQ.1) GO TO 130	PFT12800
FAC=TWO*S	PFT12900
DO 120 J=3,NP1	PFT13000
120 A(K,J)=FAC*A(K,J-1)-A(K,J-2)	PFT13100
C	PFT13200
C	PFT13300
C	PFT13400
130 CONTINUE	PFT13500
I=I+1	PFT13600
140 CONTINUE	PFT13700
CALL BHSLR2 (MEQ,IR)	PFT13800
GO TO 70	PFT13900
150 CONTINUE	PFT14000
C	PFT14100
C	PFT14200
C	PFT14300
C	PFT14400
C	PFT14500
C	PFT14600
DO 160 I=1,NP1	PFT14700
160 P(I+2)=A(I,NP2)	PFT14800
C	PFT14900
C	PFT15000
C	PFT15100
C	PFT15200
C	PFT15300
C	PFT15400
IF (IR.GE.NMAX+3) GO TO 180	PFT15500
DO 170 J=1,NP2	PFT15600
170 A(IR,J)=ZERO	PFT15700
IR=IR+1	PFT15800
180 CONTINUE	PFT15900
C	PFT16000
C	PFT16100
K=IR-2	PFT16200
A(K+1,NP2)=ABS(A(K+1,NP2))	PFT16300
190 IF (K.LE.0) GO TO 200	PFT16400
CALL SL2NRM (2,A(K,NP2),A(K,NP2))	PFT16500
K=K-1	PFT16600
GO TO 190	PFT16700
200 CONTINUE	PFT16800
C	PFT16900
C	PFT17000
C	PFT17100
IRM1=IR-1	PFT17200
IMIN=1	PFT17300
TEMP=M	PFT17400
AMIN=A(1,NP2)	PFT17500
BIAS=AMIN*EPS	PFT17600
DO 210 I=1,IRM1	PFT17700
A(I,NP2)=A(I,NP2)/SQRT(TEMP)	



TEMP=AMAX1(TEMP-ONE,ONE)	PFT17800
IF (A(I,NP2).GE.AMIN) GO TO 210	PFT17900
AMIN=A(I,NP2)-BIAS	PFT18000
IMIN=1	PFT18100
210 CONTINUE	PFT18200
C	PFT18300
C	PFT18400
C	PFT18500
IF (SEEKN) GO TO 220	PFT18600
NFT=MIN0(NMAX,IR-3)	PFT18700
GO TO 230	PFT18800
220 NFT=IMIN-2	PFT18900
230 CONTINUE	PFT19000
NFT=MAX0(NFT,0)	PFT19100
C	PFT19200
C	PFT19300
C	PFT19400
C	PFT19500
C	PFT19600
C	PFT19700
N2=NFT+1	PFT19800
IF (N2.LT.2) GO TO 260	PFT19900
DO 240 I=2,N2	PFT20000
CALL SL2NRM (I-1,A(I,I),T)	PFT20100
IF (ABS(A(I,I)).LE.TOL*T) GO TO 250	PFT20200
240 CONTINUE	PFT20300
GO TO 260	PFT20400
250 NFT=I-2	PFT20500
260 CONTINUE	PFT20600
NFIT=NFT	PFT20700
C	PFT20800
C	PFT20900
C	PFT21000
SOLVE FOR COEFFS FOR DEGREE NFT	PFT21100
SIGFAC=A(NFT+2,NP2)	PFT21200
NFP1=NFT+1	PFT21300
DO 290 I=NFP1,1,-1	PFT21400
IP1=I+1	PFT21500
T=P(I+2)	PFT21600
IF (I.EQ.NFP1) GO TO 280	PFT21700
DO 270 J=IP1,NFP1	PFT21800
270 T=T-A(I,J)*P(J+2)	PFT21900
280 P(I+2)=T/A(I,I)	PFT22000
290 CONTINUE	PFT22100
IF (NFT.EQ.NMAX) GO TO 310	PFT22200
N1=NFT+2	PFT22300
N2=NMAX+1	PFT22400
DO 300 I=N1,N2	PFT22500
300 P(I+2)=ZERO	PFT22600
310 CONTINUE	PFT22700
RETURN	PFT22800
C	PFT22900
***** ERROR TERMINATION *****	PFT23000
320 CONTINUE	PFT23100
WRITE (6,330) M,SIG(1),N,COMTRN,P(2),SIGMA	PFT23200
NFIT=-1	PFT23300
RETURN	PFT23400
330 FORMAT (48H0BAD VALUES INPUT TO PFIT. NO FIT WILL BE DONE.,12X,1HP	PFT23500
1M,7X,6HSIG(1),9X,4HNMAX,7X,6HCOMTRN,9X,4HP(2),8X,5HSIGMA/48X,113,EP	PFT23600
213.5,113,L13,2E13.5/)	
END	



CIBFTC	BHSLR. LIST BASIC SEQ. LEAST SQUARES WITH H.H. TRANS.	30 APR 68	BHSL	10
C	BHSLR. S.P. BASIC SEQ. LEAST SQUARES WITH H.H. TRANS.	30 APR 68	BHSL	20
C	R. HANSON, J.P.L.		BHSL	30
C			BHSL	40
C	ENTRY POINTS BHSLR1,BHSLR2..		BHSL	50
C			BHSL	60
C	****		BHSL	70
C	SUBROUTINE BHSLR1 (A,NDA,N,B,NDB,NB,RI)		BHSL	80
C	****		BHSL	90
C	INTEGER SMI,RI,NDA,N,NDB,NB		BHSL	100
C			BHSL	110
C	START PLACING EQUUS. OF COND. AND RT. HAND SIDES IN ROW INDEXED		BHSL	120
C	WITH RI AND PROCEED DOWNWARD FOR MEQ EQUUS.		BHSL	130
C			BHSL	140
C	THE SPACE A(I,J),(I = 1,...,RI-1 ,J=1,...,I-1) IS FREE AND		BHSL	150
C	NEVER REFERENCED AGAIN BY THIS PROGRAM AS RI INCREASES TOWARD N+2.		BHSL	160
C			BHSL	170
C	NOW USE THE SECOND ENTRY BHSLR2.		BHSL	180
C	..		BHSL	190
C	REAL A(NDA,N),B(NDB,NB),UP,ZERO		BHSL	200
C	DATA ZERO/0.E0/		BHSL	210
C	RI=1		BHSL	220
C	SMI=0		BHSL	230
C	RETURN		BHSL	240
C			BHSL	250
C	PRIMARY ENTRY TO PACK ARRAY TO UPPER TRIANGULAR FORM.		BHSL	260
C	..		BHSL	270
C	****		BHSL	280
C	ENTRY BHSLR2(MEQ,RI)		BHSL	290
C	****		BHSL	300
C	..		BHSL	310
C	MEQ NEW EQUUS. AND RT. HAND SIDES ENTER.		BHSL	320
C			BHSL	330
C	IF (MEQ.LE.0) RETURN		BHSL	340
C	..		BHSL	350
C	NO TRANSFORMATIONS NEEDED.		BHSL	360
C			BHSL	370
C	SMI=SMI+MEQ		BHSL	380
C	M=RI+MEQ-1		BHSL	390
C	NT=MIN0(M,N)		BHSL	400
C	DO 20 IP=1,NT		BHSL	410
C	IF (IP.EQ.M) GO TO 20		BHSL	420
C	L=MAX0(0,RI-IP-1)		BHSL	430
C	CALL AHLR1 (A(1,IP),1,UP,IP-1,L,M,A(1,IP+1),1,NDA,N-IP)		BHSL	440
C	..		BHSL	450
C	COMPUTE TRANSFORMATION AND APPLY TO THE REMAINING COLUMNS.		BHSL	460
C			BHSL	470
C	CALL AHLR3 (A(1,IP),1,UP,IP-1,L,M,B,1,NDB,NB)		BHSL	480
C	..		BHSL	490
C	APPLY TRANSFORMATIONS TO B,IF PRESENT.		BHSL	500
C			BHSL	510
C	L=L+IP+1		BHSL	520
C	DO 10 I=L,M		BHSL	530
C	10 A(I,IP)=ZERO		BHSL	540
C	..		BHSL	550
C	CLEAR AREA JUST MADE IMPLICITLY ZERO.		BHSL	560
C			BHSL	570
C	20 CONTINUE		BHSL	580
C	RI=MIN0(SMI,N+1)+1		BHSL	590

IF (M.LE.N) RETURN	BHSL 600
IF (NB.LE.0) RETURN	BHSL 610
DO 30 J=1,NB	BHSL 620
30 CALL SL2NRM (M-N,B(N+1,J),B(N+1,J))	BHSL 630
C ..	BHSL 640
C PACK LENGTHS OF RT. HAND SIDES OUTSIDE THE COL. SPACE OF A	BHSL 650
C TO SINGLE LOCATIONS EACH.	BHSL 660
C ..	BHSL 670
C ADVANCE NEW ORIGIN OF ROW TO START EQU. OF CONDITION AND RT.SIDES	BHSL 680
C	BHSL 690
C	BHSL 700
L=N+2	BHSL 710
IF (L.GT.M) RETURN	BHSL 720
DO 40 J=1,NB	BHSL 730
DO 40 I=L,M	BHSL 740
40 B(I,J)=ZERO	BHSL 750
RETURN	BHSL 760
C ..	BHSL 770
C IF A SOLUTION IS DESIRED WITH FURTHER ACCUMULATION INTENDED,	BHSL 780
C SAVE THE UPPER TRIANGULAR PART OF THE A ARRAY AND THE FIRST	BHSL 790
C N+1 ROWS OF THE B ARRAY. FOLLOWING CALCULATION OF THE SOLUTION,	BHSL 800
C RESTORE THESE DATA AND ZERO THE PART OF A BELOW THE MAIN	BHSL 810
C DIAGONAL TOGETHER WITH THE (N+1)ST ROW. SEQ. ACCUMULATION MAY THEN	BHSL 820
C CONTINUE AS BEFORE. THE NUMBER OF ROWS IN THE PROCESSED MATRIX	BHSL 830
C TO BE SOLVED WILL BE RI-1.	BHSL 840
C	BHSL 850
C	BHSL 860
END	

C	BHTFLR LIST BASIC H.H. TRANS. FROM THE LEFT. S.P.	10 JUN 68	HTR00100
C	ENTRY POINTS..		HTR00200
C			HTR00300
C	AHLR1, AHLR2, AHLR3		HTR00400
C	11 FEB 1970		HTR00600
C	**		HTR00700
C	SUBROUTINE AHLR1 (U,NDU,UP,L1,L2,M,P,IRA,ICA,NCOLS)		HTR00800
C	**		HTR00900
	REAL U(NDU,M),UP,P(1),CL,ZERO		HTR01000
	DOUBLE PRECISION SM,DZERO,BETA		HTR01100
	LOGICAL SRCLAV,N1GTM,CMPU		HTR01200
	DATA DZERO/0.D0/		HTR01300
	DATA ZERO/0.E0/		HTR01400
C	**		HTR01500
C	DEFINE DATA FOR LITERALLY NAMED PROGRAM CONSTANTS.		HTR01600
C			HTR01700
	REAL AV,SR,AM,SGN		HTR01800
	AV(DUM)=ABS(DUM)		HTR01900
	SR(DUM)=SQRT(DUM)		HTR02000
	AM(D1,D2)=AMAX1(D1,D2)		HTR02100
	SGN(D1,D2)=SIGN(D1,D2)		HTR02200
C	**		HTR02300
C	DEFINE FUNCTIONS USED IN THIS SUBROUTINE.		HTR02400
C			HTR02500
	CMPU=.TRUE.		HTR02600
	SRCLAV=.FALSE.		HTR02700
C	**		HTR02800
C	ENTIRE RAW U VECTOR IN THE FIRST ROW OF U.		HTR02900
C			HTR03000
	GO TO 10		HTR03100
C	**		HTR03200
C	ENTRY AHLR2(U,NDU,UP,SRCL,L1,L2,M,P,IRA,ICA,NCOLS)		HTR03300
C	**		HTR03400
	REAL SRCL		HTR03500
	CMPU=.TRUE.		HTR03600
	SRCLAV=.TRUE.		HTR03700
C	**		HTR03800
C	RAW U VECTOR IN THE FIRST ROW OF U. LENGTH OF U VECTOR IS		HTR03900
C	AVAILABLE IN SRCL.		HTR04000
C			HTR04100
	GO TO 10		HTR04200
C	**		HTR04300
C	ENTRY AHLR3(U,NDU,UP,L1,L2,M,P,IRA,ICA,NCOLS)		HTR04400
C	**		HTR04500
	CMPU=.FALSE.		HTR04600
	SRCLAV=.FALSE.		HTR04700
C	**		HTR04800
C	U TRANSFORMATION CALCULATED AND IN U. PIVOT ELEMENT IS IN UP NOW.		HTR04900
C			HTR05000
10	IF (L1.LT.0.OR.L2.LT.0.OR.M.LE.0) RETURN		HTR05100
C	**		HTR05200
C	RETURN IF TRANSFORMATION IS ABSENT OR NOT WELL-DEFINED.		HTR05300
C			HTR05400
	N1=L1+L2+2		HTR05500
	N1GTM=N1.GT.M		HTR05600
	L1P1=L1+1		HTR05700
	IF (.NOT.CMPU) GO TO 50		HTR05800
	CL=SRCL		HTR05900
			HTR06000

IF (SRCLAV) GO TO 40	HTR06100
CL=U(1,L1P1)	HTR06200
IF (CL.LE.ZERO) CL=-CL	HTR06300
IF (N1GTM) GO TO 40	HTR06400
DO 20 J=N1,M	HTR06500
20 CL=AM(AV(U(1,J)),CL)	HTR06600
IF (CL.LE.ZERO) RETURN	HTR06700
SM=(U(1,L1P1)/CL)**2	HTR06800
DO 30 J=N1,M	HTR06900
30 SM=SM+(U(1,J)/CL)**2	HTR07000
CL=CL*SR(SM)	HTR07100
C ..	HTR07200
C COMPUTE LENGTH OF U VECTOR IF SRCLAV = .FALSE..	HTR07300
C	HTR07400
40 IF (CL.LE.ZERO) RETURN	HTR07500
CL=-SGN(CL,U(1,L1P1))	HTR07600
UP=U(1,L1P1)-CL	HTR07700
U(1,L1P1)=CL	HTR07800
50 IF (NCOLS.LE.0) RETURN	HTR07900
C ..	HTR08000
C RETURN IF MATRIX P IS ABSENT.	HTR08100
C	HTR08200
BETA=-U(1,L1P1)*UP	HTR08300
IF (BETA.EQ.DZERO) RETURN	HTR08400
C ..	HTR08500
C IF BETA.EQ.ZERO, NO TRANSFORMATION IS NECESSARY.	HTR08600
C	HTR08700
DO 90 J=1,NCOLS	HTR08800
C	HTR08900
C APPLY HOUSEHOLDER TRANSFORMATION (I - 2*U*U**(T)) TO P	HTR09000
C FROM THE LEFT.	HTR09100
C	HTR09200
C	HTR09300
C IRA = NUMBER OF ROWS CELLS OF P ARE APART.	HTR09400
C	HTR09500
C ICA = NUMBER OF CELLS COLUMNS OF P ARE APART.	HTR09600
C	HTR09700
C U = (0,...,(L1 ZEROS), UP,0,...,(L2 ZEROS), U(L1+L2+2),...,U(M))	HTR09800
C L1 .GE. 0, L2 .GE. 0.	HTR09900
C ..	HTR10000
C I1=ICA*(J-1)	HTR10100
C I2=I1+L1*IRA+1	HTR10200
C I4=I1+(N1-1)*IRA+1	HTR10300
C SM=P(I2)*UP	HTR10400
C IF (N1GTM) GO TO 70	HTR10500
C I3=I4	HTR10600
C DO 60 I=N1,M	HTR10700
C SM=SM+P(I3)*U(1,I)	HTR10800
60 I3=I3+IRA	HTR10900
70 IF (SM.EQ.DZERO) GO TO 90	HTR11000
C ..	HTR11100
C TRANSFORMATION LEAVES THAT COLUMN OF P ALONE.	HTR11200
C SM=SM/BETA	HTR11300
C P(I2)=P(I2)-UP*SM	HTR11400
C IF (N1GTM) GO TO 90	HTR11500
C I3=I4	HTR11600
C DO 80 I=N1,M	HTR11700
C P(I3)=P(I3)-SM*U(1,I)	HTR11800
80 I3=I3+IRA	HTR11900

AD-A060 045

JET PROPULSION LAB PASADENA CALIF

F/G 19/1

COMBUSTION RESPONSE MODELING FOR COMPOSITE SOLID PROPELLANTS.(U)

JUN 78 N S COHEN, J M BOWYER

F04611-76-X-0050

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JPL-PUB-78-59

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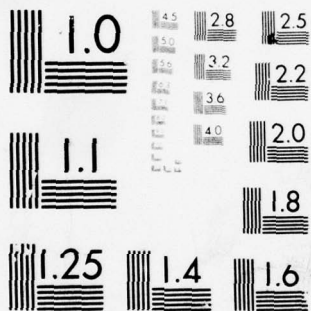
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MICROCOPY RESOLUTION TEST CHART  
NATIONAL BUREAU OF STANDARDS-1963-A

C    ..  
C    BASIC STEP OF HOUSEHOLDER TRANSFORMATION.  
C  
C    90 CONTINUE  
C    ..  
C    RETURN WITH TRANSFORMATION APPLIED FROM THE LEFT.  
C  
C    RETURN  
C    END

HTR12000  
HTR12100  
HTR12200  
HTR12300  
HTR12400  
HTR12500  
HTR12600  
HTR12700  
HTR12800

	SUBROUTINE SL2NRM (N,U,G)	L2N00100
C	MODIFIED BY C J DEVINE 3/21/72 TO ALLOW ADDRESS OF .GT. 16 BITS FOR ARGS	
C	IN CALLING SEQ	DUMMY DIMENSION ARRAY G(1),
C	WAS DEFINED . THIS ALLOWS PROGRAM TO REFERENCE LOCATIONS IN EXT. CORE	
C	ENR2. S.P. AND D.P. L2 NORM FOR ARRAY BASED VECTORS 22 APR 68	L2N00200
C	11 FEB 1970	L2N00300
	REAL U(1), G(1)	L2N00400
	F1=0.E0	L2N00500
	F2=0.E0	L2N00600
	IF (N.LE.0) GO TO 20	L2N00700
	DO 10 J=1,N	L2N00800
10	F1=AMAX1(F1,ABS(U(J)))	L2N00900
	IF (F1.NE.0.) GO TO 30	L2N01000
20	G(1)=0.0E0	L2N01100
	RETURN	L2N01200
30	DO 40 J=1,N	L2N01300
	T=U(J)/F1	L2N01400
40	F2=F2+T*T	L2N01500
	G(1)=F1*SQRT(F2)	L2N01600
	RETURN	L2N01700
	END	L2N01800

```

C      FUNCTION SCPVAL (P,NDEGP,X)
C
C      C.L.LAWSON,JPL, 1969 DEC 17   MODIFIED 1973 JULY 24
C
C      MODIFIED 1974 NOV 19
C
C      EVALUATE A POLYNOMIAL OF DEGREE NDEGP GIVEN TRANSFORMATION
C      PARAMETERS, P(1) AND P(2), AND COEFFICIENTS RELATIVE TO THE
C      CHEBYSHEV BASIS.
C
C      NDEGP          DEGREE OF POLYNOMIAL
C      (P(1),I=1,NDEGP+3)  PARAMETERS DEFINING THE POLYNOMIAL
C      X              INPUT ARGUMENT
C      THE POLYNOMIAL-S VALUE AT X IS DEFINED AS FOLLOWS.
C
C      
$$S = (X - P(1)) / P(2)$$

C
C      SCPVAL=SUM OF P(I+3)*T(I,S) FOR I=0,1,...NDEGP
C
C      WHERE T(I,S) DENOTES THE CHEBYSHEV
C      POLYNOMIAL OF DEGREE I EVALUATED AT S .
C
C      REAL          P(1),W(3),S,S2,X
C      W(1)=0.
C      W(2)=0.
C
C      TRANSFORM X TO S
C
C      S=(X-P(1))/P(2)
C      S2=S+S
C      J=NDEGP+3
C
C      EVALUATE POLYNOMIAL USING RECURSION
C
C      10  IF(J .LE. 3) GO TO 20
C           W(3)=W(2)
C           W(2)=W(1)
C           W(1)=(S2*W(2)-W(3))+P(J)
C           J = J - 1
C           GO TO 10
C      20  SCPVAL=(S*W(1)-W(2))+P(3)
C           RETURN
C           END

```

SUBROUTINE SVDQ (NEQ,T,Y,F,KD,EP,IFLAG,H,HMINA,HMAXA,DELT,  
1 TFINAL,MXSTEP,KSTEP,KEMAX,EMAX,KQ,YN,DT)

VARIABLE ORDER INTEGRATION SUBROUTINE FOR THE  
SOLUTION OF ORDINARY DIFFERENTIAL EQUATIONS

ANALYSIS AND CODING BY FRED T. KROGH, AT THE JET PROPULSION  
LABORATORY, PASADENA, CALIF. APRIL 1, 1969.  
THIS SUBROUTINE DESIGNED FOR THE IBM 7094 AND THE UNIVAC 1108.

AT THE END OF THIS LISTING INSTRUCTIONS ARE GIVEN FOR REMOVING  
SOME FEATURES AND FOR ADDING OTHERS. THE GSTOP FEATURE IS  
EXPLAINED NEAR THE END OF THE LISTING.

VARIABLES IN THE CALLING SEQUENCE HAVE THE FOLLOWING TYPES.  
INTEGER NEQ,KD(1),IFLAG,MXSTEP,KSTEP,KEMAX,KQ(1)  
REAL F(1),EP(1),HMINA,HMAXA,EMAX,DT(10,1)  
REAL T,Y(1),H,DELT,TFINAL,YN(1)

PARAMETERS WHICH MUST BE ASSIGNED VALUES BEFORE CALLING  
SVDQ ARE NEQ, T, Y, KD, H, HMINA, HMAXA, DELT,  
TFINAL, AND MXSTEP.

SVDQ IS USED ONLY ON THE INITIAL ENTRY. ALL OTHER  
ENTRIES ARE MADE BY CALLING SVDQ1. IN ADDITION TO  
THE PARAMETERS MENTIONED ABOVE THE USER MUST ASSIGN  
VALUES TO F (ONCE PER STEP INITIALLY, AND TWICE PER STEP  
AFTER GETTING STARTED) AND EP (EITHER INITIALLY, OR DURING  
THE INTEGRATION IF A RELATIVE ERROR TEST IS USED).  
THE FOLLOWING PARAMETERS GIVE ADDITIONAL INFORMATION ABOUT THE  
INTEGRATION AND ARE USED FOR STORAGE. THEY SHOULD NOT BE  
CHANGED BY THE USER. IFLAG,KSTEP,KEMAX,EMAX,KQ,YN, AND DT.

AN EXAMPLE OF HOW ONE MIGHT SET UP THE CALLS TO SVDQ IS GIVEN  
BELOW.

CALL SVDQ(NEQ,....,DT)

GO TO YYY

XXX CALL SVDQ1

YYY GO TO (N1,N2,....,N8), IFLAG

AFTER THE INITIAL CALL, RETURN TO SVDQ WITH

GO TO XXX

IF NO ERROR HAS BEEN MADE, IFLAG WILL EQUAL 1 AFTER THE INITIAL  
CALL INDICATING THE DERIVATIVES ARE TO BE COMPUTED.

THE USAGE OF THE VARIABLES IS GIVEN BELOW.

NEQ=NUMBER OF EQUATIONS (INPUT)

T=INDEPENDENT VARIABLE (INITIAL VALUE SUPPLIED BY THE USER)

Y=CURRENT VALUE OF DEPENDENT VARIABLE. THE INITIAL  
VALUE OF Y MUST BE SPECIFIED BY THE USER BEFORE  
THE FIRST ENTRY. THE DIMENSION OF Y MUST BE  
AT LEAST AS GREAT AS THE SUM OF THE ORDERS OF  
THE DIFFERENTIAL EQUATIONS WHICH ARE BEING  
INTEGRATED. IF WE LET KD(I) DENOTE THE ORDER  
OF THE I-TH DIFFERENTIAL EQUATION, THEN Y(J)

SVDQ0001  
SVDQ0002  
SVDQ0003  
SVDQ0004  
SVDQ0005  
SVDQ0006  
SVDQ0007  
SVDQ0008  
SVDQ0009  
SVDQ0010  
SVDQ0011  
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SVDQ0055  
SVDQ0056  
SVDQ0057  
SVDQ0058  
SVDQ0059



C	IS THE K-TH DERIVATIVE OF THE L-TH COMPONENT,	SVDQ0060
C	WHERE L IS THE SMALLEST INTEGER FOR WHICH	SVDQ0061
C	$KD(1)+KD(2)+\dots+KD(L) \geq J$ AND $K=KD(L)+J-1-(KD(1)$	SVDQ0062
C	$+KD(2)+\dots+KD(L))$ , $J=1,2,\dots,(KD(1)+KD(2)+\dots+KD(NEQ))$ .	SVDQ0063
C	(FOR EXAMPLE, FOR THE SYSTEM $F(1)=UPP$ , $F(2)=VPP$ , WHERE P	SVDQ0064
C	DENOTES A PRIME, $Y(1)=U$ , $Y(2)=UP$ , $Y(3)=V$ , $Y(4)=VP$ .)	SVDQ0065
C		SVDQ0066
C	$F(I)=KD(I)$ -TH DERIVATIVE OF THE I-TH COMPONENT WITH RESPECT	SVDQ0067
C	TO T, $I=1,2,\dots,NEQ$ . THE USER MUST PROVIDE	SVDQ0068
C	THE CODE WHICH COMPUTES F GIVEN Y AND T.	SVDQ0069
C		SVDQ0070
C	KD GIVES THE ORDER OF THE DIFFERENTIAL EQUATIONS IN THE	SVDQ0071
C	SYSTEM. KD MUST BE LESS THAN OR EQUAL TO 4.	SVDQ0072
C	(FOR DIFFERENTIAL EQUATIONS WITH DIFFERENT ORDERS SET	SVDQ0073
C	$KD.LT.0$ . IF THIS IS DONE IT IS ASSUMED THAT KD IS A VECTOR	SVDQ0074
C	AND THAT $ABS(KD(I))$ GIVES THE ORDER OF THE I-TH EQUATION.)	SVDQ0075
C		SVDQ0076
C	EP IS A PARAMETER USED TO CONTROL THE LOCAL ERROR.	SVDQ0077
C	IF EP IS POSITIVE THE LOCAL ERROR IS KEPT LESS	SVDQ0078
C	THAN EP IN ALL COMPONENTS OF THE DIFF. EQ.	SVDQ0079
C	(THE ESTIMATED LOCAL ERROR IS KEPT LESS THAN EP IN	SVDQ0080
C	THE $(KD(I)-1)$ -ST DERIVATIVE OF THE I-TH COMPONENT. THUS	SVDQ0081
C	FOR EQUATIONS WITH ORDER GREATER THAN ONE, THE ERROR	SVDQ0082
C	IN A DERIVATIVE IS ESTIMATED. IN THIS CASE THE VALUE OF	SVDQ0083
C	EP REQUIRED TO OBTAIN A GIVEN ACCURACY IN THE DEPENDENT	SVDQ0084
C	VARIABLE DEPENDS ON THE SCALING.)	SVDQ0085
C	IF $EP.LT.0$ , THEN IT IS ASSUMED THAT EP	SVDQ0086
C	IS A VECTOR. LET K BE THE SMALLEST VALUE	SVDQ0087
C	OF I FOR WHICH $EP(I) \geq 0$ . FOR $I.LT.K$	SVDQ0088
C	THE LOCAL ERROR CONTROL IS BASED ON	SVDQ0089
C	$ABS(EP(I))$ , AND FOR $I \geq K$ IT IS BASED ON	SVDQ0090
C	$EP(K)$ . IF ONE WANTS A RELATIVE ERROR TEST--	SVDQ0091
C	FOR EXAMPLE, THE LOCAL ERROR IS TO BE KEPT	SVDQ0092
C	LESS THAN $C \cdot P$ WHERE C IS A CONSTANT	SVDQ0093
C	AND P IS A POSITIVE FUNCTION OF T AND Y,	SVDQ0094
C	THEN ONE SHOULD SET $EP=C \cdot P$ WHEN $IFLAG=1$ .	SVDQ0095
C	IF $EP=0$ AND $HMAXA.NE.0$ , $IFLAG$ IS SET EQUAL 8. IF $EP=0$ AND $HMAXA=0$ ,	SVDQ0096
C	NO ERROR TESTS ARE PERFORMED AND THE ORDER(S) AND STEPSIZE ARE	SVDQ0097
C	NOT CHANGED. THIS OPTION SHOULD NOT BE USED IF $KQ(I)=1$ FOR ANY I.	SVDQ0098
C		SVDQ0099
C	$IFLAG$ IS USED FOR COMMUNICATION BETWEEN THE INTEGRATOR	SVDQ0100
C	AND THE PROGRAM WHICH CALLS IT. THE VALUE	SVDQ0101
C	OF $IFLAG$ SHOULD NOT BE CHANGED BY THE USER.	SVDQ0102
C	THE FOLLOWING VALUES OF $IFLAG$ HAVE THE FOLLOWING MEANINGS.	SVDQ0103
C	=1 THE VALUE OF Y FOR THE CURRENT STEP HAS BEEN	SVDQ0104
C	PREDICTED. THE USER SHOULD COMPUTE F AND CALL SVDQ1.	SVDQ0105
C	IF A RELATIVE ERROR TEST IS USED THE NEW VALUE	SVDQ0106
C	OF EP SHOULD ALSO BE COMPUTED HERE.	SVDQ0107
C	=2 THE VALUE OF Y FOR THE CURRENT STEP HAS BEEN	SVDQ0108
C	CORRECTED. THE USER SHOULD COMPUTE F AND CALL SVDQ1.	SVDQ0109
C	=3 AN OUTPUT POINT HAS BEEN REACHED (SEE DESCRIPTION	SVDQ0110
C	OF DELT), PRINT RESULTS AND CALL SVDQ1.	SVDQ0111
C	=4 $T=TFINAL$ IF SVDQ1 IS CALLED WITH $T=TFINAL$ AND	SVDQ0112
C	$IFLAG=4$ , $IFLAG$ IS SET EQUAL TO 8. IF THE VALUE OF	SVDQ0113
C	$TFINAL$ IS CHANGED THE INTEGRATION WILL CONTINUE.	SVDQ0114
C	=5 $KSTEP=KSOUT$ (SEE THE DESCRIPTION OF $MXSTEP$ ).	SVDQ0115
C	=6 $EMAX.GT..1$ AND IT APPEARS TO THE SUBROUTINE THAT	SVDQ0116
C	REDUCING H WILL NOT HELP BECAUSE OF ROUND-OFF ERROR.	SVDQ0117
C	IF THIS OCCURS A LARGER VALUE OF EP (OR OF $ABS(EP(KEMAX))$ ) IF	SVDQ0118

EP IS A VECTOR) SHOULD PROBABLY BE USED. IF EP IS NOT  
 INCREASED, TOO SMALL A STEPSIZE IS LIABLE TO BE USED. (WE HAVE  
 FOUND THAT REPLACING EP WITH  $32.*EMAX*EP$  WORKS QUITE WELL.)  
 INCREASING EP IN THIS WAY WILL NOT DEGRADE THE ACCURACY,  
 HOWEVER IF THE NATURE OF THE PROBLEM CHANGES IT MAY PAY TO  
 USE A SMALLER VALUE OF EP LATER IN THE INTEGRATION.  
 =7 ABS(H).LT.HMINA. TO CONTINUE WITH THE CURRENT  
 VALUE OF H, SET HMINA.LE.ABS(H) AND CALL SVDQ1.  
 IF THE INTEGRATOR HAS JUST HALVED H ONE MAY CONTINUE  
 WITH TWICE THE STEPSIZE BY SIMPLY CALLING SVDQ1. (SUCH  
 AN ACTION IS RISKY WITHOUT A CAREFUL ANALYSIS OF THE  
 SITUATION.) IF THE STEPSIZE HAS NOT JUST BEEN HALVED  
 (ABS(H).LT.HMINA MAY BE DUE TO THE USER INCREASING THE  
 VALUE OF HMINA OR TO HAVING TOO SMALL AN H AT THE END  
 OF THE STARTING PHASE.) THE INTEGRATION WILL CONTINUE  
 WITH THE CURRENT VALUE OF H AND A RETURN TO THE USER WITH  
 IFLAG=7 WILL BE MADE ON EVERY STEP UNTIL ABS(H).GE.HMINA.  
 =8 ILLEGAL PARAMETER IN THE CALLING SEQUENCE. IF SVDQ1  
 IS CALLED WITH IFLAG=8 THE PROGRAM IS STOPPED.  
 H=CURRENT VALUE OF THE STEPSIZE. IN SELECTING THE INITIAL  
 VALUE FOR H, THE USER SHOULD REMEMBER THE FOLLOWING--  
 1. THE INTEGRATOR IS CAPABLE OF CHANGING H QUITE QUICKLY AND  
 THUS THE INITIAL CHOICE IS NOT CRITICAL.  
 2. IF IT DOES NOT LEAD TO PROBLEMS IN COMPUTING THE DERIVATIVES  
 (E.G. BECAUSE OF OVERFLOW OR TRYING TO EXTRACT THE SQUARE  
 ROOT OF A NEGATIVE NUMBER), IT IS BETTER TO CHOOSE H MUCH  
 TOO LARGE THAN MUCH TOO SMALL.  
 3. IF H\*DELT.LE.0 INITIALLY, AN IMMEDIATE RETURN IS MADE  
 WITH IFLAG=8. THE SIGN OF H IS WHAT DETERMINES THE  
 DIRECTION OF INTEGRATION.  
 4. IF DELT=H\*(2\*\*K) K A NONNEGATIVE INTEGER THEN OUTPUT  
 VALUES WILL BE OBTAINED WITHOUT DOING AN INTERPOLATION.  
 HMINA AFTER GETTING STARTED, AND WHENEVER H  
 IS HALVED, ABS(H) IS COMPARED WITH HMINA.  
 IF ABS(H).LT.HMINA CONTROL IS RETURNED TO  
 THE USER WITH IFLAG=7.  
 HMAXA THE STEPSIZE IS NOT DOUBLED IF  
 DOING SO WOULD MAKE ABS(H).GT.HMAXA  
 DELT ENABLES THE USER TO SPECIFY THE POINTS WHERE  
 OUTPUT IS DESIRED. LET TOUT=DELT + THE VALUE OF T THE LAST  
 TIME CONTROL WAS RETURNED TO THE USER WITH IFLAG=3. (INITIALLY  
 TOUT=THE INITIAL VALUE OF T.) CONTROL IS RETURNED TO THE  
 USER WITH IFLAG=3 WHENEVER T=TOUT. IF TOUT DOES NOT FALL  
 ON AN INTEGRATION STEP, OUTPUT VALUES ARE OBTAINED BY  
 INTERPOLATION ON THE FIRST STEP THAT (T-TOUT)\*H.GT.0.  
 INTERPOLATED VALUES FOR BOTH Y AND F ARE COMPUTED.  
 (NOTE THAT A RETURN WITH IFLAG=3 IS ALWAYS MADE  
 BEFORE TAKING THE FIRST STEP.)  
 TFINAL CONTROL IS RETURNED TO THE USER WITH IFLAG=4 WHEN  
 T REACHES TFINAL. IF TFINAL DOES NOT FALL ON AN INTEGRATION  
 STEP VALUES AT TFINAL ARE OBTAINED BY EXTRAPOLATION.  
 MXSTEP ON THE INITIAL ENTRY, AND ON ENTRIES  
 WITH 2.LT.IFLAG.LT.6 KSOUT IS SET EQUAL TO

C	KSTEP+MXSTEP. AT THE END OF EACH STEP KSTEP IS INCREMENTED	SVDQ0178
C	AND COMPARED WITH KSOUT. IF KSTEP.GE.KSOUT CONTROL IS	SVDQ0179
C	RETURNED TO THE USER WITH IFLAG=5. (THUS IF DELT IS	SVDQ0180
C	SUFFICIENTLY LARGE, CONTROL WILL BE RETURNED TO THE USER	SVDQ0181
C	WITH IFLAG=5 EVERY MXSTEP STEPS.)	SVDQ0182
C		SVDQ0183
C	KSTEP=NUMBER OF INTEGRATION STEPS TAKEN (COMPUTED	SVDQ0184
C	BY THE INTEGRATOR.)	SVDQ0185
C		SVDQ0186
C	KEMAX=INDEX OF COMPONENT RESPONSIBLE FOR THE	SVDQ0187
C	VALUE OF EMAX (SEE BELOW).	SVDQ0188
C		SVDQ0189
C	EMAX=LARGEST VALUE IN ANY COMPONENT OF (ESTIMATED ERROR)/EP	SVDQ0190
C	ORDINARILY THE STEPSIZE IS HALVED IF EMAX.GT..1. WITH A	SVDQ0191
C	RECENT HISTORY OF LOCAL ROUND-OFF PROBLEMS VALUES OF EMAX AS	SVDQ0192
C	LARGE AS 1 ARE PERMITTED. THE STEPSIZE IS NOT HALVED ON ANY	SVDQ0193
C	STEP THAT ROUND OFF ERROR APPEARS TO BE LIMITING THE PRECISION.	SVDQ0194
C		SVDQ0195
C	KQ(1)=HIGHEST ORDER DIFFERENCE USED IN INTEGRATING	SVDQ0196
C	THE 1-TH EQUATION. (COMPUTED BY THE INTEGRATOR)	SVDQ0197
C		SVDQ0198
C	YN=A VECTOR WITH THE DIMENSION OF Y USED TO STORE	SVDQ0199
C	THE VALUE OF Y AT THE END OF EACH INTEGRATION STEP.	SVDQ0200
C		SVDQ0201
C	DT=AN ARRAY WITH DIMENSION DT(10,NEQ) USED TO	SVDQ0202
C	STORE THE DIFFERENCE TABLE.	SVDQ0203
C		SVDQ0204
C		SVDQ0205
C	REAL TOUT,TL,TPD,TPD1,TPD2,HH,FAC	SVDQ0206
C	DIMENSION DD(12),D(11),GAM(10,4),GAS(10),PT(11),FAC(3)	SVDQ0207
C	EQUIVALENCE(DD(2),D(1))	SVDQ0208
C		SVDQ0209
C	DATA KMAXO/4/	SVDQ0210
C	KMAXO IS THE MAXIMUM ORDER DIFFERENTIAL EQUATION	SVDQ0211
C	THIS SUBROUTINE WILL INTEGRATE.	SVDQ0212
C		SVDQ0213
C	DATA FAC/1.E0,.5E0,.166666667E0/	SVDQ0214
C	FAC(J)=1/(FACTORIAL J), J=1,2,...,MAX(2,KMAXO-1)	SVDQ0215
C		SVDQ0216
C	DATA KQMAX/9/	SVDQ0217
C	KQMAX GIVES THE MAXIMUM ORDER.	SVDQ0218
C	THERE IS LITTLE POINT IN HAVING KQMAX MUCH BIGGER THAN THE NUMBER	SVDQ0219
C	OF DECIMAL DIGITS IN THE MANTISSA.	SVDQ0220
C	IF KQMAX IS SET LESS THAN 6, DT, D, AND PT SHOULD BE DIMENSIONED	SVDQ0221
C	AS IF KQMAX=6.	SVDQ0222
C		SVDQ0223
C	DATA RND,KBIT2/6.0E-8,56/	SVDQ0224
C	RND IS APPROXIMATELY 2**((3-B) WHERE B IS	SVDQ0225
C	THE NUMBER OF BITS IN THE MANTISSA.	SVDQ0226
C	KBIT2=2*B+2 WHERE B IS THE NUMBER OF BITS IN THE MANTISSA.	SVDQ0227
C	IF THE DERIVATIVES ARE NOT COMPUTED TO THE ACCURACY EXPECTED	SVDQ0228
C	FROM THE WORD LENGTH OF THE COMPUTER (FOR EXAMPLE BECAUSE OF	SVDQ0229
C	CANCELLATION PROBLEMS OR TABULAR DATA), THEN THESE CONSTANTS	SVDQ0230
C	CAN BE CHANGED TO REFLECT THE NUMBER OF BITS WHICH ARE	SVDQ0231
C	SIGNIFICANT IN THE COMPUTED DERIVATIVES. (THIS IS NOT NECESSARY.	SVDQ0232
C	BUT IS WISE IF THE ACCURACY REQUESTED IS DIFFICULT TO OBTAIN	SVDQ0233
C	BECAUSE THE DERIVATIVES HAVE SO FEW SIGNIFICANT DIGITS.)	SVDQ0234
C		SVDQ0235
C	DATA P1,P01,P25,P3E1/.1,.01,.25,3./	SVDQ0236



C	THE ABOVE DATA STATEMENT CONTAINS VARIOUS CONSTANTS	SVDQ0237
C	USED IN THE SUBROUTINE.	SVDQ0238
C		SVDQ0239
	DATA PT/1.,2.,4.,8.,16.,32.,64.,128.,256.,512.,1024./	SVDQ0240
C	PT(J)=2**(J-1), J=1,2,...,KQMAX+2	SVDQ0241
	EQUIVALENCE (PT(1),PTS1),(PT(2),PTS2),(PT(3),PTS3),(PT(4),PTS4),	SVDQ0242
	1 (PT(5),PTS5),(GAM(2,1),P5)	SVDQ0243
C		SVDQ0244
	DATA GAS/1.,-.5,-8.33333333E-02,-4.16666667E-02,	SVDQ0245
	1 -2.63888889E-02,-1.875E-02,-1.42691799E-02,	SVDQ0246
	2 -1.13673942E-02,-9.35653660E-03,	SVDQ0247
	3 -7.89255401E-03/	SVDQ0248
C	GAS(I) GIVES THE I-TH ADAMS-MOULTON CORRECTOR	SVDQ0249
C	COEFFICIENT, I=1,2,...,KQMAX+1.	SVDQ0250
C		SVDQ0251
	DATA GAM/1.,.5,.416666667,.375,.348611111,.329861111,	SVDQ0252
	1 .315591931,.304224537,.294868000,.286975446,	SVDQ0253
	2 .5,.166666667,.125,.105555556,.9.375E-02,	SVDQ0254
	3 8.56150794E-02,7.95717593E-02,7.48522928E-02,	SVDQ0255
	4 7.10329861E-02,6.78584998E-02,	SVDQ0256
	5 .166666667,4.16666667E-02,2.91666667E-02,	SVDQ0257
	6 2.36111111E-02,2.03373016E-02,1.81299603E-02,	SVDQ0258
	7 1.65181327E-02,1.52772266E-02,1.42851882E-02,	SVDQ0259
	8 1.34693966E-02,	SVDQ0260
	9 4.16666667E-02,8.33333333E-03,5.55555556E-03,	SVDQ0261
	0 4.36507937E-03,3.67890212E-03,3.22365520E-03,	SVDQ0262
	1 2.89544753E-03,2.64543584E-03,2.44737491E-03,	SVDQ0263
	2 2.28579544E-03/	SVDQ0264
C	GAM(I,J) GIVES THE I-TH ADAMS-FALKNER PREDICTOR	SVDQ0265
C	COEFFICIENT FOR INTEGRATING J-TH ORDER DIFFERENTIAL	SVDQ0266
C	EQUATIONS, I=1,2,...,KQMAX+1, J=1,2,...,KMAX0.	SVDQ0267
C		SVDQ0268
	DIMENSION LTA(8,8)	SVDQ0269
	DATA (ETA(I, 1), I=1, 8)/ 3.33333330E-01, 2.50000000E-01,	SVDQ0270
	1 1.13636360E-01, 6.73076930E-02, 4.60526330E-02, 3.43749980E-02,	SVDQ0271
	2 2.71381590E-02, 2.22547310E-02/	SVDQ0272
	DATA (ETA(I, 2), I=1, 8)/ 2.00000000E-01, 4.00000000E-01,	SVDQ0273
	1 3.40209090E-01, 2.01923080E-01, 1.38157900E-01, 1.03124990E-01,	SVDQ0274
	2 8.14144780E-02, 6.67641930E-02/	SVDQ0275
	DATA (ETA(I, 3), I=1, 8)/ 1.42857140E-01, 2.85714280E-01,	SVDQ0276
	1 3.42857140E-01, 3.46153840E-01, 2.45614040E-01, 1.87500000E-01,	SVDQ0277
	2 1.50303650E-01, 1.24626490E-01/	SVDQ0278
	DATA (ETA(I, 4), I=1, 8)/ 1.11111110E-01, 2.22222220E-01,	SVDQ0279
	1 2.85714280E-01, 2.53968250E-01, 3.07017540E-01, 2.50000000E-01,	SVDQ0280
	2 2.08755060E-01, 1.78037850E-01/	SVDQ0281
	DATA (ETA(I, 5), I=1, 8)/ 9.09090910E-02, 1.81818180E-01,	SVDQ0282
	1 2.42424240E-01, 2.42424240E-01, 1.73160170E-01, 2.50000000E-01,	SVDQ0283
	2 2.27732800E-01, 2.05428290E-01/	SVDQ0284
	DATA (ETA(I, 6), I=1, 8)/ 7.69230760E-02, 1.53846150E-01,	SVDQ0285
	1 2.09790210E-01, 2.23776220E-01, 1.86480190E-01, 1.11888110E-01,	SVDQ0286
	2 1.91295550E-01, 1.91733070E-01/	SVDQ0287
	DATA (ETA(I, 7), I=1, 8)/ 6.66666660E-02, 1.33333330E-01,	SVDQ0288
	1 1.84615380E-01, 2.05128200E-01, 1.86480190E-01, 1.34265730E-01,	SVDQ0289
	2 6.96192690E-02, 1.39442230E-01/	SVDQ0290
	DATA (ETA(I, 8), I=1, 8)/ 5.88235290E-02, 1.17647060E-01,	SVDQ0291
	1 1.64705880E-01, 1.88235290E-01, 1.80995470E-01, 1.44796380E-01,	SVDQ0292
	2 9.21431500E-02, 4.21225830E-02/	SVDQ0293
C	ETA(I,J) I=1,2,...,J IS USED IN THE FIRST MODIFICATION OF THE	SVDQ0294
C	I-TH DIFFERENCE OF A J-TH ORDER METHOD AFTER THE STEPSIZE IS	SVDQ0295

C	HALVED.	SVDQ0296
C	ETA(1,J) J=1,2,....,I-1 IS USED IN THE SECOND MODIFICATION OF	SVDQ0297
C	THE (J+1)-ST DIFFERENCE OF AN I-TH ORDER METHOD.	SVDQ0298
C	THE TWO MODIFICATIONS OF THE DIFFERENCE TABLE AFTER HALVING THE	SVDQ0299
C	STEPSIZE REMOVES MOST OF THE INSTABILITY INHERENT IN THE METHOD	SVDQ0300
C	USED HERE FOR HALVING THE STEPSIZE.	SVDQ0301
C		SVDQ0302
C		SVDQ0303
C	IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE FOLLOWING CARD.	SVDQ0304
C	DATA LGSS,LGSD,LGSE/0,0,0/	SVDQ0305
C		SVDQ0306
C	*****	
C	THE STATEMENTS BETWEEN THE LINE ABOVE AND A SIMILAR LINE BELOW	
C	ARE INSERTED IN THE JPL VERSION OF THIS SUBROUTINE TO INSURE	
C	THAT THE CODE IS COMPILED CORRECTLY. THESE STATEMENTS THEMSELVES	
C	ARE NOT ACTUALLY COMPILED.	
C		
	NEQ=NEQ	
	HMINA=HMINA	
	HMAXA=HMAXA	
	DELT=DELT	
	TFINAL=TFINAL	
	MXSTEP=MXSTEP	
C	*****	
C		SVDQ0307
C	INITIALIZE	SVDQ0308
	KSTEP=-1	SVDQ0309
	NE=NEQ	SVDQ0310
	IF (NE.LE.0) GO TO 1190	SVDQ0311
	HH=H	SVDQ0312
	NV=0	SVDQ0313
	KDMAX=0	SVDQ0314
	KDD=KD(1)	SVDQ0315
	KDS=KDD	SVDQ0316
	DO 10 I=1,NE	SVDQ0317
	KQ(I)=1	SVDQ0318
	DT(1,I)=0.	SVDQ0319
	IF (KDS.LE.0) KDD=IABS(KD(1))	SVDQ0320
	IF ((KDD.EQ.0).OR.(KDD.GT.KMAX0)) HH=0.E0	SVDQ0321
	IF (KDD.GT.KDMAX) KDMAX=KDD	SVDQ0322
	10 NV=NV+KDD	SVDQ0323
C		SVDQ0324
	IF ((DELT*HH).LE.0.E0) GO TO 1190	SVDQ0325
	ERRMX=P1	SVDQ0326
	EMAX=ERND	SVDQ0327
	RNDC=RND*P25	SVDQ0328
	LDOUB=0	SVDQ0329
	E2HFAC=P25	SVDQ0330
	LSC=8	SVDQ0331
	LSTC=4	SVDQ0332
C	LSC AND LSTC ARE USED IN COMBINATION AS FOLLOWS	SVDQ0333
C	LSTC=4, LSC=4 FIRST TIME THROUGH THE FIRST STEP	SVDQ0334
C	LSTC=3, LSC=4 SECOND TIME THROUGH THE FIRST STEP	SVDQ0335
C	(NECESSARY TO CHECK STABILITY)	SVDQ0336
C	LSTC=2, LSC=4 THIRD TIME THROUGH THE FIRST STEP	SVDQ0337
C	(ONLY OCCURS IF INSTABILITY POSSIBLE)	SVDQ0338
C	LSTC=2, LSC=2 SECOND STEP (IF KQ(I)=2, I=1,....,NEQ)	SVDQ0339
C	LSTC=1, LSC=0 STARTING, ONE DERIVATIVE EVAL. PER STEP.	SVDQ0340
C	LSTC=1, LSC.GT.0 SET WHEN STARTING TWO DERIV. EVAL. PER STEP	SVDQ0341



C	LSTC=-1 LSC.LT.0 SET WHEN HALVING THE STEPSIZE	SVDQ0342
C	IN THE LAST TWO CASES LSC IS SET EQUAL TO LSTC*(MAXIMUM KQ(I)	SVDQ0343
C	+1). AT THE END OF EACH STEP IF LSC.NE.0 IT IS REPLACED BY	SVDQ0344
C	LSC-LSTC UNTIL LSC=0, AT WHICH TIME LSTC IS SET EQUAL TO 0.	SVDQ0345
C	WHEN DOUBLING H, LSTC IS SET EQUAL TO -1 AND LSC TO -3.	SVDQ0346
C	UNDER CERTAIN CONDITIONS WHEN KQ(I)=1, LSTC IS SET =-1 AND LSC=-5	SVDQ0347
C		SVDQ0348
	KSOUT=MXSTEP	SVDQ0349
	TOUT=T	SVDQ0350
	IFL=13	SVDQ0351
20	IFLAG=1	SVDQ0352
	GO TO 315	SVDQ0353
C	END OF INITIALIZATION	SVDQ0354
C		SVDQ0355
C		SVDQ0356
	ENTRY SVDQ1	SVDQ0357
C		SVDQ0358
C		SVDQ0359
C	TO OUTPUT VARIABLES IN THE CALLING SEQUENCE REMOVE THE C-S	SVDQ0360
C	IN COLUMN ONE OF THE FOLLOWING CARDS UNTIL REACHING THE COMMENT	SVDQ0361
C	END OF CODE FOR PRINTING VARIABLES IN CALLING SEQUENCE.	SVDQ0362
C	IF (NEQ.NE.0) GO TO 28	SVDQ0363
C	NEQ=1	SVDQ0364
C	22 WRITE(6,5000) T,DELT,HMINA,HMAXA,KEMAX,EMAX,IFLAG,TFINAL,MXSTEP	SVDQ0365
C5000	FORMAT(3H0T=1PE15.8,7H DELT=E12.5,8H HMINA=,E10.3,8H HMAXA=,	SVDQ0366
C	1 E10.3,8H KEMAX=,I2,7H EMAX=E10.3,8H IFLAG=,I2/	SVDQ0367
C	2 9H I KQ KD,7X,4HF(I),9X,1HJ,8X,4HY(J),13X,5HYN(J),	SVDQ0368
C	3 10X,7HTFINAL=1E15.8,9H MXSTEP=I4)	SVDQ0369
C	J=1	SVDQ0370
C	DO 24 I=1,NE	SVDQ0371
C	IF (KDS.LT.0) KDD=IABS(KD(I))	SVDQ0372
C	K=KDD	SVDQ0373
C	WRITE(6,5001) I,KQ(I),KDD,F(I),J,Y(J),YN(J)	SVDQ0374
C5001	FORMAT(1H ,I2,2I3,1PE17.8,I4,2E17.8)	SVDQ0375
C	23 J=J+1	SVDQ0376
C	K=K-1	SVDQ0377
C	IF (K.EQ.0) GO TO 24	SVDQ0378
C	WRITE(6,5002) J,Y(J),YN(J)	SVDQ0379
C5002	FORMAT(26X,I4,1P2E17.8)	SVDQ0380
C	GO TO 23	SVDQ0381
C	24 CONTINUE	SVDQ0382
C	WRITE(6,5003)	SVDQ0383
C5003	FORMAT(3H0 I,15X,16HDIFFERENCE TABLE)	SVDQ0384
C	DO 27 I=1,NE	SVDQ0385
C	KQQ=KQ(I)+1	SVDQ0386
C	K=MIN0(KQQ,7)	SVDQ0387
C	WRITE(6,5004) I,(DT(10,I),IO=1,K)	SVDQ0388
C5004	FORMAT(1H ,I2,1PE19.8,6E16.7)	SVDQ0389
C		SVDQ0390
C	IF (K.EQ.KQQ) GO TO 27	SVDQ0391
C	K=K+1	SVDQ0392
C	WRITE(6,5005) (DT(10,I),IO=K,KQQ)	SVDQ0393
C5005	FORMAT(1H ,1PE21.5,7E14.5)	SVDQ0394
C	27 CONTINUE	SVDQ0395
C	IF (NEQ.EQ.0) RETURN	SVDQ0396
C	NEQ=0	SVDQ0397
C	28 CONTINUE	SVDQ0398
C	END OF CODE FOR PRINTING VARIABLES IN CALLING SEQUENCE.	SVDQ0399
C		SVDQ0400

IF (2-IFL) 30,60,320	SVDQ0401
30 IF (IFL.GT.5) GO TO 1180	SVDQ0402
C	SVDQ0403
C SET STEP STOP	SVDQ0404
KSOOT=KSTEP+MXSTEP	SVDQ0405
IF (IFL-4) 40,1210,210	SVDQ0406
C	SVDQ0407
C	SVDQ0408
C SET PRINT STOP	SVDQ0409
40 TOUT=T+DELT	SVDQ0410
C	SVDQ0411
50 TPS1=ABS(AMOD((TOUT-TL)/HH,PTS2)-PTS1)	SVDQ0412
LFD=-1	SVDQ0413
IF (TPS1.GE.P5) LFD=1	SVDQ0414
C	SVDQ0415
C LFD IS USED TO INDICATE WHETHER DOUBLING H IS PERMITTED.	SVDQ0416
C IF LFD.LT.0 AT THE END OF A STEP THEN DOUBLING H IS	SVDQ0417
C NOT PERMITTED. THE SIGN OF LFD IS CHANGED JUST BEFORE THE	SVDQ0418
C END OF EACH STEP. IF DELT=H*(POWER OF 2) THEN	SVDQ0419
C OUTPUT VALUES WILL BE OBTAINED WITHOUT INTERPOLATION.	SVDQ0420
C	SVDQ0421
GO TO 200	SVDQ0422
C	SVDQ0423
C	SVDQ0424
C ENTRY WITH IFLAG=2	SVDQ0425
C	SVDQ0426
C UPDATE DIFFERENCE TABLE	SVDQ0427
C AND COMPUTE KQM=MAXIMUM VALUE OF KQ(I), I=1,2,...,NEQ.	SVDQ0428
C	SVDQ0429
60 KQM=0	SVDQ0430
DO 80 I=1,NE	SVDQ0431
KQQ=KQ(I)	SVDQ0432
IF (KQQ.GT.KQM) KQM=KQQ	SVDQ0433
D(1)=F(1)	SVDQ0434
DO 70 K=1,KQQ	SVDQ0435
D(K+1)=D(K)-DT(K,I)	SVDQ0436
70 DT(K,I)=D(K)	SVDQ0437
DT(KQQ+1,I)=D(KQQ+1)	SVDQ0438
80 CONTINUE	SVDQ0439
C END OF UPDATING DIFFERENCE TABLE	SVDQ0440
C	SVDQ0441
C STORE Y(J) IN YN(J)	SVDQ0442
DO 90 J=1,NV	SVDQ0443
90 YN(J)=Y(J)	SVDQ0444
C	SVDQ0445
LFD=-LFD	SVDQ0446
TL=T	SVDQ0447
KSTEP=KSTEP+1	SVDQ0448
C	SVDQ0449
C IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE 2 FOLLOWING CARDS.	SVDQ0450
IF (LGSS) 1430,110,1510	SVDQ0451
100 IFLAG=2	SVDQ0452
110 IF (LSC.EQ.0) GO TO 140	SVDQ0453
LSC=LSC-LSTC	SVDQ0454
IF (LSC.EQ.0) GO TO 130	SVDQ0455
IF (LSTC.NE.(-1)) GO TO 140	SVDQ0456
IF (LDOUB.LT.0) RND=C=RND*P1	SVDQ0457
120 E2HAVE=E2HMAX	SVDQ0458
TPS1=PTS1	SVDQ0459

GO TO 190	SVDQ0460
130 IF (ABS(HH).LT.HMINA) GO TO 1000	SVDQ0461
LSTC=0	SVDQ0462
140 IF (LDOUB.NE.1) GO TO 150	SVDQ0463
IF ((LFD.GT.0).AND.(ABS(HH+HH).LE.HMAXA)) GO TO 1030	SVDQ0464
GO TO 200	SVDQ0465
150 RQMAX=PTS1/FLOAT(KQM+3)	SVDQ0466
IF (LSTC.NE.0.OR.E2HAVE.EQ.0.E0) GO TO 120	FK
TPS1=E2HMAX/E2HAVE	SVDQ0468
IF (TPS1-PTS1) 160,190,170	SVDQ0469
160 E2HFAC=AMAX1(.075E0,E2HFAC-RQMAX,E2HFAC*TPS1)	SVDQ0470
GO TO 180	SVDQ0471
170 TPS1=TPS1*TPS1	SVDQ0472
E2HFAC=AMIN1(PTS1,E2HFAC*TPS1)	SVDQ0473
180 RNDC=(1.1-E2HFAC)*RND	SVDQ0474
E2HAVE=P5*(E2HMAX+E2HAVE)	SVDQ0475
190 ERRMX=AMAX1(P1,ERRMX-RQMAX*TPS1)	SVDQ0476
E2HFAC IS A FACTOR WHICH IS TAKEN TIMES AN INITIAL ESTIMATE OF	SVDQ0477
E2H TO GET A FINAL VALUE OF E2H. (E2H=ESTIMATE OF WHAT	SVDQ0478
(ESTIMATED ERROR)/(REQUESTED ERROR) WOULD BE IF H WERE	SVDQ0479
DOUBLED.)	SVDQ0480
E2HMAX IS THE MAXIMUM VALUE OF THE INITIAL ESTIMATE OF E2H OVER	SVDQ0481
ALL COMPONENTS WITH KQ(I).GT.1.	SVDQ0482
E2HAVE IS A WEIGHTED AVERAGE OF PAST VALUES OF E2HMAX.	SVDQ0483
THE VALUE OF E2HFAC TENDS TO BE SMALLER WHEN E2HMAX IS	SVDQ0484
CONSISTANTLY SMALLER THAN E2HAVE.	SVDQ0485
	SVDQ0486
	SVDQ0487
C CHECK FOR PRINT STOP AND FOR T REACHING TFINAL	SVDQ0488
200 TPD=(TOUT-TL)/HH	SVDQ0489
TPD1=(TFINAL-TL)/HH	SVDQ0490
	SVDQ0491
C IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE FOLLOWING CARD.	SVDQ0492
IF (LGSE.LT.0) GO TO 1780	SVDQ0493
IF (TPD1.LT.FAC(1)) GO TO 1220	SVDQ0494
IF (TPD.LE.0.E0) GO TO 1280	SVDQ0495
	SVDQ0496
C CHECK FOR STEP STOP	SVDQ0497
IF (KSOUT.GT.KSTEP) GO TO 210	SVDQ0498
	SVDQ0499
IFL=5	SVDQ0500
GO TO 310	SVDQ0501
	SVDQ0502
C CHECK TO SEE IF ROUND-OFF ERROR IS PROMINENT	SVDQ0503
210 IF (EMAX.EQ.ERND) GO TO 220	SVDQ0504
IT IS	SVDQ0505
IFL=6	SVDQ0506
IF (EMAX.GE.P1) GO TO 310	SVDQ0507
IF ((LSTC.GE.0).OR.(LDOUB.EQ.1)) ERRMX=PTS1	SVDQ0508
	SVDQ0509
220 IFL=1	SVDQ0510
230 T=TL+HH	SVDQ0511
	SVDQ0512
C START A NEW STEP	SVDQ0513
	SVDQ0514
C PREDICT	SVDQ0515
240 J=0	SVDQ0516
DO 290 I=1,NE	SVDQ0517
IF (KDS.LE.0) KDD=IABS(KD(I))	SVDQ0518

	KDC=KDD	SVDQ0519
250	KQQ=KQ(I)	SVDQ0520
	TPD=0.EU	SVDQ0521
	K=KDC	SVDQ0522
260	TPD=TPD+DT(KQQ,I)*GAM(KQQ,KDC)	SVDQ0523
	KQQ=KQQ-1	SVDQ0524
	IF (KQQ.GT.0) GO TO 260	SVDQ0525
270	K=K-1	SVDQ0526
	IF (K.LE.0) GO TO 280	SVDQ0527
	L=J+K	SVDQ0528
	TPD=YN(L+1)*FAC(K)+HH*TPD	SVDQ0529
	GO TO 270	SVDQ0530
280	J=J+1	SVDQ0531
	Y(J)=YN(J)+HH*TPD	SVDQ0532
	KDC=KDC-1	SVDQ0533
	IF (KDC.GT.0) GO TO 250	SVDQ0534
290	CONTINUE	SVDQ0535
C	END OF PREDICT	SVDQ0536
C		SVDQ0537
C	IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE C IN COLUMN ONE	SVDQ0538
C	OF THE 2 FOLLOWING CARDS	SVDQ0539
C	IF (IFL) 20,320,300	SVDQ0540
C	300 CONTINUE	SVDQ0541
C	AND THEN REMOVE THE 2 FOLLOWING CARDS.	SVDQ0542
	IF (IFL) 1240,320,300	SVDQ0543
300	IF (LGSD.NE.0) GO TO 1520	SVDQ0544
C		SVDQ0545
310	IFLAG=IFL	SVDQ0546
315	CONTINUE	SVDQ0547
C		SVDQ0548
C	TO OUTPUT VARIABLES IN THE CALLING SEQUENCE REMOVE THE C IN	SVDQ0549
C	COLUMN ONE OF THE FOLLOWING CARD.	SVDQ0550
C	IF (NEQ.EQ.0) GO TO 22	SVDQ0551
C		SVDQ0552
C	RETURN	SVDQ0553
C		SVDQ0554
C		SVDQ0555
C	ENTRY WITH IFLAG=1	SVDQ0556
320	EPS=EP(1)	SVDQ0557
	ERND=0.	SVDQ0558
	EMAX=0.	SVDQ0559
	E2HMAX=0.	SVDQ0560
	J=0	SVDQ0561
	IF (LDOUB.GE.0) LDOUB=1	SVDQ0562
C		SVDQ0563
C	LDOUB IS SET IN THE LOOP BELOW AS FOLLOWS	SVDQ0564
C	LDOUB=0 HALVE	SVDQ0565
C	LDOUB=1 DOUBLE	SVDQ0566
C	LDOUB=2 DO NOT DOUBLE	SVDQ0567
C		SVDQ0568
C	LDOUB,LT.0 AT THE BEGINNING OF THE LOOP INDICATES THE FOLLOWING	SVDQ0569
C	--3 STEPSIZE HAS JUST BEEN HALVED. IF A DISCONTINUITY IS	SVDQ0570
C	NOT INDICATED MODIFY THE DIFFERENCE TABLE AND REPEAT	SVDQ0571
C	THE STEP.	SVDQ0572
C	--2 STEP AFTER LDOUB=-3. PROCEED AS USUAL (ORDER IS NOT	SVDQ0573
C	CHANGED)	SVDQ0574
C	--1 STEP AFTER LDOUB=-2. MODIFY THE DIFFERENCE TABLE ONCE	SVDQ0575
C	AGAIN AND REPEAT THE STEP.	SVDQ0576
C	IF LDOUB IS SET EQUAL TO -4 THE ORDER IN AT LEAST ONE COMPONENT	SVDQ0577



C	HAS BEEN GREATLY REDUCED AND THE STEP IS REPEATED.	SVDQ0578
C		SVDQ0579
C		SVDQ0580
C	IF THE OUTPUT OPTION IS ELIMINATED, REMOVE THE 4 FOLLOWING CARDS.	SVDQ0581
	IF (NEQ.LE.0) WRITE (6,5020) LSC,LFD,LSTC,KSTEP,E2HFAC,ERRMX,HH	SVDQ0582
5020	FORMAT (19H0 1 KQQ LRND LDOUB,5X,1HE,9X,3HE2H,	SVDQ0583
	1 8X,3HEPS,3X,4HLSC=,I3,6H LFD=,I2,7H LSTC=,I2,8H KSTEP=,I4,	SVDQ0584
	2 9H E2HFAC=,F4.2,8H ERRMX=,F4.2,4H H=,1PE9.2)	SVDQ0585
C		SVDQ0586
C		SVDQ0587
C	BEGINNING OF LOOP FOR CORRECTING, ESTIMATING THE ERROR,	SVDQ0588
C	AND ADJUSTING THE NUMBER OF DIFFERENCES USED	SVDQ0589
C		SVDQ0590
	DO 790 I=1,NE	SVDQ0591
	IF (KDS.LE.0) KDD=IABS(KD(I))	SVDQ0592
	KQQ=KQ(I)	SVDQ0593
C	KQQ GIVES THE ORDER OF THE PREDICTOR FORMULA AND KQQ+1 THE	SVDQ0594
C	ORDER OF THE CORRECTOR FORMULA.	SVDQ0595
C		SVDQ0596
	KQ1=KQQ+1	SVDQ0597
	D(1)=F(1)	SVDQ0598
C	FORM THE DIFFERENCE TABLE FROM PREDICTED DERIVATIVE VALUES.	SVDQ0599
	DO 330 K=1,KQ1	SVDQ0600
	D(K+1)=D(K)-DT(K,I)	SVDQ0601
330	CONTINUE	SVDQ0602
C	D(K) GIVES THE (K-1)-ST DIFFERENCE FORMED FROM PREDICTED	SVDQ0603
C	DERIVATIVE VALUES	SVDQ0604
	TPS3=ABS(D(KQQ+1))	SVDQ0605
	IF (LDOUB.LT.0) GO TO 720	SVDQ0606
C		SVDQ0607
340	IF (KQQ.NE.1) GO TO 520	SVDQ0608
C		SVDQ0609
C	KQ(I)=1 IS TREATED AS A SPECIAL CASE	SVDQ0610
	E2H=PTS2	SVDQ0611
	TPS5=DT(3,I)	SVDQ0612
	IF (LSTC.LT.2) GO TO 370	SVDQ0613
C	FIRST STEP OF INTEGRATION	SVDQ0614
	IF (LSTC.NE.4) GO TO 350	SVDQ0615
	TPS4=0.	SVDQ0616
	IF (KDD.GT.1) TPS3=AMAX1(TPS3,ABS(HH*D(1)))	SVDQ0617
	TPS3=TPS3*P1	SVDQ0618
350	DT(2,I)=D(2)	SVDQ0620
	D(2)=D(1)-DT(5,I)	SVDQ0621
	TPS2=-D(2)	SVDQ0622
	TPS3=PTS5*ABS(TPS2)	SVDQ0623
C	FIRST STEP THAT KQ(I)=1	SVDQ0624
360	DT(7,I)=PT(4)	SVDQ0625
	IF (LSTC-2) 420,380,380	SVDQ0626
370	IF (TPS5.EQ.0.) GO TO 360	SVDQ0627
	IF (DT(6,I).EQ.0.) GO TO 400	SVDQ0628
	TPS2=DT(5,I)-DT(1,I)	SVDQ0629
380	TPS4=DT(4,I)	SVDQ0630
	TPS1=ABS(TPS4)	SVDQ0631
	TPS4=TPS2*SIGN(PTS2,TPS4)-TPS5*TPS1	SVDQ0632
	IF (TPS4.GT.(-TPS1)) GO TO 410	SVDQ0633
390	TPS6=-PTS1	SVDQ0634
	GO TO 450	SVDQ0635
C	FIRST STEP AFTER THE STEPSIZE HAS BEEN CHANGED	SVDQ0636
400	DT(6,I)=PT(1)	SVDQ0637



	TPS6=0.	SVDQ0638
	GO TO 450	SVDQ0639
410	IF (TPS4.LT.TPS1) GO TO 440	SVDQ0640
	IF (TPS1.EQ.0.) GO TO 390	SVDQ0641
420	TPS6=PTS1	SVDQ0642
	GO TO 450	SVDQ0643
430	KQ(I)=2	SVDQ0644
	IF (2-LSTC) 510,510,520	SVDQ0645
440	TPS6=TPS4/TPS1	SVDQ0646
450	TPS4=TPS5+TPS6	SVDQ0647
	IF (TPS4.LT.P25) GO TO 430	SVDQ0648
C	INCREASE E2H IF (-S).GT..25	SVDQ0649
	E2H=PTS4*TPS4	SVDQ0650
	IF (2-LSTC) 460,470,480	SVDQ0651
460	LSC=0	SVDQ0652
	GO TO 510	SVDQ0653
470	IF (TPS5-P25) 430,460,460	SVDQ0654
480	IF (TPS4.GT.PTS2) GO TO 490	SVDQ0655
	IF (TPS4.GT.P5) D(2)=D(2)*GAM(2,1)	SVDQ0656
	GO TO 510	SVDQ0657
490	IF (TPS4.LT.PTS4) GO TO 500	SVDQ0658
	TPS4=PTS4	SVDQ0659
	D(2)=D(2)/PT(3)	SVDQ0660
C	THE ESTIMATE OF E (AND HENCE OF E2H) IS INCREASED IF (-S).GE.8.	SVDQ0661
	TPS3=TPS3*DT(7,1)	SVDQ0662
	GO TO 510	SVDQ0663
500	D(2)=D(2)*PTS2*(TPS4-PTS1)/(TPS4*TPS4)	SVDQ0664
	IF (TPS4.GE.P3E1) E2H=E2H*DT(7,1)	SVDQ0665
C	STORE D(1)=PREDICTED DERIVATIVE AND D(2)=2*(CORRECTED Y -	SVDQ0666
C	PREDICTED Y)/H D(1) AND D(2) ARE USED TO COMPUTE (-S) ON	SVDQ0667
C	THE NEXT STEP.	SVDQ0668
510	DT(5,1)=D(1)	SVDQ0669
	DT(4,1)=D(2)	SVDQ0670
	D(4)=TPS4	SVDQ0671
C	STORE D(4)= CURRENT ESTIMATE OF (-S). (-S).CT.3 IS AN INDICATION	SVDQ0672
C	THAT THE STEPSIZE SHOULD BE LIMITED BECAUSE OF STABILITY PROBLEMS.	SVDQ0673
C	S=H*(ESTIMATE OF EIGENVALUE OF F)=H*(DIFFERENCE BETWEEN PREDICTED	SVDQ0674
C	AND CORRECTED DERIVATIVE VALUES)/(DIFFERENCE BETWEEN PREDICTED	SVDQ0675
C	AND CORRECTED INTEGRALS OF THE DERIVATIVE VALUES)	SVDQ0676
C	THE TREATMENT OF THE CASE KQ(I)=1 COULD BE IMPROVED BY USING A	SVDQ0677
C	SPECIAL METHOD FOR STIFF EQUATIONS WHEN (-S).GT.3 (MAYBE).	SVDQ0678
C	(THE ENTIRE TREATMENT OF THE CASE KQ(I)=1 IS FAR FROM IDEAL.)	SVDQ0679
	DT(3,1)=D(4)	SVDQ0680
C		SVDQ0681
C	CORRECT	SVDQ0682
520	KDC=0	SVDQ0683
	TPD=D(KQ1)	SVDQ0684
	J=J+KDD	SVDQ0685
	K=J	SVDQ0686
530	TPD=HH*TPD	SVDQ0687
	KDC=KDC+1	SVDQ0688
	Y(K)=Y(K)+GAM(KQQ+1,KDC)*TPD	SVDQ0689
	K=K-1	SVDQ0690
	IF (KDC.LT.KDD) GO TO 530	SVDQ0691
C	END OF CORRECT	SVDQ0692
C		SVDQ0693
	IF (LPS) 540,550,560	SVDQ0694
540	EPS=EP(1)	SVDQ0695
	IF (EPS.NE.0.) GO TO 560	SVDQ0696

550	IF (HMAXA) 1190,780,1190	SVDQ0697
560	TPS4=ABS(D(KQQ+2))	SVDQ0698
	TPS2=ABS(D(KQQ))	SVDQ0699
	TPS6=HH/EPS	SVDQ0700
C		SVDQ0701
	E=ABS(GAS(KQQ+1)*TPS3*TPS6)	SVDQ0702
C	E GIVES ABS((ESTIMATED ERROR)/EPS)	SVDQ0703
C		SVDQ0704
	LRND=1	SVDQ0705
C		SVDQ0706
C	LRND= 1 MEANS NO ROUND-OFF ERROR	SVDQ0707
C	= 0 MEANS SOME ROUND-OFF ERROR	SVDQ0708
C	=-1 MEANS EXTREME ROUND-OFF ERROR	SVDQ0709
C		SVDQ0710
	FRND=PT(KQQ+2)*RNDC*ABS(D(1))	SVDQ0711
C	CHECK TO SEE IF ROUND OFF ERROR IS DOMINANT	SVDQ0712
	IF ((TPS3+TPS4).GT.FRND) GO TO 570	SVDQ0713
	LRND=0	SVDQ0714
	IF ((PTS4*TPS2).LT.FRND) LRND=-1	SVDQ0715
C		SVDQ0716
570	IF (E.LE.ERND) GO TO 590	SVDQ0717
	IF (E.LE.EMAX) GO TO 580	SVDQ0718
	EMAX=E	SVDQ0719
	KEMAX=1	SVDQ0720
580	IF (LRND.LE.0) GO TO 590	SVDQ0721
	ERND=E	SVDQ0722
	IF (ERND.GT.ERRMX) LDOUB=0	SVDQ0723
590	IF (LDOUB.LE.0) GO TO 780	SVDQ0724
	TPS1=ABS(D(KQQ))	SVDQ0725
	TPS5=TPS1	SVDQ0726
	IF (KQQ-2) 600,610,620	SVDQ0727
600	E2H=E*E2H	SVDQ0728
	IF (E2H.LT.P01) GO TO 780	SVDQ0729
	IF (D(4).LT.P3E1) GO TO 770	SVDQ0730
	LSTC=-1	SVDQ0731
	LSC=-5	SVDQ0732
	GO TO 770	SVDQ0733
610	TPS1=TPS2	SVDQ0734
	IF (LSTC.NE.2) GO TO 620	SVDQ0735
	KQ(1)=3	SVDQ0736
	TPS2=0.	SVDQ0737
	TPS4=0.	SVDQ0738
	LRND=0	SVDQ0739
620	E2H=TPS2+TPS3+TPS4	SVDQ0740
	E2H=ABS(GAS(KQQ-1)*PT(KQQ+1)*E2H*TPS6)	SVDQ0741
C	E2H IS USED AS AN ESTIMATE OF WHAT THE VALUE OF E WOULD BE	SVDQ0742
C	IF H WERE DOUBLED. THE ESTIMATE IS CONSERVATIVELY LARGE.	SVDQ0743
	IF (E2H.GT.E2HMAX) E2HMAX=E2H	SVDQ0744
C		SVDQ0745
	IF (LRND) 630,640,660	SVDQ0746
C	EXTREME ROUND-OFF ERROR--REDUCE E2H	SVDQ0747
630	K=(KBIT2/KQQ)-4	SVDQ0748
	IF (K.LE.3) GO TO 640	SVDQ0749
	IF (K.GT.KQMAX) K=KQMAX	SVDQ0750
	E2H=E2H/PT(K+1)	SVDQ0751
	GO TO 650	SVDQ0752
640	E2H=AMIN1(E2H,E2H*P3E1*E2HFAC)	SVDQ0753
650	E2H=E2H*P1	SVDQ0754
	TPS6=PTS4	SVDQ0755

	GO TO 670	SVDQ0756
C		SVDQ0757
660	E2H=E2H*E2HFAC	SVDQ0758
	TPS6=FLOAT(KQQ+2)	SVDQ0759
C	TEST TO SEE IF DIFFERENCES DECREASE MORE RAPIDLY THAN NECESSARY	SVDQ0760
C		SVDQ0761
670	IF (TPS5.LT.(TPS3*TPS6)) GO TO 680	SVDQ0762
	IF (TPS2.LE.(TPS4*TPS6)) GO TO 760	SVDQ0763
C	THEY DO INCREASE KQ(I)	SVDQ0764
	IF (KQQ.NE.KQMAX) KQ(I)=KQ1	SVDQ0765
	GO TO 760	SVDQ0766
C		SVDQ0767
C	TEST TO SEE IF DIFFERENCES DECREASE TOO SLOWLY	SVDQ0768
680	TPS6=TPS6*P25	SVDQ0769
	IF ((TPS1.GT.(TPS3*TPS6)).OR.(TPS2.GT.(TPS4*TPS6))) GO TO 760	SVDQ0770
C	THEY DO	SVDQ0771
	IF (LSTC.LE.0) GO TO 750	SVDQ0772
	IF (E2H.LT.P01) GO TO 750	SVDQ0773
	IF (LSC-LSTC) 690,750,770	SVDQ0774
690	IF (KSTEP-4) 750,700,710	SVDQ0775
700	KQ1=LSTC	SVDQ0776
710	LSC=KQ1	SVDQ0777
C	END OF ONE DERIVATIVE EVALUATION PER STEP	SVDQ0778
	GO TO 770	SVDQ0779
C		SVDQ0780
C	AFTER HALVING H. REDUCE KQ(I) IF A DISCONTINUITY HAS OCCURRED.	SVDQ0781
720	IF (LDOUB.EQ.(-2)) GO TO 340	SVDQ0782
	DT(KQQ+1,I)=D(KQQ+1)	SVDQ0783
	IF (LDOUB.EQ.(-1)) DT(KQQ+1,I)=D(KQQ+2)	SVDQ0784
	K=KQQ	SVDQ0785
730	IF (K.EQ.1) GO TO 740	SVDQ0786
	IF ((ABS(D(K-1)).GT.(PT(2)*ABS(D(K+1))))).OR.	SVDQ0787
1	(ABS(D(K)).GT.(PT(2)*ABS(D(K+2)))) GO TO 740	SVDQ0788
	K=K-1	SVDQ0789
	GO TO 730	SVDQ0790
740	IF ((K+K).GE.KQQ) GO TO 780	SVDQ0791
	LDOUB=-4	SVDQ0792
	E2H=0.	SVDQ0793
	KQQ=K+1	SVDQ0794
C		SVDQ0795
C		SVDQ0796
C	DIFFERENCES DECREASE TOO SLOWLY REDUCE KQ(I).	SVDQ0797
750	KQ(I)=KQQ-1	SVDQ0798
	IF (KQQ.EQ.2) DT(3,I)=0.	SVDQ0799
760	IF (E2H.LT.P01) GO TO 780	SVDQ0800
770	LDOUB=2	SVDQ0801
780	CONTINUE	SVDQ0802
C		SVDQ0803
C	IF THE OUTPUT OPTION IS ELIMINATED, REMOVE THE 6 FOLLOWING CARDS.	SVDQ0804
	IF (NEQ.GT.0) GO TO 790	SVDQ0805
	IO2=MAX0(1,(KQQ-1))	SVDQ0806
	IO3=IO2+3	SVDQ0807
	WRITE (6,5021) I,KQQ,LRND,LDOUB,E,E2H,EPS,	SVDQ0808
1	(IO1,D(IO1),IO1=IO2,IO3)	SVDQ0809
5021	FORMAT (1H I2,I4,2I5,1PE13.3,2E11.3,4(3H (,I2,1H),E10.3))	SVDQ0810
C		SVDQ0811
790	CONTINUE	SVDQ0812
C		SVDQ0813
C	END OF LOOP FOR CORRECTING, ESTIMATING THE ERROR, ETC.	SVDQ0814

C		SVDQ0815
C		SVDQ0816
C	IF THE INTERPOLATION CAPABILITY IS ELIMINATED REMOVE THE	SVDQ0817
C	FOLLOWING CARD.	SVDQ0818
	IF (IFL.LT.0) GO TO 1250	SVDQ0819
C	TEST FOR HALVING H	SVDQ0820
	IF (LDOUB) 800,950,870	SVDQ0821
800	LDOUB=LDOUB+1	SVDQ0822
	IF (LDOUB+1) 810,870,820	SVDQ0823
810	IF (LDOUB.EQ.(-2)) GO TO 820	SVDQ0824
C	ORDER IN AT LEAST ONE COMPONENT HAS BEEN GREATLY REDUCED	SVDQ0825
	LDOUB=0	SVDQ0826
	GO TO 220	SVDQ0827
820	DO 860 I=1,NE	SVDQ0828
	KQQ=KG(I)	SVDQ0829
	TP=DT(KQQ+1,I)	SVDQ0830
	IF (KQQ.LE.3) GO TO 860	SVDQ0831
	IF (LDOUB.NE.0) GO TO 840	SVDQ0832
	DO 830 K=3,KQQ	SVDQ0833
C	SECOND MODIFICATION OF DIFFERENCE TABLE AFTER HALVING H	SVDQ0834
830	DT(K,I)=DT(K,I)+ETA(KQQ-1,K-2)*TP	SVDQ0835
	GO TO 860	SVDQ0836
840	DO 850 K=2,KQQ	SVDQ0837
C	FIRST MODIFICATION OF DIFFERENCE TABLE AFTER HALVING H	SVDQ0838
850	DT(K,I)=DT(K,I)+ETA(K-1,KQQ-1)*TP	SVDQ0839
860	CONTINUE	SVDQ0840
	IFL=0	SVDQ0841
	GO TO 240	SVDQ0842
C		SVDQ0843
870	IFL=2	SVDQ0844
	IF (LSTC.LE.0) GO TO 300	SVDQ0845
	IF (2-LSTC) 880,900,940	SVDQ0846
880	LSTC=LSTC-1	SVDQ0847
	IF (LSTC.EQ.3) GO TO 890	SVDQ0848
	IF (LSC) 920,960,920	SVDQ0849
890	IFL=1	SVDQ0850
	GO TO 300	SVDQ0851
900	IF (LSC-2) 910,930,920	SVDQ0852
910	LSTC=0	SVDQ0853
920	LDOUB=2	SVDQ0854
	GO TO 60	SVDQ0855
930	LSTC=1	SVDQ0856
	LSC=0	SVDQ0857
	GO TO 60	SVDQ0858
940	IF (LSC) 300,60,300	SVDQ0859
C		SVDQ0860
C	HALVE H	SVDQ0861
950	HH=FAC(2)*HH	SVDQ0862
	IF (LSTC.LT.2) GO TO 990	SVDQ0863
	ERND=P25*ERND	SVDQ0864
C	IN LOOP TO FIND A NEW INITIAL STEPSIZE	SVDQ0865
	IF (ERND.GE.P1) GO TO 950	SVDQ0866
	EMAX = ERND	
	LSTC=4	SVDQ0867
960	LSC=4	SVDQ0868
	DO 970 I=1,NE	SVDQ0869
970	KQ(I)=1	SVDQ0870
	IF (LSTC-3) 890,890,1170	SVDQ0871
C		SVDQ0872



C	ENTRY AFTER IFLAG=7	SVDQ0873
980	IF (LDOUB.EQ.0) GO TO 990	SVDQ0874
	LSC=1	SVDQ0875
	LSTC=1	SVDQ0876
	GO TO 140	SVDQ0877
C	TEST TO SEE IF H IS TOO SMALL FOR HALVING	SVDQ0878
990	IF (ABS(HH).GE.HMINA) GO TO 1040	SVDQ0879
	IF (IFL.EQ.7) GO TO 1010	SVDQ0880
1000	IFL=7	SVDQ0881
	GO TO 1020	SVDQ0882
C		SVDQ0883
1010	HH=HH+HH	SVDQ0884
	IFL=2	SVDQ0885
1020	H=HH	SVDQ0886
	GO TO 310	SVDQ0887
C		SVDQ0888
C		SVDQ0889
C	ERROR CRITERIA PERMIT DOUBLING	SVDQ0890
1030	HH=HH+HH	SVDQ0891
	IF (LSTC.EQ.1) GO TO 1050	SVDQ0892
	LSC=-3	SVDQ0893
1040	LSTC=-1	SVDQ0894
C		SVDQ0895
C	CHANGE THE STEPSIZE	SVDQ0896
1050	DO 1160 I=1,NE	SVDQ0897
	KQQ=KQ(I)	SVDQ0898
	IF (KQQ.NE.1) GO TO 1070	SVDQ0899
	DT(6,I)=0.	SVDQ0900
	D(3)=DT(3,I)*PT(2)	SVDQ0901
	IF (D(3).GT.PT(3)) LSC=-6	SVDQ0902
	IF (LDOUB.NE.0) GO TO 1060	SVDQ0903
	KQM=8	SVDQ0904
	IF (D(3).GE.PT(5)) DT(7,I)=DT(7,I)*PT(2)	SVDQ0905
	D(3)=D(3)/PT(3)	SVDQ0906
1060	DT(3,I)=D(3)	SVDQ0907
	GO TO 1160	SVDQ0908
C		SVDQ0909
C	BEGINNING OF LOOP FOR CHANGING DIFFERENCE TABLE TO	SVDQ0910
C	CORRESPOND TO NEW VALUE OF H	SVDQ0911
1070	DO 1080 K=1,KQQ	SVDQ0912
	D(K)=DT(K,I)/PT(K)	SVDQ0913
1080	IF (LDOUB.EQ.0) D(K)=D(K)/PT(K)	SVDQ0914
	KQQ2=KQQ-2	SVDQ0915
	IF (KQQ2) 1160,1140,1090	SVDQ0916
1090	DO 1130 J=1,KQQ2	SVDQ0917
	IF (LDOUB.NE.0) GO TO 1110	SVDQ0918
C		SVDQ0919
C	HALVE	SVDQ0920
	K=KQQ	SVDQ0921
1100	D(K-1)=D(K-1)+D(K)	SVDQ0922
	K=K-1	SVDQ0923
	IF (K+J-KQQ) 1130,1130,1100	SVDQ0924
C		SVDQ0925
C	DOUBLE	SVDQ0926
1110	DO 1120 K=J,KQQ2	SVDQ0927
1120	D(K+1)=D(K+1)-D(K+2)	SVDQ0928
1130	CONTINUE	SVDQ0929
C		SVDQ0930
1140	DO 1150 K=2,KQQ	SVDQ0931



IF (LDOUB.NE.0) D(K)=D(K)*PT(K)	SVDQ0932
DT(K,I)=D(K)*PT(K)	SVDQ0933
1150 CONTINUE	SVDQ0934
C DIFFERENCE TABLE NOW CORRESPONDS TO NEW VALUE OF H	SVDQ0935
C	SVDQ0936
1160 CONTINUE	SVDQ0937
1170 H=HH	SVDQ0938
IF (LDOUB.NE.0) GO TO 50	SVDQ0939
LFD=1	SVDQ0940
IF (LSTC.GE.0) GO TO 220	SVDQ0941
LDOUB=-3	SVDQ0942
LSC=LSTC-KQM	SVDQ0943
GO TO 220	SVDQ0944
C END OF CHANGING STEPSIZE	SVDQ0945
C	SVDQ0946
C	SVDQ0947
C IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE C IN COLUMN ONE	SVDQ0948
C OF THE 2 FOLLOWING CARDS	SVDQ0949
C1180 IF (7-IFL) 1181,980,220	SVDQ0950
C1181 IF (IFL-8) 60,1200,60	SVDQ0951
C AND THEN REMOVE THE 2 FOLLOWING CARDS.	SVDQ0952
1180 K=IFL-5	SVDQ0953
GO TO (220,980,1200,1570,1570,1720,1720,60,1480,1450,1630,1570), K	SVDQ0954
C	SVDQ0955
C ILLEGAL VALUE OF PARAMETER INTEGRATION CAN NOT PROCEED	SVDQ0956
1190 IFL=8	SVDQ0957
GO TO 310	SVDQ0958
1200 WRITE (6,4000)	SVDQ0959
4000 FORMAT (26H0IFLAG=8 IN CALL TO DVDQ1.)	SVDQ0960
STOP	SVDQ0961
C	SVDQ0962
C	SVDQ0963
1210 IF (T-TFINAL) 200,1190,200	SVDQ0964
C	SVDQ0965
C IF ONE DOES NOT WANT THE INTERPOLATION FEATURE, REMOVE ALL CARDS	SVDQ0966
C BELOW THIS POINT (EXCLPT FOR THE END STATEMENT), AND ADD THE	SVDQ0967
C FIVE FOLLOWING STATEMENTS.	SVDQ0968
C1220 IFL=4	SVDQ0969
C IF (TPD1.GT.TPD) GO TO 1280	SVDQ0970
C GO TO 310	SVDQ0971
C1280 IFL=3	SVDQ0972
C GO TO 310	SVDQ0973
C	SVDQ0974
1220 IFL=4	SVDQ0975
IF (KSTEP.NE.0) GO TO 1270	SVDQ0976
TPD2=TPD	SVDQ0977
C ESTIMATE ERROR WHEN EXTRAPOLATION FROM INITIAL POINT IS REQUESTED	SVDQ0978
1230 HH=HH*TPD1*.75E0	SVDQ0979
C	SVDQ0980
C IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE FOLLOWING CARD.	SVDQ0981
IFLS=IFL	SVDQ0982
IFL=-1	SVDQ0983
GO TO 230	SVDQ0984
C	SVDQ0985
C IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE 4 FOLLOWING CARDS.	SVDQ0986
1240 IF ((LGSD.EQ.0).OR.(IFLS.NE.4)) GO TO 20	SVDQ0987
LGSE=-1	SVDQ0988
TPD=FAC(1)	SVDQ0989
GO TO 1820	SVDQ0990

1250	HH=H	SVDQ0991
	IF (EMAX.LT.P01) GO TO 1260	SVDQ0992
C	ERROR IS TOO LARGE, REDUCE H AND REPEAT THE FIRST STEP	SVDQ0993
	IF (TPD1.LT.C.E0) GO TO 1190	SVDQ0994
	LDOUB=1	
	ERND=FAC(1)/TPD1	
	ERND=ERND*ERND*P25	
C	SET IFLAG SO INTERPOLATION IS DONE	
	IFLAG = 3	
	GO TO 950	SVDQ0998
C		SVDQ0999
C	IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE C IN COLUMN ONE	SVDQ1000
C	OF THE FOLLOWING CARD	SVDQ1001
C1260	IFL=4	SVDQ1002
C	AND THEN REMOVE THE 2 FOLLOWING CARDS.	SVDQ1003
1260	IFL=IFLS	SVDQ1004
	IF (IFL.NE.4) GO TO 1790	SVDQ1005
	TPD=TPD2	SVDQ1006
	IFLAG=3	SVDQ1007
1270	IF (TPD1.GT.TPD) GO TO 1280	SVDQ1008
	T=TFINAL	SVDQ1009
	TPD=TPD1	SVDQ1010
	GO TO 1290	SVDQ1011
1280	T=TOUT	SVDQ1012
	IFL=3	SVDQ1013
1290	IF ((TPD.EQ.C.E0).AND.(IFLAG.LE.2)) GO TO 310	SVDQ1014
C		SVDQ1015
C	INTERPOLATE FOR OUTPUT	SVDQ1016
1300	TP=TPD	SVDQ1017
	D(2)=TP	SVDQ1018
	KQQ2=0	SVDQ1019
	KDC=0	SVDQ1020
	D(1)=PT(1)	SVDQ1021
	DD(1)=PT(1)	SVDQ1022
	DO 1310 K=2,KQM	SVDQ1023
	DD(1)=DD(1)+PT(1)	SVDQ1024
	TP=TP+PT(1)	SVDQ1025
1310	D(K+1)=(D(K)*TP)/DD(1)	SVDQ1026
	GO TO 1350	SVDQ1027
C		SVDQ1028
C	COMPUTE THE INTERPOLATING INTEGRATION COEFFICIENTS	SVDQ1029
1320	KQQ2=1	SVDQ1030
	L=KQM-KDC	SVDQ1031
	KDC=KDC+1	SVDQ1032
1330	IF (L.LE.0) GO TO 1350	SVDQ1033
	TP=0.	SVDQ1034
	K=L	SVDQ1035
	J=L+KDC	SVDQ1036
1340	JS=J-K	SVDQ1037
	TP=TP+GAS(K)*D(JS+1)	SVDQ1038
	K=K-1	SVDQ1039
	IF (K.GT.0) GO TO 1340	SVDQ1040
	D(J)=TP	SVDQ1041
C		SVDQ1042
C	D(J) IS THE INTEGRATION COEFFICIENT FOR THE INTERPOLATION WHICH	SVDQ1043
C	CORRESPONDS TO GAM(J-KDC,KDC).	SVDQ1044
C		SVDQ1045
	L=L-1	SVDQ1046
	GO TO 1330	SVDQ1047

C	END OF COMPUTING INTEGRATION COEFFICIENTS	SVDQ1048
C		SVDQ1049
C	PERFORM THE PARTIAL STEP INTEGRATION	SVDQ1050
1350	J=0	SVDQ1051
	DO 1420 I=1,NE	SVDQ1052
	IF (KDS.LE.0) KDD=IABS(KD(I))	SVDQ1053
	IF (KDC.GT.KDD) GO TO 1410	SVDQ1054
	TP=0.	SVDQ1055
	KQQ=KQ(I)+KQQ2	SVDQ1056
1360	L=KQQ-KDC	SVDQ1057
	IF (L.LE.0) GO TO 1370	SVDQ1058
	TP=TP+D(KQQ)*DT(L,I)	SVDQ1059
	KQQ=KQQ-1	SVDQ1060
	IF (KQQ) 1390,1390,1360	SVDQ1061
1370	K=J+KDD	SVDQ1062
	L=KDC	SVDQ1063
1380	L=L-1	SVDQ1064
	IF (L.EQ.0) GO TO 1400	SVDQ1065
	TP=TP*HH+YN(K)*FAC(L)*TPD**L	SVDQ1066
	K=K-1	SVDQ1067
	GO TO 1380	SVDQ1068
1390	F(I)=TP	SVDQ1069
	GO TO 1420	SVDQ1070
1400	Y(K)=YN(K)+HH*TP	SVDQ1071
1410	J=J+KDD	SVDQ1072
1420	CONTINUE	SVDQ1073
	IF (KDC.NE.KDMAX) GO TO 1320	SVDQ1074
C	END OF PARTIAL STEP INTEGRATION	SVDQ1075
C		SVDQ1076
C	IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE C IN COLUMN ONE	SVDQ1077
C	OF THE FOLLOWING CARD	SVDQ1078
C	GO TO 310	SVDQ1079
C	ALL STATEMENTS BELOW THIS POINT SHOULD THEN BE REMOVED (EXCEPT	SVDQ1080
C	FOR THE END STATEMENT)	SVDQ1081
	IF (LGSE) 1800,310,1810	SVDQ1082
C		SVDQ1083
C		SVDQ1084
C	SECTION FOR COMPUTING GSTOPS	SVDQ1085
C		SVDQ1086
	ENTRY SVDQG(NG,NSTOP,G,GT)	SVDQ1087
C		SVDQ1088
C	VARIABLES IN THE CALLING SEQUENCE HAVE THE FOLLOWING TYPES.	SVDQ1089
	INTEGER NG,NSTOP	SVDQ1090
	REAL G(1),GT(1)	SVDQ1091
C		SVDQ1092
C	A GSTOP IS DEFINED AS A RETURN WHICH IS MADE TO THE USER WHEN A	SVDQ1093
C	USER SPECIFIED FUNCTION G PASSES THROUGH ZERO. THE USER MAY	SVDQ1094
C	SPECIFY ANY NUMBER OF FUNCTIONS G OF TWO TYPES. ZEROS OF THE FIRST	SVDQ1095
C	TYPE ARE LOCATED WITHOUT REQUIRING A DERIVATIVE EVALUATION	SVDQ1096
C	BEYOND THE ZERO. THIS TYPE OF GSTOP REQUIRES THAT G BE EVALUATED	SVDQ1097
C	BEFORE EACH DERIVATIVE EVALUATION. ZEROS OF THE SECOND TYPE ARE	SVDQ1098
C	LOCATED USING INTERPOLATION, WHICH IS MORE ACCURATE THAN THE	SVDQ1099
C	EXTRAPOLATION USED IN THE PRECEDING CASE AND ONLY REQUIRES ONE	SVDQ1100
C	EVALUATION OF G PER STEP. THUS ONE SHOULD USE THE SECOND TYPE OF	SVDQ1101
C	GSTOP IF POSSIBLE. USERS NOT USING THE GSTOP FEATURE NEED READ	SVDQ1102
C	NO FURTHER.	SVDQ1103
C		SVDQ1104
C	SVDQG IS USED AS A SET UP CALL TO INDICATE A CHANGE IN THE NUMBER	SVDQ1105
C	OR TYPES OF GSTOPS. SVDQG SHOULD BE CALLED JUST BEFORE OR JUST	SVDQ1106

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C AFTER CALLING SVDQ IF SVDQ1107
C 1. ONE WANTS TO TEST FOR GSTOPS BEGINNING WITH THE FIRST STEP. SVDQ1108
C 2. A JOB IS BEING RUN AFTER ANOTHER JOB THAT USES THE GSTOP SVDQ1109
C FEATURE. SVDQG MUST BE CALLED EVEN IF ALL THE VARIABLES IN SVDQ1110
C THE NEW JOB ARE THE SAME. SVDQ1111
C IN ADDITION SVDQG MAY BE CALLED AT ANY TIME IN THE INTEGRATION SVDQ1112
C TO CHANGE THE NUMBER OR TYPE OF GSTOPS. SVDQ1113
C SVDQ1114
C THE USAGE OF THE VARIABLES IS GIVEN BELOW. SVDQ1115
C NG= THE NUMBER OF COMPONENTS IN G TO BE EXAMINED FOR A ZERO. SVDQ1116
C IF SVDQG IS CALLED AFTER THE FIRST STEP OF THE INTEGRATION, SVDQ1117
C THEN G IS EVALUATED FOR THE FIRST TIME AT THE END OF THE SVDQ1118
C NEXT STEP AND THUS A GSTOP IS NOT DETECTED IF G CHANGES SVDQ1119
C SIGN ON THE CURRENT STEP. IF IT IS IMPORTANT THAT G BE SVDQ1120
C EVALUATED IMMEDIATELY SET NG EQUAL TO THE NEGATIVE OF THE SVDQ1121
C NUMBER OF COMPONENTS TO BE TESTED FOR A ZERO. SETTING NG SVDQ1122
C LESS THAN ZERO WHEN CALLING SVDQG BEFORE THE FIRST STEP IS SVDQ1123
C NOT NECESSARY AND IS LIABLE TO BE DISASTEROUS. IF SVDQG IS SVDQ1124
C CALLED DURING THE INTEGRATION THE FOLLOWING STATEMENT SHOULD SVDQ1125
C BE A GO TO (THE COMPUTED GO TO FOLLOWING THE CALL TO SVDQ1). SVDQ1126
C SVDQ1127
C NSTOP=THE NUMBER OF COMPONENTS OF G THAT MUST BE EXAMINED FOR SVDQ1128
C A ZERO BEFORE COMPUTING THE DERIVATIVES (FIRST TYPE OF SVDQ1129
C GSTOP). IF NSTOP.LT.0 OR NSTOP.GT.ABS(NG) IFLAG IS SET SVDQ1130
C EQUAL 8 AND AN IMMEDIATE RETURN IS MADE. IF NSTOP.GT.0, SVDQ1131
C G(1),G(2),...,G(NSTOP) ARE EXAMINED FOR A ZERO BEFORE EACH SVDQ1132
C DERIVATIVE EVALUATION, THE REMAINING COMPONENTS (IF ANY) SVDQ1133
C ARE EXAMINED AT THE END OF EACH STEP. WHEN A GSTOP IS FOUND SVDQ1134
C THE SUBROUTINE SETS NSTOP EQUAL TO THE INDEX OF THE SVDQ1135
C COMPONENT OF G RESPONSIBLE FOR THE STOP. SVDQ1136
C SVDQ1137
C G= A VECTOR CONTAINING THE CURRENT VALUES OF THE FUNCTIONS SVDQ1138
C WHOSE ZEROS ARE TO BE DETERMINED. SVDQ1139
C SVDQ1140
C GT= A VECTOR WITH THE SAME DIMENSION AS G USED BY THE SVDQ1141
C SUBROUTINE FOR TEMPORARY STORAGE. SVDQ1142
C SVDQ1143
C RETURNS FROM CALLING SVDQ1 WITH IFLAG.GT.8 SHOULD BE INTERPETED SVDQ1144
C AS FOLLOWS. (WE USE NSTOPI TO DENOTE THE INITIAL VALUE OF NSTOP.) SVDQ1145
C IFLAG SVDQ1146
C = 9 COMPUTE G(NSTOPI+1),...,G(ABS(NG)) (THE COMPONENTS OF G WITH SVDQ1147
C ZEROS TO BE LOCATED USING INTERPOLATION). THEN CALL SVDQ1. SVDQ1148
C NO RETURN IS MADE WITH IFLAG=9 IF NSTOPI=ABS(NG). SVDQ1149
C =10 COMPUTE G(1),G(2),...,G(NSTOPI) (THE COMPONENTS OF G WITH SVDQ1150
C ZEROS TO BE LOCATED USING EXTRAPOLATION). THEN CALL SVDQ1. SVDQ1151
C NO RETURN IS MADE WITH IFLAG=10 IF NSTOPI=0. SVDQ1152
C -11 G(NSTOP) IS APPROXIMATELY ZERO. IF THERE ARE NO SVDQ1153
C DISCONTINUITIES SIMPLY CALL SVDQ1 TO CONTINUE THE INTEGRATION. SVDQ1154
C =12 G(NSTOP) CHANGES SIGN, BUT THERE IS DIFFICULTY IN CONVERGING SVDQ1155
C TO A ZERO. THE USER MAY WISH TO MAKE A SPECIAL CHECK TO BE SVDQ1156
C CERTAIN THAT EVERYTHING IS ALL RIGHT. TO CONTINUE THE SVDQ1157
C INTEGRATION CALL SVDQ1. SVDQ1158
C SVDQ1159
C REAL RG SVDQ1160
C DIMENSION GI(2),RG(3) SVDQ1161
C SVDQ1162
C INITIALIZE FOR GSTOPS SVDQ1163
C NGA=IABS(NG) SVDQ1164
C LGSS=-NGA SVDQ1165

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LGSD=0	SVDQ1166
LGSE=0	SVDQ1167
IFLG=-20	SVDQ1168
IF (NG.GE.0) RETURN	SVDQ1169
IFLG=-IFL	SVDQ1170
1430 LGSD=NSTOP	SVDQ1171
IF (LGSD) 1190,1450,1440	SVDQ1172
1440 IFL=15	SVDQ1173
GO TO 1470	SVDQ1174
C ENTRY WITH IFL=15	SVDQ1175
1450 LGSS=0	SVDQ1176
IF (LGSD-NGA) 1460,1480,1190	SVDQ1177
1460 LGSS=LGSD+1	SVDQ1178
IFL=14	SVDQ1179
1470 IFLAG=IFL-5	SVDQ1180
GO TO 315	SVDQ1181
C ENTRY WITH IFL=14	SVDQ1182
1480 DO 1490 I=1,NGA	SVDQ1183
1490 GT(I)=G(I)	SVDQ1184
GO TO 1730	SVDQ1185
C END OF INITIALIZATION FOR GSTOPS	SVDQ1186
C	SVDQ1187
C ENTRY TO EVALUATE G AT THE END OF THE STEP	SVDQ1188
1500 LGSE=1	SVDQ1189
1510 IGK=LGSS	SVDQ1190
IFLG=0	SVDQ1191
IFL=9	SVDQ1192
GO TO 310	SVDQ1193
C ENTRY TO EVALUATE G BEFORE EVALUATING THE DERIVATIVES	SVDQ1194
1520 IFLG=IFL	SVDQ1195
IFL=10	SVDQ1196
1530 IFLAG=10	SVDQ1197
IGKM=LGSD	SVDQ1198
1540 IGK=1	SVDQ1199
1550 GO TO 315	SVDQ1200
1560 IGK=IGK+1	SVDQ1201
IF (IGK.GT.IGKM) GO TO 1650	SVDQ1202
C ENTRY WITH IFL=9,10, AND 17	SVDQ1203
C TEST FOR G CHANGING SIGN	SVDQ1204
1570 IF (G(IGK)*GT(IGK)) 1600,1580,1590	SVDQ1205
1580 IF (GT(IGK).NE.0.) GO TO 1600	SVDQ1206
IF (TL.EQ.TG) GO TO 1560	SVDQ1207
1590 IF (LGSE.GT.0) GT(IGK)=G(IGK)	SVDQ1208
GO TO 1560	SVDQ1209
C G CHANGES SIGN -- PREPARE FOR ITERATION TO FIND ZERO	SVDQ1210
1600 NSTOP=IGK	SVDQ1211
NSTOPI=IGK	SVDQ1212
IFLGS=IFL	SVDQ1213
C COMPUTE INITIAL VALUE FOR RG (=RATIO OF PARTIAL STEPSIZE WHERE	SVDQ1214
C G IS KNOWN/THE INTEGRATION STEPSIZE)	SVDQ1215
IF (IFLG.EQ.0) GO TO 1610	SVDQ1216
RG(3)=FAC(1)	SVDQ1217
RG(2)=0.E0	SVDQ1218
IF ((IFLG.EQ.2).AND.(IGK.LT.LGSS)) RG(2)=FAC(1)	SVDQ1219
GO TO 1620	SVDQ1220
1610 RG(3)=0.E0	SVDQ1221
RG(2)=-FAC(1)	SVDQ1222
1620 IF (LGSE.LT.0) RG(3)=IPD	SVDQ1223
LGSE=-3	SVDQ1224



GI(2)=GT(IGK)	SVDQ1225
EPSGS=RND	SVDQ1226
IFL=16	SVDQ1227
K=1	SVDQ1228
GO TO 1640	SVDQ1229
C END OF PREPARATION TO BEGIN THE ITERATION	SVDQ1230
C	SVDQ1231
C ENTRY WITH IFL=16	SVDQ1232
C ITERATE TO FIND GSTOP	SVDQ1233
1630 K=1	SVDQ1234
IF ((GI(2)*G(IGK)).GT.0.) K=2	SVDQ1235
IF (ABS(GI(K)).GT.ABS(G(IGK))) GO TO 1640	SVDQ1236
C CONVERGENCE PROBLEMS	SVDQ1237
LGSE=LGSE-1	SVDQ1238
IF (LGSE.EQ.(-5)) EPSGS=PTS1	SVDQ1239
EPSGS=EPSGS*PTS4	SVDQ1240
1640 GI(K)=G(IGK)	SVDQ1241
RG(K)=RG(3)	SVDQ1242
C SECANT ITERATION (GIVES NEW PARTIAL STEPSIZE/H)	SVDQ1243
TPD=RG(1)-(GI(1)*(RG(2)-RG(1)))/(GI(2)-GI(1))	SVDQ1244
T=TL+TPD*HH	SVDQ1245
C TEST FOR CONVERGENCE OF ITERATION	SVDQ1246
IF (ABS(TPD-RG(3)).LE.EPSGS) GO TO 1560	SVDQ1247
RG(3)=TPD	SVDQ1248
GO TO 1300	SVDQ1249
1650 IF (10-IFL) 1660,1700,100	SVDQ1250
1660 IF (IGKM.NE.NGA) GO TO 1710	SVDQ1251
IF (LGSE.GT.(-3)) GO TO 1690	SVDQ1252
IF (LSTC.NE.4) GO TO 1670	SVDQ1253
C ESTIMATE ERROR -- GSTOP IS THE RESULT OF EXTRAPOLATING FROM	SVDQ1254
C THE INITIAL POINT	SVDQ1255
TPD1=TPD	SVDQ1256
RG(3)=TPD	SVDQ1257
GO TO 1230	SVDQ1258
1670 IFL=11	SVDQ1259
IF (LGSE.LT.(-4)) IFL=12	SVDQ1260
1680 IFLAG=IFL	SVDQ1261
C TEST TO SEE IF GSTOP IS PRECEDED BY ANOTHER STOP	SVDQ1262
IF (((T-TOUT)*HH.LE.0.E0).AND.((T-TFINAL)*HH.LE.0.E0)) GO TO 1300	SVDQ1263
C IT IS	SVDQ1264
RG(3)=TPD	SVDQ1265
IFLS=IFL	SVDQ1266
GO TO 200	SVDQ1267
1690 LGSE=1	SVDQ1268
IFL=IFLG	SVDQ1269
IF (IFL.LT.0) GO TO 20	SVDQ1270
1700 IGKM=NGA	SVDQ1271
IFL=IFLG	SVDQ1272
GO TO 310	SVDQ1273
1710 IFL=17	SVDQ1274
IFLAG=9	SVDQ1275
IGKM=NGA	SVDQ1276
GO TO 315	SVDQ1277
C ENTRY WITH IFL=11 AND 12	SVDQ1278
C SET PARAMETERS TO INDICATE A GSTOP HAS BEEN FOUND	SVDQ1279
1720 GT(NSTOP1)=0.	SVDQ1280
1730 LGSE=1	SVDQ1281
IGKM=NGA	SVDQ1282
TG=TL	SVDQ1283

IF (IFLG) 1740,1760,1770	SVDQ1284
1740 IF (IFL.LT.13) GO TO 1750	SVDQ1285
IF (IFLG.EQ.(-20)) GO TO 100	SVDQ1286
IFL=-IFLG	SVDQ1287
GO TO 310	SVDQ1288
1750 HH=H	SVDQ1289
GO TO 200	SVDQ1290
1760 TPD=C.EQ	SVDQ1291
T=TL	SVDQ1292
LGSE=-2	SVDQ1293
GO TO 1300	SVDQ1294
1770 IF (IFLG-3) 220,200,200	SVDQ1295
1780 IF (LGSE.EQ.(-1)) GO TO 1790	SVDQ1296
LGSE=-1	SVDQ1297
GO TO 1220	SVDQ1298
1790 TPD=RG(3)	SVDQ1299
T=TL+TPD*HH	SVDQ1300
IF (LGSE.NE.(-1)) GO TO 1670	SVDQ1301
IFL=IFLS	SVDQ1302
LGSE=-3	SVDQ1303
GO TO 1680	SVDQ1304
1800 IF (LGSE+2) 1550,1500,310	SVDQ1305
1810 IF (TPD.LE.0.EQ) GO TO 310	SVDQ1306
LGSE=-2	SVDQ1307
1820 IFLG=IFL	SVDQ1308
IFL=17	SVDQ1309
IFLAG=9	SVDQ1310
IF (LGSD) 1540,1540,1530	SVDQ1311
END OF SECTION FOR COMPUTING GSTOPS	SVDQ1312
C	SVDQ1313
C	SVDQ1314
C	SVDQ1315
C	SVDQ1316
C	SVDQ1317
C	SVDQ1318
C	SVDQ1319
C	SVDQ1320
C	SVDQ1321
C	SVDQ1322
C	SVDQ1323
C	SVDQ1324
C	SVDQ1325
C	SVDQ1326
C	SVDQ1327
C	SVDQ1328
C	SVDQ1329
C	SVDQ1330
C	SVDQ1331
C	SVDQ1332
C	SVDQ1333
C	SVDQ1334
C	SVDQ1335
C	SVDQ1336
C	SVDQ1337
C	SVDQ1338
C	SVDQ1339
C	SVDQ1340
C	SVDQ1341
C	SVDQ1342

C	303,449,491,537,947,980,985,999, AND 1076.	SVDQ1343
C	THIS MAKES THE SUBROUTINE SHORTER AND REDUCES OVERHEAD A LITTLE.	SVDQ1344
C		SVDQ1345
C	TO REMOVE THE INTERPOLATION CAPABILITY, SEE JUST BELOW CARDS	SVDQ1346
C	SEQUENCED 816 AND 965.	SVDQ1347
C	THE GSTOP FEATURE MUST ALSO BE ELIMINATED SINCE IT REQUIRES THE	SVDQ1348
C	INTERPOLATION CAPABILITY. IF OUTPUT POINTS ARE NOT HIT EXACTLY	SVDQ1349
C	(THEY ARE HIT EXACTLY IF $HMAXA \cdot LE \cdot ABS(DELT)$ , AND INITIAL $H =$	SVDQ1350
C	$DELT * (2 * (-K))$ , $K = 0, 1, 2, \dots$ ), THEN $IFLAG = 3$ ON THE FIRST STEP THAT	SVDQ1351
C	$(T - TOUT) * H \cdot GT \cdot 0$ (SEE THE USAGE OF DELT). $IFLAG$ IS SET EQUAL TO 4	SVDQ1352
C	ON THE LAST STEP THAT $(T - TFINAL) * H \cdot LE \cdot 0$ .	SVDQ1353
C		SVDQ1354
C	THE OUTPUT OPTION GIVES OUTPUT OF VARIABLES USED IN THE	SVDQ1355
C	INTEGRATION ON EVERY STEP THAT $NEQ \cdot LE \cdot 0$ . (WHICH OF COURSE MUST	SVDQ1356
C	BE SET AFTER THE INITIAL CALL TO THE INTEGRATOR) TO ELIMINATE	SVDQ1357
C	THIS OPTION, SEE JUST BELOW CARDS SEQUENCED 580 AND 803.	SVDQ1358
C		SVDQ1359
C	THE CHECK OPTION WHEN ADDED TO THE OUTPUT OPTION OUTPUTS EVERY	SVDQ1360
C	VARIABLE IN THE CALLING SEQUENCE JUST AFTER ENTERING AND JUST	SVDQ1361
C	BEFORE LEAVING THE INTEGRATOR WHEN $NEQ = 0$ . THIS OUTPUT IS	SVDQ1362
C	SOMETIMES USEFUL IN DEBUGGING A PROGRAM. TO INCLUDE THIS OPTION	SVDQ1363
C	SEE JUST BELOW CARDS SEQUENCED 359 AND 548.	SVDQ1364
C		SVDQ1365
C	END	SVDQ1366

#### A-5. DESCRIPTIONS OF PROGRAM LOGIC, SUBROUTINES AND USE OF TEXT EQUATIONS

A FORFLO chart of the overall program is shown in Figure A-1. The purpose of each subroutine was indicated by comment cards in the listing presented in Appendix A-4. A brief summary indicating the usage of the text equations is presented as follows.

DATAIN loads input and calculates various constants (in the nature of input) which are used throughout the program. For example, DATAIN calculates thermal diffusivity and dimensionless frequency from constituent inputs. DATAIN also equalizes all thermal properties to represent a homogeneous solid if IHOMO=1.

Function TAU defines the dimensionless temperature.

SLDFAZ solves Eq. (12) for wall temperature. If burn rate is specified, ITERA = 0, only one pass is made to calculate the wall temperature associated with that rate. If ITERA = 1, burn rate and wall temperature are solved by iteration in association with subroutine GASFAZ. SLDFAZ also calculates certain constants that are associated with Eqs. (4), (5) and (22) and are needed to calculate the thermal profiles.

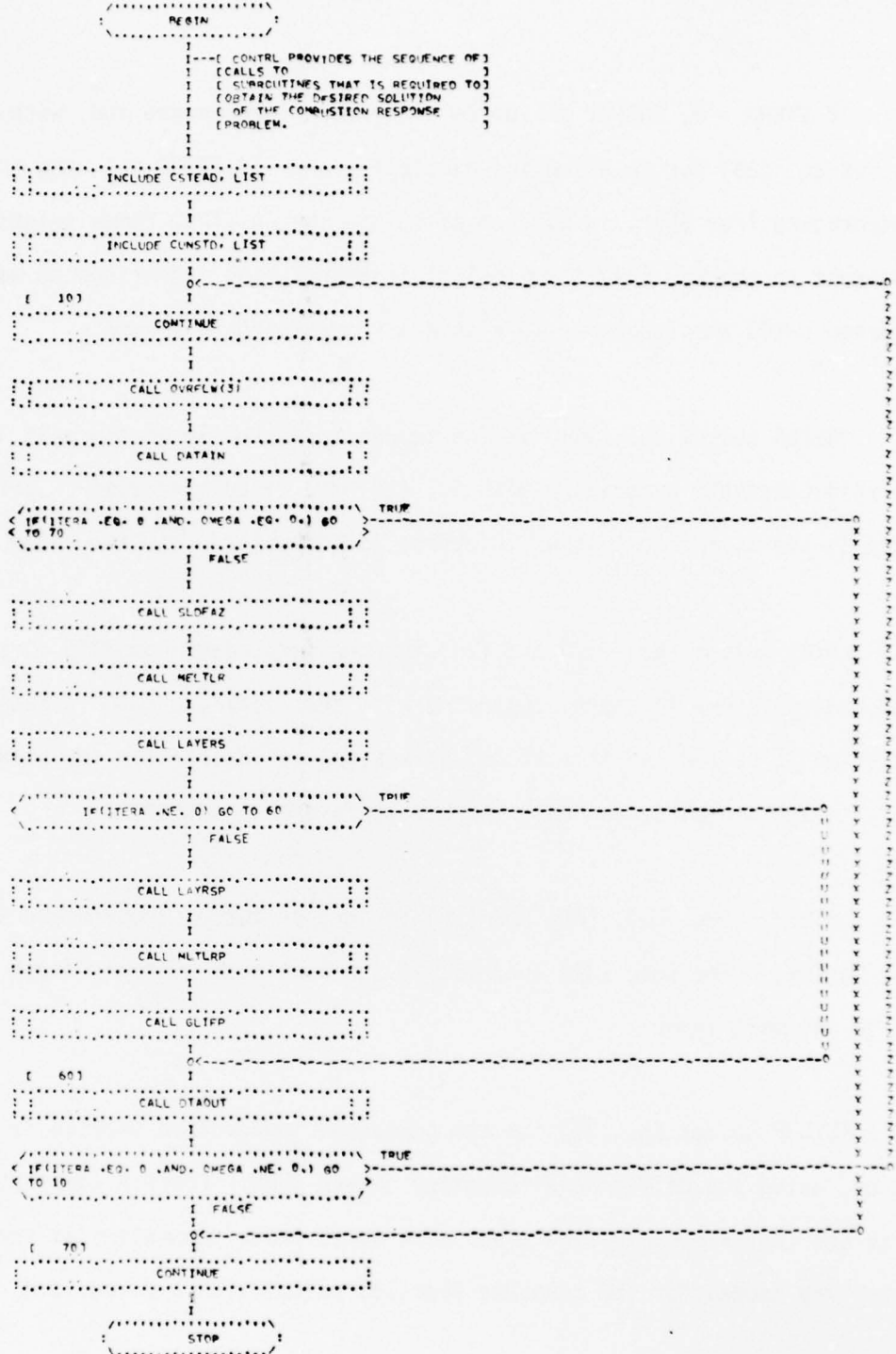


FIGURE A-1. FORFLO Chart of Overall Program



If ITERA = 0, GASFAZ solves Eq. (23) for flame height and, with AMULTI, solves Eq. (24) for an effective particle size. If ITERA = 1, the trial wall temperature from SLDFZ is used to calculate the Eq. (23) flame height. This is compared to the Eq. (24) flame height in AMULTI, and iterations on wall temperature proceed until the two agree to within a preassigned tolerance.

MELTLR solves Eq. (16) for the temperature profile in the melt layer. Certain constants associated with Eq. (16) are calculated also. Surface temperature is known, and melt layer thickness is determined from the known melting point.

LAYRS solves Eqs. (17) and (18) for the temperature profile in the succeeding layers in depth, beginning with the melting point. A satisfactory solution is tested in terms of the dimensionless temperature and gradient tending to zero at some adequate depth (number of layers traversed).

LAYRSP solves Eqs. (35) and (36) for the perturbed temperature profile in the layers, using Eqs. (34) and (38) to start at some adequate depth and working up to the melt layer.

MLTLRP solves Eq. (28) for the perturbed temperature profile in the melt layer, using the differential equation solver SVDQ. Certain constants associated with Eq. (28) are calculated also. The solid phase parameters at the mean surface which are needed for the response function calculation are provided.

GLIFP calculates the response function, Eq. (50), and the zero frequency limit, Eq. (53). Using Eqs. (29) - (31), the solid phase parameters at the mean surface are converted to values at the oscillating surface. Necessary gas phase parameters derived from Eq. (47) are calculated also.

DTAOUT prints the input and output.

Auxiliary JPL library routines which are used to solve the equations in the melt layer are subroutine PFIT, function SCPVAL and subroutine SVDQ. These were included in the listing to provide a self-contained program. PFIT and SCPVAL are called by MELTLR (steady-state solution); SVDQ and SCPVAL are called by MLTLRP (perturbed, complex solution). PFIT is a polynomial least squares curve fitting routine and SCPVAL evaluates the polynomial at a specified argument. Subroutines BHSLR, AHLR and SL2NRM are orthogonal transformation subroutines which are called by PFIT to solve the least squares problem. SVDQ computes the numerical solution of the ordinary differential equation describing the perturbed melt layer.

A-6. SOLUTIONS TO SAMPLE PROBLEM

COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

NDEG= 6	SIGFAC= .0000		
P(1),...,P(NDEG+3)=	.19436020	.19436020	.84546567
	-.17224529	-.01451589	.00289440
	-.00031804	-.00000467	.00000915

TOLERANCE TESTS FOR A SATISFACTORY STEADY-STATE SOLUTION HAVE BEEN MET.

A SATISFACTORY STEADY-STATE SOLUTION HAS BEEN OBTAINED.

## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

YABRV	TAPR	DTAPR	D2TAPR
IFLAG= 3	H= -.388720-02		
.338720+00	-.479468-16	.446635-16	.699864-16
IFLAG= 3	H= -.388720-02		
.349848+00	-.496136-16	.408895-16	.119785-15
IFLAG= 3	H= -.388720-02		
.310976+00	-.510967-16	.349742-16	.188050-15
IFLAG= 3	H= -.388720-02		
.272104+00	-.522927-16	.259677-16	.279606-15
IFLAG= 3	H= -.388720-02		
.233232+00	-.530627-16	.128803-16	.398577-15
IFLAG= 3	H= -.388720-02		
.194360+00	-.532267-16	-.539890-17	.546672-15
IFLAG= 3	H= -.388720-02		
.155483+00	-.525615-16	-.299537-16	.720195-15
IFLAG= 3	H= -.388720-02		
.116616+00	-.508064-16	-.615565-16	.906141-15
IFLAG= 3	H= -.388720-02		
.777441-01	-.476837-16	-.100234-15	.107872-14
IFLAG= 3	H= -.388720-02		
.388721-01	-.429374-16	-.144748-15	.119919-14
IFLAG= 3	H= -.388720-02		
.144355-07	-.363915-16	-.192204-15	.122273-14
IFLAG= 4	H= -.388720-02		
.000000	-.363915-16	-.192204-15	.122273-14

YABRV

TAPI

DTAPI

D2TAPI



# COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

IFLAG= 3	H=	-.388720-02		
		.388720+00	-.291908-16	.723704-16
				-.256974-17
IFLAG= 3	H=	-.388720-02		
		.349843+00	-.319983-16	.718517-16
				.317750-16
IFLAG= 3	H=	-.388720-02		
		.310976+00	-.347558-16	.696997-16
				.820005-16
IFLAG= 3	H=	-.388720-02		
		.272104+00	-.373863-16	.652042-16
				.153267-15
IFLAG= 3	H=	-.388720-02		
		.233232+00	-.397828-16	.574403-16
				.251042-15
IFLAG= 3	H=	-.388720-02		
		.194360+00	-.417956-16	.452850-16
				.379742-15
IFLAG= 3	H=	-.388720-02		
		.155483+00	-.432305-16	.275029-16
				.540203-15
IFLAG= 3	H=	-.388720-02		
		.116610+00	-.438459-16	.295507-17
				.725921-15
IFLAG= 3	H=	-.388720-02		
		.777441-01	-.433634-16	-.290331-16
				.918866-15
IFLAG= 3	H=	-.388720-02		
		.388721-01	-.414955-16	-.681674-16
				.108720-14
IFLAG= 3	H=	-.388720-02		
		.144355-07	-.379932-16	-.112688-15
				.118857-14
IFLAG= 4	H=	-.388720-02		
		.000000	-.379932-16	-.112688-15
				.118857-14

\$TPOUT3

K2	=	(.40739436E+01, -.11566977E+01)
V3	=	.43017409E+00
V5	=	.38842347E+01
V6A	=	.15725228E+01
V6B	=	.19052972E+01
V7	=	.24288042E+00
RFO	=	.42596531E+00

## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

```

K2NM      =      .00000000E+00
V5NM      =      .00000000E+00
$END
$INPUT
CA         =      .32800000E+00
CB         =      .30000000E+00
CG         =      .30000000E+00
KA         =      .90000000E-03
KB         =      .44000000E-03
ROA        =      .19500000E+01
ROB        =      .90000000E+00
WAC        =      .33000000E+00,      .54000000E+00,      .00000000E+00,      .00000000E+00
SMLA       =      .45000000E-02,      .20000000E-01,      .00000000E+00,      .00000000E+00
E          =      .22000000E+05
R          =      .19862000E+01
PRXFAC     =      .13500000E+09
QS         =      -.20957000E+03
QB         =      .56900000E+03
QLM        =      .59570000E+02
KFLHHT     =      .24600000E+02
TFLM       =      .21000000E+04
TH         =      .83315000E+03
TZRO       =      .30000000E+03
PBAR       =      .34030000E+02
RBR        =      .12300000E+01
TOL        =      .10000000E-04
ITERA      =      +0
NSMAX      =      +50
NPP        =      ( .50000000E-02,      .00000000E+00 )
TAPIN      =      ( .10000000E-29,      .00000000E+00 )
YTD        =      .10000000E+02
OMEGA      =      .12566000E+04
NEQ        =      +1
KD         =      +2
MXSTEP     =      +100
EP         =      .10000000E-04
IHOMO      =      +0
$END
$OUTPT1
JMAX       =      +2
WA         =      .37000000E+00
DNM        =      .10033333E+03
WB         =      .13000001E+00
VFA        =      .75542691E+00
SMLAFP     =      .16329932E-01
DLTYTP     =      .14274320E+02
DLTYAB     =      .39335400E+01
SMLB       =      .65503794E-02
DLTYBB     =      .19440478E+01
KS         =      .90000000E-03
ROS        =      .16931982E+01
CS         =      .32436000E+00
KAPA       =      .14071294E-02
KAPB       =      .16296296E-02
KAPS       =      .16387300E-02
Z          =      .85867067E+00
ZPR        =      .20340954E+01

```

## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

\*END

\*OUTPT2

THETA = .10012712E+02

CHI = .72881025E+00

D = .72973667E+01

QSDMLS = -.68946471E+00

QBDMLS = .30582425E+00

QMDMLS = .19597945E+00

FDMLS = -.21616689E+00

B = -.86570440E+05

KMLTLR = -.53178746E+00

\*END

\*OUTPT3

TWBAR = .11062365E+04

YSSTR = .94488705E+00

XSTR = .12588738E-02

AMM = .14158066E-02

TAUMLT = .99661283E+00, .99322566E+00, .98983848E+00, .98645131E+00,

.98306413E+00, .97967695E+00, .97628978E+00, .97290260E+00,

.96951543E+00, .96612825E+00, .96274108E+00, .95935390E+00,

.95596673E+00, .95257955E+00, .94919237E+00, .94580520E+00,

.94241802E+00, .93903085E+00, .93564367E+00, .93225650E+00,

.92886932E+00, .92548215E+00, .92209497E+00, .91870780E+00,

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.67144398E+00, .66805681E+00, .66466963E+00, .66128246E+00,

.00000000E+00, .00000000E+00, .00000000E+00, .00000000E+00,

.00000000E+00, .00000000E+00, .00000000E+00, .00000000E+00,

.00000000E+00, .00000000E+00, .00000000E+00, .00000000E+00,

XMLT = .87110704E-05, .16906565E-04, .24678197E-04, .32093999E-04,

.39205886E-04, .46054691E-04, .52673046E-04, .59087671E-04,

.65320610E-04, .71390445E-04, .77312846E-04, .83101363E-04,

.88767592E-04, .94321742E-04, .99772671E-04, .10512831E-03,

.11039558E-03, .11558078E-03, .12068946E-03, .12572670E-03,

.13069701E-03, .13560458E-03, .14045313E-03, .14524615E-03,

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.16847998E-03, .1729791E-03, .17747784E-03, .18192166E-03,

.18633102E-03, .19070757E-03, .19505277E-03, .19936806E-03,

.20365472E-03, .20791404E-03, .21214713E-03, .21635514E-03,

.22053907E-03, .22469994E-03, .22883863E-03, .23295607E-03,

.23705304E-03, .24113038E-03, .24518879E-03, .24922903E-03,

## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

	.25325174E-03,	.25725760E-03,	.26124719E-03,	.26522113E-03,
	.26917995E-03,	.27312420E-03,	.27705438E-03,	.28097099E-03,
	.28487448E-03,	.28876531E-03,	.29264389E-03,	.29651067E-03,
	.30036598E-03,	.30421025E-03,	.30804382E-03,	.31186704E-03,
	.31568024E-03,	.31948374E-03,	.32327785E-03,	.32706287E-03,
	.33083907E-03,	.33460675E-03,	.33836614E-03,	.34211753E-03,
	.34586112E-03,	.34959721E-03,	.35332597E-03,	.35704764E-03,
	.36076244E-03,	.36447057E-03,	.36817221E-03,	.37186758E-03,
	.37555683E-03,	.37924018E-03,	.38291777E-03,	.38658978E-03,
	.39025635E-03,	.39391768E-03,	.39757387E-03,	.40122510E-03,
	.40487149E-03,	.40851320E-03,	.41215033E-03,	.41578304E-03,
	.41941143E-03,	.42303563E-03,	.42665576E-03,	.43027192E-03,
	.43388423E-03,	.43749280E-03,	.44109772E-03,	.44469911E-03,
	.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
	.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
	.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
M	=	+101		
N	=	+99		
RBR	=	.12300000E+01		
ITERA	=	+0		
NS	=	+1		
NSMAX	=	+50		
LFLAG	=	+1		
GWBR5	=	-.43017409E+00		
DGWBR5	=	-.34504740E+01		
QDML5	=	-.68946471E+00		
END				
OUTPT4				
TAULR	=	.66128246E+00,	.93458967E-01,	-.95290865E-01,
		.15364397E-01,	.24296824E-02,	-.24773068E-02,
		.39943310E-03,	.63165220E-04,	-.64403327E-04,
		.10384188E-04,	.16421262E-05,	-.16743137E-05,
		.26996103E-06,	.42690874E-07,	-.43527661E-07,
		.70182622E-08,	.11098481E-08,	-.11316024E-08,
		.18245598E-09,	.28853073E-10,	-.29418624E-10,
		.47433658E-11,	.75010245E-12,	-.76480528E-12,
		.12331478E-12,	.19500651E-13,	-.19882885E-13,
		.32058533E-14,	.50696458E-15,	-.51690164E-15,
		.83343583E-16,	.13179719E-16,	-.13438055E-16,
		.21667095E-17,	.34263731E-18,	-.34935337E-18,
		.56328630E-19,	.69076502E-20,	-.90822499E-20,
		.14643932E-20,	.23157500E-21,	-.23611412E-21,
		.38070294E-22,	.60203286E-23,	-.61383336E-23,
		.98972545E-24,	.15651238E-24,	-.15958020E-24,
		.25730206E-25,	.40689019E-26,	-.41486568E-26,
		.66891628E-27,	.10578053E-27,	-.10785394E-27,
		.17390028E-28,	.27500098E-29,	-.28039130E-29,
		.45209405E-30,	.71492874E-31,	-.72894211E-31,
		.11753232E-31,	.18586228E-32,	-.18950538E-32,
		.30555248E-33,	.48319205E-34,	-.49266314E-34,
		.79435445E-35,	.12561697E-35,	-.12807920E-35,
		.20651084E-36,	.32657040E-37,	-.33770496E-37,
		.49354910E-38,	.00000000E+00,	.00000000E+00,
		.00000000E+00,	.00000000E+00,	.00000000E+00,
		.00000000E+00,	.00000000E+00,	.00000000E+00,
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		.00000000E+00,	.00000000E+00,	.00000000E+00,
DTAULR	=	-.73799413E+00,	-.35855919E-06,	-.13546264E-02,
				.16016336E-02,



## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

XLR

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DSCRIM

=

.21841563E-03,	-.25824233E-03,	-.35216653E-04,	.41638174E-04,
.56782192E-05,	-.67136070E-05,	-.91553829E-06,	.10824808E-05,
.14761649E-06,	-.17453577E-06,	-.23801533E-07,	.28141596E-07,
.38376839E-08,	-.45374615E-08,	-.61877614E-09,	.73160594E-09,
.99769526E-10,	-.11796182E-09,	-.16086521E-10,	.19019791E-10,
.25937395E-11,	-.30666908E-11,	-.41820627E-12,	.49446352E-12,
.67430274E-13,	-.79725729E-13,	-.10872244E-13,	.12854724E-13,
.17530058E-14,	-.20726551E-14,	-.28264918E-15,	.33418833E-15,
.45573443E-16,	-.53883465E-16,	-.73481167E-17,	.86879996E-17,
.11847873E-17,	-.14008256E-17,	-.19103137E-18,	.22586466E-18,
.30801285E-19,	-.36417706E-19,	-.49663019E-20,	.58718749E-20,
.80075041E-21,	-.94676254E-21,	-.12911055E-21,	.15265300E-21,
.20817370E-22,	-.24613287E-22,	-.33565274E-23,	.39685683E-23,
.54119566E-24,	-.63987940E-24,	-.87260687E-25,	.10317212E-24,
.14069642E-25,	-.16635146E-25,	-.22685436E-26,	.26821983E-26,
.36577262E-27,	-.43246916E-27,	-.58976067E-28,	.69729955E-28,
.95091106E-29,	-.11243037E-28,	-.15332193E-29,	.18127917E-29,
.24721135E-30,	-.29228879E-30,	-.39859579E-31,	.47127720E-31,
.64268332E-32,	-.75987239E-32,	-.10362424E-32,	.12251942E-32,
.16708045E-33,	-.19754642E-33,	-.26939507E-34,	.31851761E-34,
.43436410E-35,	-.51356770E-35,	-.70035471E-36,	.82606031E-36,
.11292304E-36,	-.13351382E-36,	-.18207351E-37,	.21527347E-37,
.29356951E-38,	-.34710009E-38,	.00000000E+00,	.00000000E+00,
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.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
.44469911E-03,	.16774631E-01,	.23325010E-01,	.27625010E-01,
.34375389E-01,	.38875389E-01,	.45425768E-01,	.49925768E-01,
.56476147E-01,	.60976147E-01,	.67526526E-01,	.72026526E-01,
.78576905E-01,	.83076905E-01,	.89627284E-01,	.94127283E-01,
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.12277842E+00,	.12727842E+00,	.13382880E+00,	.13832880E+00,
.14487918E+00,	.14937918E+00,	.15592956E+00,	.16042956E+00,
.16697994E+00,	.17147993E+00,	.17803031E+00,	.18253031E+00,
.18908069E+00,	.19358069E+00,	.20013107E+00,	.20463107E+00,
.21118145E+00,	.21568145E+00,	.22223183E+00,	.22673183E+00,
.23328221E+00,	.23778221E+00,	.24433259E+00,	.24883259E+00,
.25538297E+00,	.25988296E+00,	.26643334E+00,	.27093334E+00,
.27748372E+00,	.28198372E+00,	.28853410E+00,	.29303410E+00,
.29958447E+00,	.30408447E+00,	.31063485E+00,	.31513485E+00,
.32168523E+00,	.32618523E+00,	.33273561E+00,	.33723561E+00,
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.38798749E+00,	.39248749E+00,	.39903787E+00,	.40353787E+00,
.41008824E+00,	.41458824E+00,	.42113862E+00,	.42563862E+00,
.43218900E+00,	.43668900E+00,	.44323938E+00,	.44773937E+00,
.45428975E+00,	.45878975E+00,	.46534013E+00,	.46984013E+00,
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.15582813E-01,	.21714400E-02,	-.25125234E-02,	-.35011611E-03,



## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

		.40511132E-03,	.56451613E-04,	-.65318865E-04,	-.91020792E-05,
		.10531807E-04,	.14675904E-05,	-.16981152E-05,	-.23662963E-06,
		.27379872E-06,	.38153412E-07,	-.44146438E-07,	-.61517353E-08,
		.71180318E-08,	.99188632E-09,	-.11476889E-08,	-.15992861E-09,
		.18504972E-09,	.25786382E-10,	-.29836830E-10,	-.41577145E-11,
		.48107961E-11,	.67037672E-12,	-.77567752E-12,	-.10808942E-12,
		.12506779E-12,	.17427996E-13,	-.20165534E-13,	-.28100348E-14,
		.32514268E-14,	.45308111E-15,	-.52424975E-15,	-.73053363E-16,
		.84528370E-16,	.11778893E-16,	-.13629087E-16,	-.18991914E-17,
		.21975107E-17,	.30621960E-18,	-.35431967E-18,	-.49373878E-19,
		.57129381E-19,	.79608877E-20,	-.92113604E-20,	-.12835883E-20,
		.14852106E-20,	.20696171E-21,	-.23947065E-21,	-.33369851E-22,
		.38611489E-22,	.53804492E-23,	-.62255943E-23,	-.86752658E-24,
		.10037951E-23,	.13987724E-24,	-.16184874E-24,	-.22553363E-25,
		.26095978E-25,	.36364328E-26,	-.42076329E-26,	-.58632690E-27,
		.67842539E-27,	.94537491E-28,	-.10938716E-27,	-.15242925E-28,
		.17637239E-28,	.24577210E-29,	-.28437726E-29,	-.39627515E-30,
		.45852088E-30,	.63894150E-31,	-.73930454E-31,	-.10302090E-31,
		.11920312E-31,	.16610764E-32,	-.19219933E-32,	-.26782669E-33,
		.30989612E-33,	.43183528E-34,	-.49966669E-34,	-.69627753E-35,
		.80564675E-35,	.11226558E-35,	-.12989993E-35,	-.18101347E-36,
		.20944654E-36,	.29186039E-37,	-.33770496E-37,	-.47727617E-38,
		.49354910E-38,	.00000000E+00,	.00000000E+00,	.00000000E+00,
		.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
		.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
		.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
N	=		+99		
XTD	=	.11419713E-01			
CAPOA	=	.11687480E+01			
CAPOB	=	.13535545E+01			
CAPOS	=	.13611132E+01			
%END					
%OUTPTS					
N2	=		+0		
N2MXP1	=		+4		
TAPIN	=	(.10000000E-27,	.00000000E+00)		
DTAPIN	=	(-.13500550E-29,	-.68745435E-30)		
XLR	=	.44469911E-03,	.16774631E-01,	.23325010E-01,	.27825010E-01,
		.34375389E-01,	.38875389E-01,	.45425768E-01,	.49925768E-01,
		.56476147E-01,	.60976147E-01,	.67526526E-01,	.72026526E-01,
		.78576905E-01,	.83076905E-01,	.89627284E-01,	.94127283E-01,
		.10067766E+00,	.10517766E+00,	.11172804E+00,	.11622804E+00,
		.12277842E+00,	.12727842E+00,	.13382880E+00,	.13832880E+00,
		.14487918E+00,	.14937918E+00,	.15592956E+00,	.16042956E+00,
		.16697994E+00,	.17147993E+00,	.17803031E+00,	.18253031E+00,
		.18908069E+00,	.19358069E+00,	.20013107E+00,	.20463107E+00,
		.21118145E+00,	.21568145E+00,	.22223183E+00,	.22673183E+00,
		.23328221E+00,	.23778221E+00,	.24433259E+00,	.24883259E+00,
		.25538297E+00,	.25988296E+00,	.26643334E+00,	.27093334E+00,
		.27748372E+00,	.28198372E+00,	.28853410E+00,	.29303410E+00,
		.29958447E+00,	.30408447E+00,	.31063485E+00,	.31513485E+00,
		.32168523E+00,	.32618523E+00,	.33273561E+00,	.33723560E+00,
		.34378598E+00,	.34828598E+00,	.35483636E+00,	.35933636E+00,
		.36588674E+00,	.37038673E+00,	.37693711E+00,	.38143711E+00,
		.38798749E+00,	.39248749E+00,	.39903787E+00,	.40353787E+00,
		.41008824E+00,	.41458824E+00,	.42113862E+00,	.42563862E+00,
		.43218900E+00,	.43668900E+00,	.44323938E+00,	.44773937E+00,

## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

TAPLR

三

45428975E+00,	45878975E+00,	46534013E+00,	46784013E+00,
47639051E+00,	48089051E+00,	48744088E+00,	48994088E+00,
49849126E+00,	50299126E+00,	50954164E+00,	51404163E+00,
52059201E+00,	52509201E+00,	53164238E+00,	53614238E+00,
54269276E+00,	54719275E+00,	55374313E+00,	55824313E+00,
56479351E+00,	56989351E+00,	57739428E+00,	58189428E+00,
58689426E+00,	59199426E+00,	59949501E+00,	60399501E+00,
60899576E+00,	61409576E+00,	62209651E+00,	62659651E+00,
64419726E+00,	64869726E+00,	65629801E+00,	66079801E+00,
68049876E+00,	68499876E+00,	69309951E+00,	69759951E+00,
70660001E+00,	71110001E+00,	71990076E+00,	72440076E+00,
74010151E+00,	74460151E+00,	75340226E+00,	75790226E+00,
77160301E+00,	77610301E+00,	78490376E+00,	78940376E+00,
80340451E+00,	80790451E+00,	81630526E+00,	82080526E+00,
84010601E+00,	84460601E+00,	85300676E+00,	85750676E+00,
87660726E+00,	88110726E+00,	88990801E+00,	89440801E+00,
91260876E+00,	91710876E+00,	92600951E+00,	93050951E+00,
95411001E+00,	95861001E+00,	96731076E+00,	97181076E+00,
99661151E+00,	10011151E+00,	10100126E+00,	10145126E+00,
10360201E+00,	10405201E+00,	10495276E+00,	10540276E+00,
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11200401E+00,	11245401E+00,	11340476E+00,	11385476E+00,
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14411201E+00,	14456201E+00,	14541251E+00,	14586251E+00,
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17082101E+00,	17127101E+00,	17202126E+00,	17247126E+00,
17352201E+00,	17397201E+00,	17472251E+00,	17517251E+00,
17622301E+00,	17667301E+00,	17742326E+00,	17787326E+00,
17892401E+00,	17937401E+00,	18012451E+00,	18057451E+00,
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18432601E+00,	18477601E+00,	18552651E+00,	18597651E+00,
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18972801E+00,	19017801E+00,	19092851E+00,	19137851E+00,
19242901E+00,	19287901E+00,	19362926E+00,	19407926E+00,
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20053201E+00,	20098201E+00,	20173251E+00,	20218251E+00,
20323301E+00,	20368301E+00,	20443326E+00,	20488326E+00,
20593401E+00,	20638401E+00,	20713451E+00,	20758451E+00,
20863501E+00,	20908501E+00,	20983526E+00,	21028526E+00,
21133601E+00,	21178601E+00,	21253651E+00,	21298651E+00,
21403701E+00,	21448701E+00,	21523726E+00,	21568726E+00,
21673801E+00,	21718801E+00,	21793851E+00,	21838851E+00,

## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

DTAPLR ■

[illegible]



## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

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( .00000000E+00, .00000000E+00), ( .00000000E+00, .00000000E+00),
( .00000000E+00, .00000000E+00), ( .00000000E+00, .00000000E+00),
( .00000000E+00, .00000000E+00), ( .00000000E+00, .00000000E+00),
( .00000000E+00, .00000000E+00), ( .00000000E+00, .00000000E+00)
TAUOPS = (-.36391481E-16, -.37993231E-16)
GOPPS = (-.19220352E-15, -.11268834E-15)
DGOPPS = (.12227293E-14, .11885721E-14)
RF = (.47143511E+00, .27978254E+00)
NRP = (.23571755E-02, .13989127E-02)
YSWP = (.10277711E-02, -.17317998E-02)
XWP = (.13693002E-05, -.23072783E-05)
NXSTP = (-.37305429E-02, .32317242E-02)
XSTP = (-.46962826E-05, .40683328E-05)
NYSSTP = (-.37305429E-02, .32317242E-02)
YSSTP = (-.35249417E-02, .30536143E-02)
RFNMLT = (.00000000E+00, .00000000E+00)
NRPNM = (.00000000E+00, .00000000E+00)
YSWPNM = (.00000000E+00, .00000000E+00)
XWPNM = (.00000000E+00, .00000000E+00)
NXSTPN = (.00000000E+00, .00000000E+00)
XSTPNM = (.00000000E+00, .00000000E+00)
YSSTPN = (.00000000E+00, .00000000E+00)
$END
$TPOUT1
TWBAR = .11062365E+04
QSDMLS = -.68946471E+00
QMDMLS = .19597945E+00
QBDMLS = .30582425E+00
THETAA = .10012712E+02
CHI = .72881025E+00
D = .72973667E+01
B = -.86570440E+05
KMLTLR = -.53178746E+00
QLDMLS = -.68946471E+00
FDMLS = -.21616689E+00
GWBR5 = -.43017409E+00
DGWBR5 = -.34504740E+01
$END

```